

**Heat Exchanger Modeling by Neural Network Optimization for  
PETRONAS Penapisan Melaka Sdn. Bhd (PPMSB) Crude Preheat**

**Train**

by

Norazliza Binti Md. Tahir

Dissertation submitted in partial fulfillment of  
The requirements for the  
Bachelor of Engineering (Hons)  
(Chemical Engineering)

JULY 2005

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**CERTIFICATION OF APPROVAL**

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BACHELOR OF ENGINEERING (Hons)  
(CHEMICAL ENGINEERING)

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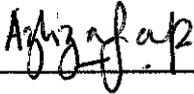
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**TRONOH, PERAK**

July 2005

## **CERTIFICATION OF ORIGINALITY**

This is to certify that I am responsible for the work submitted in this project, that the original work is my own except as specified in the references and acknowledgements, and that the original work contained herein have not been undertaken or done by unspecified sources or persons.



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**NORAZLIZA BINTI MD. TAHIR**

## **ABSTRACT**

The title of this Final Year Research Project is 'Heat Exchanger Modeling by Neural Network Optimization for PETRONAS Penapisan Melaka Sdn. Bhd (PPMSB) Crude Preheat Train'. This project involves the post modeling of heat exchanger sensitivity analysis that covers neural network based model and implication of statistical analysis to predict the heat exchanger efficiency for maintenance scheduling strategy of Crude Preheat Train (CPT). The main objectives of this study are to minimize the error in the predicted values and enhance the robustness of the previous model to predict in future.

This Final Report consists of five major sections. The first section describes the introduction to Neural Network based Predictive Model, background of the CPT, fouling activity and Heat Exchanger Maintenance in PP(M)SB, problem statement that defined the significant of the post modeling heat exchanger sensitivity analysis, project objectives and scope of works done throughout the study. The next section consists of literature review and theory extracted from well established journals and web sites to provide relevant information for the project as references.

The third section entails the project methodology comprising series of stages for the project to be carried out. It follows by the fourth section that serves as the gist of the report that presents the findings and includes discussion on the results obtained and significance behind any failure occurs at each stage of the completed optimization strategies. The results are discussed in term of statistical analysis, comparison of results between different transfer functions configurations used and graphs of actual de-normalized versus predicted outlet temperature for both tube side and shell side. The final section of the report consists of the conclusion corresponds to the objectives set earlier and some recommendations for future improvement of the Neural Network model. The Final Report ends with a list of references and appendices.

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## **ABBREVIATIONS AND NOMENCLATURES**

<b>NN:</b>	<b>Neural Network</b>
<b>FYP:</b>	<b>Final Year Project</b>
<b>PP(M)SB:</b>	<b>PETRONAS Penapisan Melaka Sdn. Bhd</b>
<b>PSR:</b>	<b>PETRONAS Second Refinery</b>
<b>CPT:</b>	<b>Crude Preheat Train</b>
<b>CDU:</b>	<b>Crude Distillation Unit</b>
<b>LSWR:</b>	<b>Low Sulphur Waxy Residue</b>
<b>IVt:</b>	<b>Tube Integral Flow</b>
<b>ANOVA:</b>	<b>Analysis of Variances</b>
<b>RMSE:</b>	<b>Root Means Square Error</b>
<b>CDC:</b>	<b>Correct Directional Change</b>
<b>P:</b>	<b>Purelin Transfer Function</b>
<b>T:</b>	<b>Tan-sigmoid Transfer Function</b>
<b>L:</b>	<b>Log-sigmoid Transfer Function</b>
<b>To:</b>	<b>Shell side outlet temperature</b>
<b>to:</b>	<b>Tube side outlet temperature</b>

# **CHAPTER 1**

## **INTRODUCTION**

The title of this Final Year Research Project is 'Heat Exchanger Modeling by Neural Network Optimization for PETRONAS Penapisan Melaka Sdn. Bhd (PPMSB) Crude Preheat Train'. The Neural Network (NN) Modeling used for this project is carried out with reference to Do Thanh Van's predictive model for heat exchanger efficiency in the Crude Preheat Train (CPT) of PP(M)SB. It is the post modeling of heat exchanger sensitivity analysis that covers neural network based model to predict and anticipate in future the heat exchanger efficiency using new test set of data for simulation, implication of statistical analysis and research based study for the optimization and maintenance scheduling strategy of CPT.

