

DEDICATION

This dissertation is dedicated to my beloved parents, Mrs. Miskiah Abu Naim and Mr. Mohammad Hj. Seman, and special dedication to my beloved husband Mr. Asan Azhari bin Sahalan. Without their continual love and support, the completion of this dissertation would not have been possible.

ACKNOWLEDGEMENT

In The name of Allah the Beneficent, the Merciful

I would like to express my greatest appreciation to my supervisor, Assoc. Prof. Dr Saikat Maitra for his valuable guidance, assistant, encouragement, friendship and constructive criticisms during my study. Special appreciations for my previous supervisor Prof. Binay Kanti Dutta from Petroleum Institute, Abu Dhabi and Dr. Tushar Kanti Sen from Curtin University, Australia, for their concern, and continuously support and assistant. Appreciation is also expressed to my co-supervisor Assoc. Prof. Dr. Mohd Azmi bin Bustam @ Khalil for his encouragement and advice. Not to forget, Prof. Khairun from Chemical Eng. Dept. for her support and advice.

I also acknowledge the help of all personnel from Chemical Engineering Department; especially Mr Yusoff and Miss Norazimah, Mr Anuar from Civil Engineering Department; and Mr. Anuar, Mr. Shairul and Mr. Irwan from Mechanical Engineering Department, and not to forget Pn Kamaliah, Pn Puspa Dahlia, Pn. Nurul Aizat, Mr. Kahar, Mr. Imran, Mr. Jamidi, Mr. Zulkarnaen, Major Borhan and Dr. Mohd Noh from UTP Postgraduate Office for their assistant and providing me with necessary facilities.

Thanks are for all my fellow graduate students and special gratitude is given to my beloved parents, brothers, sisters and husband who always encouraged and supported me throughout my education.

ABSTRACT

In this work, the adsorption potential of physic seed hull (PSH), *Jantropia curcas L.* as an adsorbent for the removal of metal ions (Zn^{2+} and Cd^{2+}) and malachite green dye (MG) from aqueous solution has been investigated. The study also has been extended to investigate the effect of anionic surfactant (tetra sodium N-(1, 2dicarboxy ethyl)-Noctadecyl sulfosuccinamate), known as Aerosol 22, on these adsorption processes. The performance of the adsorbent PSH has also been compared with granular activated carbon (GAC) adsorbent. The adsorbent, PSH was thoroughly characterized by SEM-EDX, BET, CHNS, Zeta potential measurement and FTIR studies. It has been observed that the adsorption of metal ions and dye increased with the increase in initial metal ions/dye concentration, contact time of adsorbent and adsorbate, temperature of adsorption, dosage of adsorbent and pH of the solution in an acidic range, but decreased with the increase in the particle size of PSH. Both PSH and GAC adsorbent exhibited better adsorption ability towards Zn^{2+} than Cd^{2+} from aqueous solution. But the adsorption capacity of PSH was found to be higher than that of GAC for both the metal ions and MG dye. Aerosol 22 was used during the adsorption process to provide the anionic functional group on the surface of PSH for supplying further adsorption site for metal ions. Addition of Aerosol 22 improved the adsorbing capacity of PSH for both the metal ions, but the effect was observed to be more for Zn^{2+} . Again, it was further observed that at higher concentration of the surfactant there was a decrease in the adsorption of metal ions. It might be related to the formation of micelles that prevented the adsorption of metal ions. The adsorption process for both the metal ions and dye on PSH was found to be consists of three-staged process - a rapid initial adsorption of the metal ions initially, followed by a period of slower uptake of the metal ions and finally no significant uptake of the metal ions. The kinetics of metal ions adsorption process

was therefore described by a pseudo-second order model. The adsorption equilibrium data were fitted in the three adsorption isotherms, e.g. Freundlich isotherm, Langmuir isotherm and Dubinin-Radushkevich isotherm. The adsorption data fitted best to the Langmuir isotherm indicating the adsorption of metal ions and dye on PSH could be described as a monolayer chemisorption process. The activating energy for the adsorption of metal ions and dye as calculated using from D-R Isotherm was found to be more than 16kJ/mol which is particle diffusion. The adsorption capacity of PSH was found to be comparable to that for other available adsorbents as cited in literatures. From the study it is evident that as an adsorbent, PSH has significant potential for usage in the separation of metal ions and dye from waste water.

