

FINAL EXAMINATION JANUARY 2025 SEMESTER

COURSE

CEB2093 - REACTION ENGINEERING II

DATE

15 APRIL 2025 (TUESDAY)

TIME

2.30 PM - 5.30 PM (3 HOURS)

INSTRUCTIONS TO CANDIDATES

- 1. Answer **ALL** questions in the Answer Booklet.
- 2. Begin EACH answer on a new page in the Answer Booklet.
- 3. Indicate clearly answers that are cancelled, if any.
- 4. Where applicable, show clearly steps taken in arriving at the solutions and indicate **ALL** assumptions, if any.
- 5. **DO NOT** open this Question Booklet until instructed.

Note:

- There are SIX (6) pages in this Question Booklet including the cover page and appendix.
- ii. DOUBLE-SIDED Question Booklet.
- iii. Graph papers and Engineering Data & Formulae Booklet will be provided.

Universiti Teknologi PETRONAS

1. A new type of amorphous aluminosilicate catalyst was prepared by a sol-gel method using poly(ethylene glycol) (PEG) template, for hydrocracking purposes. Nitrogen physisorption isotherm was carried out at 77 K using 3.4 g of the catalyst. The data for the adsorption of nitrogen on the amorphous aluminosilicate catalyst is available in TABLE Q1, where P/Po refers to the relative pressure and V is the volume of nitrogen gas absorbed, cm³(STP)·g-1.

TABLE Q1: Nitrogen absorption on the amorphous aluminosilicate catalyst

| V, cm ³ (STP))⋅g ⁻¹ |
|--|
| 3.0 |
| 5.5 |
| 7.0 |
| 10.5 |
| 15.5 |
| |

a. Determine the volume of gas (V_m) required to fit into Langmuir adsorption isotherm model.

[19 marks]

b. Explain and calculate the BET surface area of the catalyst at STP.

[6 marks]

2. a. Derive a rate of expression of the hydroisomerisation of n-hexane to iso-hexane over a Pt/Al₂O₃ catalyst, assuming that the reaction is a dual site surface reaction-controlled mechanism.

$$n-C_6H_{14} \rightleftharpoons i-C_6H_{14}$$

[17 marks]

 Compare the differences between Langmuir-Hinselwood model and Eiley-Rideal mechanism in terms of adsorption taking place and reaction pathway.

[8 marks]

 a. Explain the importance of high porosity and low tortuosity preferred in a catalyst.

[4 marks]

 Describe a graph of the relationship between diffusion flux and pore size of a catalyst. Identify and explain different diffusion regimes in the graph.

[8 marks]

c. A porous cylindrical catalyst pellet is used in a first-order gas-phase reaction:

 $A \rightarrow B$

The pellet has a radius, R = 2.5 mm, and the reaction occurs with an intrinsic rate constant of k = 0.02 s⁻¹. Species A within the catalyst pores has effective diffusivity of $D_e = 5.0 \times 10^{-6}$ m²·s⁻¹. Assume that the reaction occurs only inside the catalyst, and external mass transfer resistance is negligible.

Calculate the Thiele Modulus for the catalyst pellet and discuss
 TWO (2) significance in relation to internal diffusion resistance.

[7 marks]

ii. Given that effectiveness factor of the catalyst, η = 1. Propose a strategy to enhance catalyst efficiency based on design modification or operating conditions.

[6 marks]

- 4. a. Dry reforming of methane (CH₄) is a catalytic process for syngas production. A 10% Ni/Al₂O₃ catalyst was synthesized via sol-gel method and tested in a fixed-bed reactor. After 30 minutes and 70 minutes on stream, CH₄ conversion of 85% and 60% were obtained respectively.
 - Describe if the catalyst has undergone deactivation with justifications.

[4 marks]

ii. The Ni/Al₂O₃ catalyst may undergo different types of catalyst deactivation. Provide **THREE** (3) types of deactivation mechanism and explain each of them using appropriate illustrations.

[12 marks]

b. In a blast furnace, hematite (Fe₂O₃) is reduced to iron (Fe) in carbon monoxide (CO) according to the following reaction:

$$Fe_2O_3 + 3CO \rightarrow 2Fe + 3CO_2$$

A spherical Fe₂O₃ pellet with an initial radius of 125 μ m is placed in a high temperature CO stream at 1000°C and 3 atmospheric pressures. The reduction process follows the shrinking core model with chemical reaction control. Assume that the rate of reaction constant at this temperature, $k = 3.0 \times 10^{-6}$ cm·s⁻¹, molecular weight of Fe₂O₃ is 159.7 g·mol⁻¹ with density 7.24 g·cm⁻³. Calculate the minimum time required for complete reduction of the Fe₂O₃ pellet into iron. State your assumptions.

[9 marks]

-END OF PAPER-

APPENDIX I: FORMULAS

$$\frac{x}{v(1-x)} = \frac{1}{v_m c} + \frac{(c-1)}{v_m c} x$$

$$S=4.35v_m$$

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$$C_t = C_v + C_{R.S} + C_{P.S}$$

$$\phi = R \sqrt{\frac{k}{D_e}}$$

$$\phi = R \sqrt{\frac{k}{D_e}}$$

$$t = \frac{\rho_B R}{3bk_g C_{Ag}} \left\{ 1 - \left(\frac{r_c}{R}\right)^3 \right\}$$

$$t = \frac{\rho_B R^2}{6b D_e C_{Ag}} \left\{ 1 - 3 \left(\frac{r_c}{R} \right)^2 + 2 \left(\frac{r_c}{R} \right)^3 \right\}$$

$$t = \frac{\rho_B R}{b k_g C_{Ag}} \left(1 - \frac{r_c}{R} \right)$$

$$S_a = \frac{S_o}{1 + k_a t}$$