Fouling in crude oil preheat trains is a major problem that costs the industry billions of dollars per years (ESDU, 2000). In the refinery, the crude oil which is untreated petroleum tends to foul the heat exchangers due to the nature viscous characteristic and at the same time carries a lot of particles. By philosophy, the more energy recovered by the CPT the more beneficial it is to the operation. However, the dynamic behavior of fouling has hindered the proper application of many integration techniques to the preheat train design hence results in the least efficient heat recovery over a time period. [1]

The research on a predictive model for maintenance scheduling and performance of CPT in PP(M)SB will be developed by application of NN with the implication of Analysis of Variance (ANOVA). The network designs consider the fouling behavior and any parameters which promote significant fouling prior to predict future performance of the heat exchanger. This study is vital to aid the industrial practitioner in making more informed decision to plan on the suitable time for heat exchanger preventive maintenance scheduling prior to reduce the need of unplanned shutdown and to avoid the refinery production loss.

Prior to make this project feasible within the scope and time frame, this predictive model for Cold Low Sulphur Waxy Residue (LSWR) Pumparound Heat Exchanger, E-1104 A-D will be using the same NN architecture as previous model with current 24 predictors. The model is to be further developed, optimized and tested against the original data set A and new data set B to test on the robustness of the model in predicting future trend and compare the data behavior change. Any necessary amendment on the control strategy and modeling approach will be considered over the time period.

## 1.1. BACKGROUND OF STUDY

### 1.1.1 PETRONAS Penapisan (Melaka) Sdn. Bhd, PP(M)SB

PETRONAS Penapisan (Melaka) Sdn. Bhd, PP(M)SB is the PETRONAS second refinery after Petronas Penapisan (Kerteh) Sdn. Bhd. Located in Sungai Udang, PP(M)SB within an area of 926 acres consists of two crude refining trains, namely PETRONAS Second Refinery Phase 1 (PSR-1) and PETRONAS Second Refinery Phase 2 (PSR-2) plants. Both PSR-1 and PSR-2 are designed to operate as an integrated complex with common utility, offsite and marine facilities.

Table 1. Comparison between PSR-1 and PSR-2

Train	Facilities	Capacity	Ownership
PSR-1	Sweet train- hydroskimming	100,000 BPSD	PETRONAS
PSR-2	Sour train- deep conversion	100,000 BPSD	Malaysian Refining Company Sdn. Bhd

PSR-1 is wholly owned by PETRONAS and was incorporated on September 19, 1987 to process local sweet crude (i.e sulfur content less than 0.5 wt%). PSR-2 operated by Malaysian Refining Company (MRC) is a joint venture between PETRONAS (53%) and Conoco Philips USA (47%) and was incorporated in May 1991 to process Middle East sour crude (i.e crude with sulfur content of more than 0.5 wt%). [2]

### **1.1.2 Crude Preheat Train of PPMSB**

The Crude Preheat Train in the Crude Distillation Unit (CDU) is a series of heat exchangers used to maximize heat recovery by having heat exchange from the CDU product pumparounds streams with the mixed crude from the storage tanks. The CPT in PP(M)SB has four Pre-Desalter and seven Post-Desalter heat exchangers. The mixed crude oil is preheated from the ambient temperature to 130 °C in the Pre-Desalter heat exchangers before entering the Desalter Vessel. The mixed crude then is further preheated up to 232 °C before entering the Preflash Drum, Furnace and the Distillation Column. [3]

For this final year research project, main focus of the modeling optimization is the continuation from the previous heat exchanger E-1104. It has a counter flow of one shell pass and six tube passes with crude oil as the shell side fluid and LSWR as the tube side fluid. Subject to the available time frame, NN based model for all eleven heat exchangers in the CPT of the CDU will be considered and developed gradually.