ABSTRAK

Dalam kajian ini, potensi lapisan kulit luar biji buah jarak pagar (PSH), (*Jantropa curcas L.*) sebagai bahan penjerap untuk membuang sisa logam berat (Zn^{2+} dan Cd^{2+}) dan pewarna (Malachite Green) dari larutan cecair telah dikaji. Kajian tambahan telah dijalankan dengan menambahkan bahan aktif permukaan bersifat anionik (tetra sodium N-(1,2dicarboxy ethyl)-Noctadecyl sulfosuccinamate) atau dikenali sebagai Aerosol 22 dalam process penjerapan ini. Kajian perbandingan juga telah dilakukan terhadap prestasi bahan penjerap PSH dengan menggunakan bahan penjerap karbon teraktif berbutir (GAC). Kajian pencirian juga telah dilakukan terhadap PSH dengan menggunakan teknik SEM-EDX, BET, CHNS, ukuran potensi Zeta dan kajian FTIR. Pemerhatian mendapati penjerapan ion-ion logam dan pewarna bertambah dengan setiap peningkatan kepekatan ion-ion logam/pewarna, masa interaksi bahan penjerap dengan zat terjerap, suhu penjerapan, dos bahan penjerap dan pH larutan dalam julat berasid, tetapi berkurangan apabila saiz butiran PSH bertambah. Kedua-dua bahan penjerap PSH dan GAC menunjukkan keupayaan penjerapan lebih baik ke atas Zn^{2+} daripada Cd^{2+} di dalam larutan cecair. Walaubagaimanapun keupayaan jerapan PSH didapati lebih tinggi daripada GAC bagi kedua-dua ion logam dan pewarna MG. Aerosol 22 telah digunakan dalam proses penjerapan bagi menyediakan kumpulan berfungsi beranion pada permukaan PSH sebagai tapak penjerapan tambahan bagi ion-ion logam. Aerosol 22 mampu memperbaiki keupayaan menjerap PSH bagi kedua-dua ion logam dan kesan lebih baik adalah pada ion Zn^{2+} . Kajian juga mendapati bahawa pada kepekatan bahan aktif permukaan yang lebih tinggi, penjerapan ion-ion logam adalah berkurangan. Ia mungkin berkait dgn pembentukan misel yang menghalang penjerapan ion-ion logam. Proses penjerapan untuk kedua-dua ion logam dan pewarna pada PSH melibatkan tiga peringkat proses - penjerapan pantas pada

peringkat awal, diikuti penyerapan perlahan dan akhirnya tiada penyerapan. Proses kinetik penyerapan ion-ion logam dan pewarna juga dapat diterangkan menggunakan model pseudo-peringkat kedua. Data keseimbangan penyerapan adalah bersesuaian dengan tiga isoterma penyerapan - isoterma Freundlich, isoterma Langmuir dan isoterma Dubinin-Radushkevich. Data penyerapan isoterma Langmuir merupakan isoterma yang terbaik digunakan bagi menunjukkan penyerapan ion-ion logam dan pewarna pada PSH merupakan proses selapis serapan kimia. Tenaga pengaktifan bagi penyerapan ion-ion logam dan pewarna yang dikira dengan menggunakan isoterma D-R didapati lebih daripada 16kJ/mol dan ini menunjukkan jerapan partikel. Keupayaan jerapan PSH didapati setanding dengan bahan penyerap lain seperti yang dinyatakan dalam imbasan rujukan. Kajian jelas menunjukkan bahawa bahan penyerap PSH mempunyai berpotensi tinggi dalam proses pengasingan ion logam dan pewarna daripada air buangan.

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LIST OF ABBREVIATIONS

<i>A</i>	area, m^2
<i>AAS</i>	Atomic Absorption Spectrometer
<i>b</i>	Langmuir constant, L/mg
<i>BET</i>	Brunauer-Emmett-Teller
C_i	initial concentration, mg/L
C_e	equilibrium concentration, mg/L
C_t	concentration of the sorbate at time t , mg/L
Cd^{2+}	cadmium ion
<i>cec</i>	cation exchange capacity
<i>D-R</i>	Dubinin Radushkevich
<i>E</i>	mean free energy ($kJ\ mol^{-1}$)
<i>EPA</i>	Environmental Protection Agency.
<i>FDA</i>	United States Food and Drug Administration
<i>FTIR</i>	Fourier Transform Infrared
<i>G</i>	Gibbs free energy
<i>GAC</i>	granular activated carbon
<i>h</i>	initial sorption rate
<i>H</i>	standard enthalpy
<i>HM</i>	heavy metals.
<i>IUPAC</i>	International Union of Pure and Applied Chemistry.
k_i	intraparticle diffusion rate constant
k_1	rate constant for first-order model, min^{-1}
<i>KBr</i>	potassium bromide.
k_f	rate constant for Freundlich
k_2	rate constant for second-order model, $g/mg.h$,
K_L	rate constant for Langmuir, mg/g
k_a	adsorption equilibrium constant for thermodynamic
L_a	separation factor of Langmuir
<i>m</i>	mass of adsorbent, mg
<i>MG</i>	malachite green
<i>n</i>	adsorption intensity for Freundlich
P_c	critical pressure
pH_{zpc}	pH at zero point charge
<i>PSH</i>	physic seed hull

q_e	adsorbed amount at equilibrium, mg/g
q_t	adsorbed amount at t time, mg/g
q_m	adsorbed amount at maximum monolayer, mg/g
r	radius
R	gas constant (8.314 J/molK)
R^2	regression correlation coefficient
R_L	separation factor
r_{peak}	peak radius
S	standard entropy
$S_{1/s}$	spreading coefficient
SEM	Scanning Electron Microscopy
T	absolute temperature (k)
t	time, minute
$t^{1/2}$	half-time for adsorption, min
$UV-VIS$	Ultraviolet-visible spectrophotometer
V	solution volume, $m^3 @ mL$
V_{mes}	mesopore volumes.
X_m	maximum adsorption capacity for D-R isotherm (mg/g)
XRD	X-ray diffraction.
Zn^{2+}	zinc ion
Z	charge
Z^2/r	ionic potential

Greek letters

\AA	Angstrom
λ_{max}	maximum wavelength, nm
Δ	change
ε	Polanyi potential
β	constant related to sorption energy ($mol^2 kJ^{-2}$)
Φ_s	sphericity
θ	contact angle