### **1.1.3 Fouling and Heat Exchanger Maintenance**

Fouling in heat exchanger tends to reduce the overall heat transfer coefficient. The two main impacts of fouling on preheat train operation are reduced heat recovery and increased pressure drop. By theory, fouling happens when small particles and thick fluids with relatively low thermal conductivity deposit on the heat transfer surfaces, thus building up higher heat transfer resistance. The phenomena explain why a fouled heat exchanger could not meet the targeted heating or cooling requirement and need to be compensated by additional heating or cooling outside the heat exchanger which resulted in higher energy consumption.

There are two key parameters influencing the fouling rate of a heat exchange surface namely the film temperature and the fluid velocity at the vicinity of the surface. The first way in fouling mitigation technique is to clean the heat exchangers at regular intervals.

However, this benefit is rapidly lost after a few weeks as several exchangers are prone to rapid fouling. [4] In PP(M)SB, two common methods widely applied to remove deposit in the CPT heat exchangers namely mechanical cleaning and hotmelting.

Through mechanical cleaning, deposited material can be removed completely and the peak efficiency of the respective heat exchanger after cleaning may reach the design value. However, it might require 3 days of completely shutdown of the equipment for cleaning purpose. Meanwhile for hotmelting, the cleaning can be done on-line such that the crude will bypass the fouled heat exchanger when the heating medium is flowing through to melt off the foulants. Kerosene or diesel wash (i.e act as flushing oil) are used to effectively dissolve these foulants. However, hotmelting does not remove the deposit completely especially the heavy sludge but take lesser time (8 hours) as compared to mechanical cleaning. [3]

## **1.2 PROBLEM STATEMENT**

Due to the frequent changes in process condition and irregular fouling rate in the heat exchanger, a reliable tool is needed to assess and monitor the effect of every individual fouling resistance on the preheat train overall fouling trend. [4] The former NN Predictive Model for Heat Exchanger Efficiency in the CPT of PPMSB developed by Do Thanh Van used to predict the suitable time to clean the exchanger so that maintenance task can be prepared hence reduce the shutdown time.

The successful of the previous NN predictive model architecture is only capture the historical data of original Data Set A Reset Tube Integral Flow (IVt) taken from 2/06/2002 till 16/02/2005 with 933 observations but not for the new Data Set B Reset taken from 17/02/2005 till 9/06/2005 with 111 observations (i.e lack of robustness). Based on the results obtained from the ANOVA test performed by Mr. Nasser M Ramli and Ms. Haslinda Zabiri, the ANOVA results shown that between the old data set and the new data set 11 variables are statistically the same while 14 variables are statistically different. The statistical different in data indicates the data set are not from the same

population and cannot be physically mean. This condition explains why the prediction using the old model for the new data is not really good that might incorporates some sort of gradual change which has been masked in the huge old data set. Thus, the old model need to be re-validated by tested against the tail of the old Data Set A Reset IVt with 121 observations and then compared with the Data Set B Reset to observe the data behavior changes. From the comparison, a new NN-based model is required and built using different approach in normalization technique of the Tube Integral flow (IVt). Optimization of the new NN-based model is necessary if there is gradual drift in the crude properties by dropping unnecessary parameters, introducing feedback with time lagged into the model and changing the NN modeling architecture and configurations.

### **1.3 OBJECTIVES AND SCOPE OF STUDY**

#### **1.3.1 Objectives**

The objectives of this final year research project are as listed below:

- i. To construct and develop a Feed Forward Backpropagation (BP) NN architecture using MATLAB's "Network/Data Manager".
- ii. To train, validate and make necessary amendment on the best NN configurations by using training set of data with optimum number of predictors.
- iii. To simulate network using testing set of data to compute the tolerance, percentage error, Root Means Square Error (RMSE), Correct Directional Change (CDC), scatter plot and residual of the network via Statistical Analysis.
- iv. To optimize and enhance robustness of the Heat Exchanger Predictive Model by introducing feedback mode and implication of ANOVA.
- v. To perform literature study on the Fouling mitigation technique and optimization of heat recovery system in preheat train.
- vi. To develop the NN based model for all eleven heat exchangers in the CPT of PPMSB subject to the available time frame.

### 1.3.2 Scope of Work

The scope of research works covers the post modeling of the heat exchanger sensitivity analysis predictive model as continuation from the one developed by Do Thanh Van. As in line with the objectives set earlier, the tasks include comparison of the data behavior trends of both the *Data Set B Reset* and the *tail of old Data Set A Reset IVt*, optimization of the new NN model with different normalization technique by tested against normalized Tube Integral Flow using the minimum and maximum value of the whole period for both Data Set A and Data Set B, application of feedback mode in NN new model, implication of Statistical Analysis by application of ANOVA and literature study for optimization of heat recovery system and fouling propensity in the preheat train of Crude Distillation Unit.

The first task required the author to study on the features, characteristics and proper chronological of NN architecture and training to be applied in the heat exchanger modeling. The NN model training, validation and testing phase will be conducted in the MATLAB NN Tool with the integration of calculation spreadsheet created using Microsoft Excel®. For this project, the variables used have been reduced from original 25 predictors to 24 predictors by dropping the Flash Point.

Further study will be conducted to determine the accuracy and compatibility in the simulated results with implication of Statistical Analysis. Necessary amendment on the best NN configurations and modeling approach will be required if there is significant data behavior change observed. The successful of the predictive modeling enable the expansion of the project scope to develop NN based model for all eleven heat exchangers in the CPT of PPMSB subject to the available time frame.

## CHAPTER 2

### LITERATURE REVIEW AND THEORY

#### 2.1 COLD LSWR PUMPAROUND HEAT EXCHANGER E-1104 A-D

Since the prediction using the old model for the new data set is not so good, therefore this project will concentrate on the previous model heat exchanger E-1104 A-D. The heat exchanger chosen has a counter flow of one shell pass and six tube passes with crude oil as the shell side fluid and LSWR as the tube side fluid. It consists of two pairs of identical series heat exchangers connected in parallel. Figure 1 below shows the preheat train system for CDU in PP(M)SB. [3]

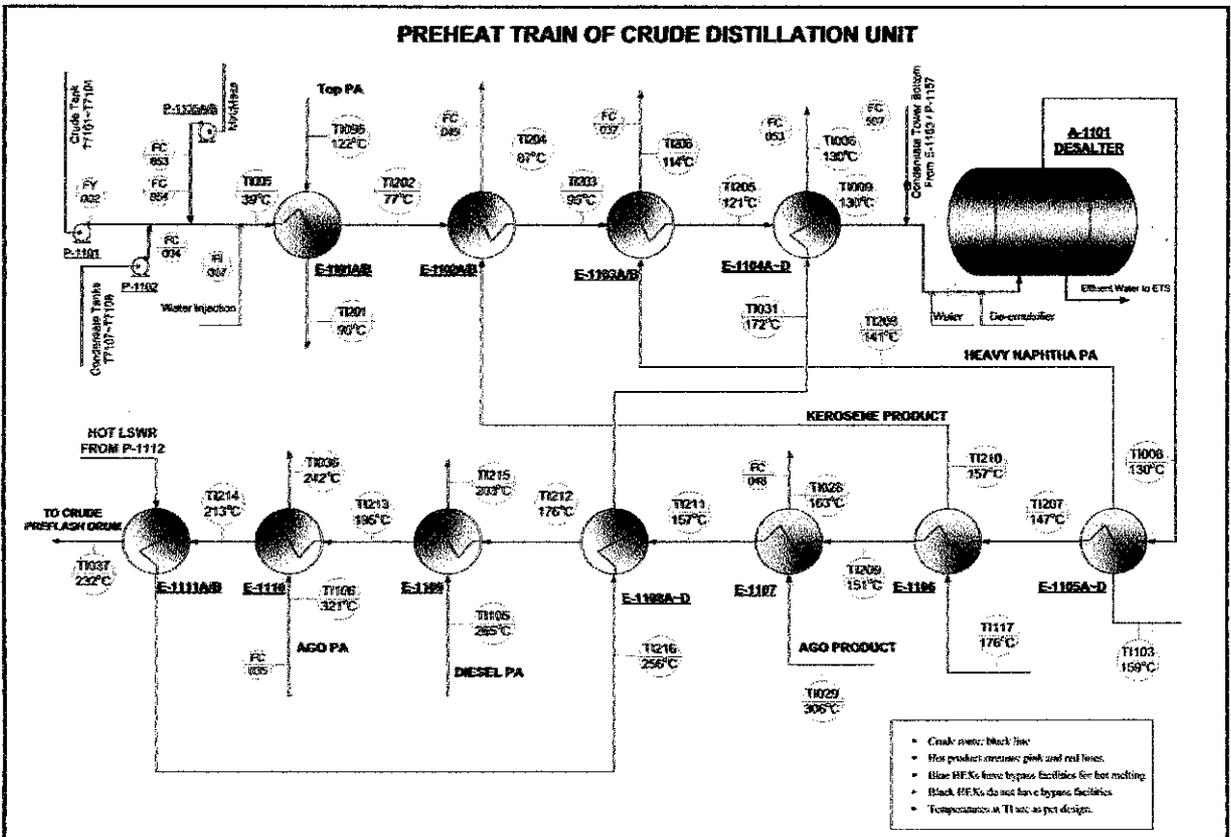


Figure 1. Preheat train system for Crude Distillation Unit

Legends of the Figure 1:

- Crude route is represented by the black line while the hot product streams are represented by the pink and red lines.
- The heat exchangers in blue have bypass facilities, whereas those in black do not.
- The temperature at the Temperature Indicator (TI) is as per design.

## **2.2 FOULING AND HEAT RECOVERY SYSTEM**

### **2.2.1 Fouling in Heat Exchanger**

By definition, fouling includes any kind of deposit of extraneous material that appears upon the heat transfer surface during the lifetime of the heat exchanger. An additional resistance to heat transfer is introduced and the operational capability of the heat exchanger is correspondingly reduced. In many cases, the deposit is heavy enough to significantly interfere with the fluid flow and increase the pressure drop required to maintain the flow rate through heat exchanger. [5]

Fouling of heat exchangers is one of the major concerns of the petroleum refining industry. It leads to operating problems, affects the efficiency of the heat recovery systems, and can seriously alter the profitability of a refinery through over consumption of fuel, throughput reduction during cleaning operations, significant increase in pressure drop, furnace bottlenecks, increase of maintenance costs etc. Since the preheat train of CDU is the heavy energy consumer in the refinery operation, the smart way to mitigate fouling is to start from the design step of the exchangers. In the refining industry where shell & tube heat exchanger are widely applied, the common methods used are: [4]

- Usage of anti-fouling additives.
- Careful sequential ordering of the processed crude.
- Adapt the lay out to facilitate heat exchanger cleaning operations such as mechanical cleaning (i.e turnaround), hotmelting, bypasses and shells connected in parallel.

In addition, splitting crude stream is encouraged as it is the only cold stream and needs to be contacted by many hot streams. Where pump-around streams are used as a source of heat, exchanger bypasses on the crude side are necessary to maintain a fixed duty which resulted in lower crude flow rates in the heat exchangers.

Chemical reaction fouling where deposition is caused by species generated through chemical reactions in the bulk fluid, viscous sublayer or tube walls tends to be the dominant fouling mechanisms in crude oil preheat trains (Watkinson and Wilson, 1997). Chronic chemical reaction fouling is very sensitive to high wall temperatures and low flow velocities. The network designs proposed by traditional energy integration approaches are likely to suffer severe fouling. Alternative approaches must therefore incorporate models for fouling behavior, to identify and avoid those conditions which promote significant fouling. [1]

### **2.2.2 Preheat train overall fouling trend**

Fouling has significant impact on the refinery operation and utilization. However, the mechanism of fouling or factors contribute to it are still in research. Operating conditions mainly feed and product flow rate, are expected to vary on a daily basis due to crude slate changes and to throughput reduction due to fouling. Because of frequent changes in process conditions, a reliable tool is needed to assess the effect of every individual fouling resistance on the preheat train overall fouling trend by using the Normalized Furnace Inlet Temperature (NFIT) as the point of reference. The change in NFIT over the monitoring period is due only to changes in fouling resistances.

The NFIT monitoring approach which is widely applied in the Ebert and Panchal Model is according to the journal referred to M.Bories and T. Patureaux (2004). The validity of this approach has been demonstrated by a statistical analysis of fouling data collected in Chevron and Exxon refineries to determine whether it could explain the differences observed in the fouling rates of the exchangers of the preheat train in CDU.

In this model, the fouling resistance is obtained via the following formula:

$$R_f = \frac{1}{U_a} - \frac{1}{U_c} \quad (1)$$

Where the fouling resistance,  $R_f$  appears to be linear function of time. Based on the observations done, *heat exchangers upstream the Desalter unit present much lower fouling rates* than those placed downstream. In general cases, the exchanger presenting the highest fouling rate is the hottest one just before the furnace. The preheat exchanger network scheme and the trend on heat exchanger fouling rates are attached in Appendix A-1 and A-2 respectively.

In agreement to the Ebert and Panchal Model, fouling model on minimize fouling while maximizing heat recovery according to the journal referred to B.L Yeap, D.I Wilson, G.T Polley and S.J.Pugh (2004) stated that the *chemical reaction fouling is dominant fouling mechanism in the hottest exchangers* (i.e near to the furnace). Chemical reaction fouling nature characteristic which is very sensitive to temperature and less sensitive to flow velocity appears to be contradicting to the design philosophy. The main objective of the preheat train which is to maximize heat recovery resulted in higher crude stream temperature and hence greater fouling, which eventually deteriorates the preheat train network performance over time.

### **2.3 NEURAL NETWORK MODELS**

Most industrial processes such as chemical reactors and separation systems exhibit nonlinear behavior such that significant engineering time and effort is required to develop and validate detailed theoretical dynamics models. Neural Networks (NN) or Artificial Neural Networks (ANN) are important class of empirical non-linear models to model complex or little understood process with large input-output data sets and as well

to replace models that are too complicated to be solved in real time (Ramchadran and Rhinehart, 1995; Su and McAvoy, 1997). [6]

### **2.3.1 Biological Analogy**

The exceptional computational abilities of the human brain have motivated the concept of NN. The inherent characteristics of the brain can perform certain types of computation such as perception, pattern recognition, and motor control much faster than existing digital computers (Su and McAvoy, 1997; Haykin, 1999). This complex and nonlinear computation performed by the human brain has led to the development of ANN by using structural constituents called neurons and the synaptic interconnection between them. Each of the neuron has a branching input structure (dendrites), cell body and branching output structure (axon). The real power of the NN comes when neurons are combined into the multilayer structures.

### **2.3.2 Artificial Neural Network**

Artificial neural networks are relatively crude electronic networks of "neurons" based on the neural structure of the brain. It process records one at a time, and "learn" by comparing their prediction of the record with the known actual record. The errors from the initial prediction of the first record is fed back into the network, and used to modify the networks algorithm the second time for many iterations. As shown in Figure 2, a neuron in an artificial neural network is:

- i. A set of input values ( $x_i$ ) and associated weights ( $w_i$ ).
- ii. A function ( $g$ ) that sums the weights and maps the results to an output ( $y$ ).

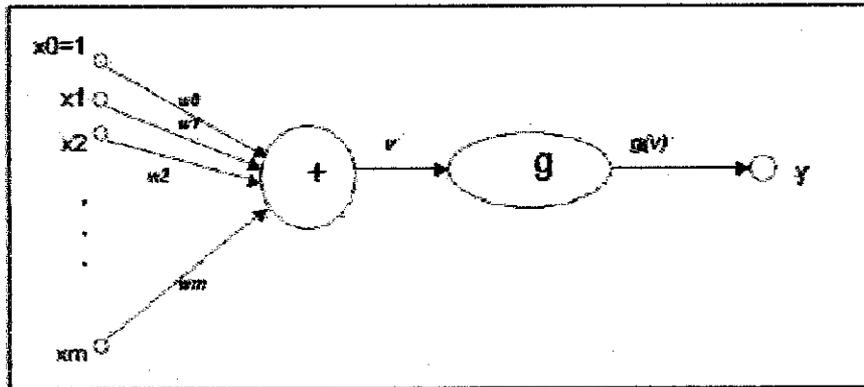


Figure 2. Signal diagram of Artificial Neural Network

Basically, the neurons (i.e nodes) are organized into several layers which are the *input*, *output* and *hidden layer* as shown in Figure 3. Each neuron in the hidden layer is connected to the neuron in adjacent layers via the connection weights. These weights are the unknown parameters that are estimated based on the data input/output from the process to be modeled. The number of the unknown parameters can be quite large and powerful nonlinear programming algorithms are required to fit the parameters to the data using the least-squares objective function (Edgar et al., 2001). If enough neurons are utilized, it is proven that any input-output process can be simulated accurately by a NN model (Su and McAvoy, 1997).

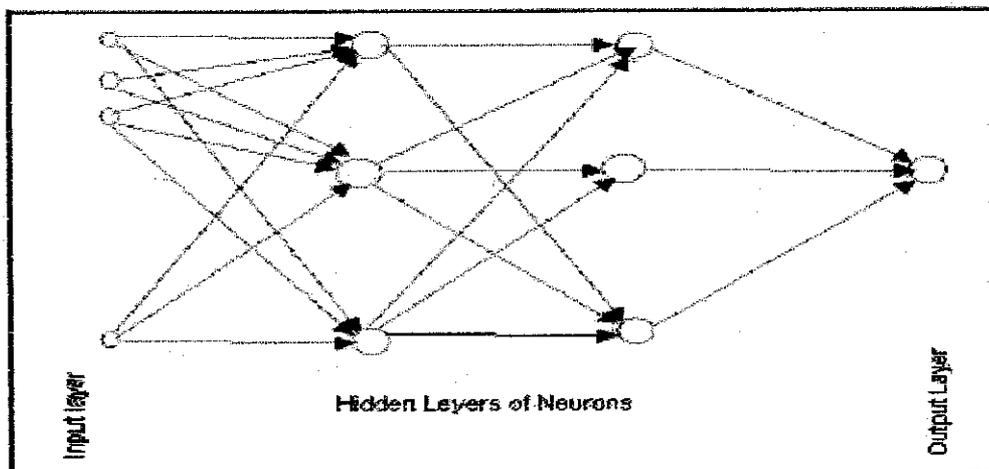


Figure 3. Multilayer Neural Network with three layers.

*Training* of a NN model involves estimating the unknown parameters which generally utilizes normal operating data taken in the operating region where the model is intended

to be used. The network processes the records in the training data one at a time, using the weights and functions in the hidden layers and compares the resulting outputs against the desired outputs. Errors are then propagated back through the system, causing the system to adjust the weights for application to the next record to be processed. This process occurs over and over as the weights are continually tweaked. During the training of a network the same set of data is processed many times as the connection weights are continually refined.

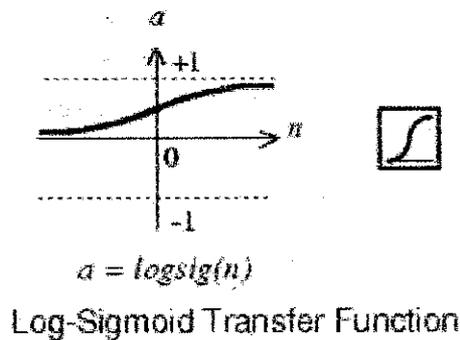
After the parameters have been trained, another large set of data is used to validate whether the model is adequate. Changes in the NN architecture must be made often by trial and error if the resulting NN model is not satisfactory.

### **2.3.3 Feedforward Back Propagation Network**

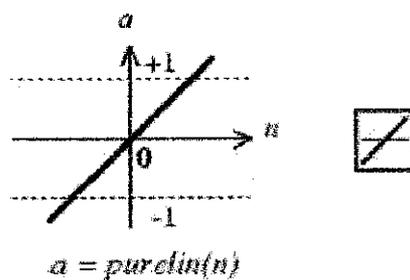
The feedforward, back-propagation architecture was developed in the early 1970's by several independent sources (Werbor, Parker, Rumelhart, Hinton and Williams). Currently, this synergistically developed back-propagation architecture is the most popular, effective, and easy-to-learn model for complex and multi-layered networks. Its greatest strength is in non-linear solutions to ill-defined problems by generalizing the Widrow-Hoff learning rule. The typical back-propagation network has an input layer, an output layer, and at least one hidden layer. Each layer is fully connected to the succeeding layer. The backpropagation (BP) algorithm is also known as *error backpropagation* or *back error propagation* or the *generalised delta rule*.

The *Training* process uses some variant of the Delta Rule, which starts with the calculated difference between the actual outputs and the desired outputs. The connection weights are increased in proportion to the error times a scaling factor for global accuracy provided the inputs, output and the desired output must be present at the same processing element. The complex part of this learning mechanism is for the system to determine which input contributed the most to an incorrect output and how does that element get changed to correct the error. An inactive node would not contribute to the

error and would have no need to change its weights. The training inputs are applied to the input layer of the network, and desired outputs are compared at the output layer. During the learning process, a forward sweep is made through the network, and the output of each element is computed layer by layer. The difference between the output of the final layer and the desired output is back-propagated to the previous layer(s), usually modified by the derivative of the transfer function, and the connection weights are normally adjusted using the Delta Rule. This process proceeds for the previous layer(s) until the input layer is reached. Networks with biases, a sigmoid layer, and a linear output layer are capable of approximating any function with a finite number of discontinuities. The most commonly used transfer functions include PURELIN and LOG-SIGMOID as shown in Figure 4.



(a)



(b)

Figure 4. Purelin and log-sigmoid transfer functions.

### **2.3.4 Structuring the Feedforward Back Propagation Network**

The number of layers and the number of processing elements per layer are important decisions. There is no quantifiable or best answer to the layout of the network for any particular application. However, the followings are the general rules in developing a NN model:

**Rule One:** As the complexity in the relationship between the input data and the desired output increases, the number of the processing elements in the hidden layer should also increase.

**Rule Two:** If the process being modeled is separable into multiple stages, then additional hidden layer(s) may be required. If the process is not separable into stages, then additional layers may simply enable memorization of the training set, and not a true general solution effective with other data.

**Rule Three:** The amount of training data available sets an upper bound for the number of processing elements in the hidden layer(s). To calculate this upper bound, use the number of cases in the training data set and divide that number by the sum of the number of nodes in the input and output layers in the network. Then divide that result again by a scaling factor between five and ten. Larger scaling factors are used for relatively less noisy data. Too many of the artificial neurons causing the training set will be memorized hence generalization of the data will not occur making the network useless on new data sets (i.e over trained of the model).

## **2.4 STATISTICAL ANALYSIS**

### **2.4.1 Analysis of Variance (ANOVA)**

The main purpose of Analysis of Variance (ANOVA) is to test differences in *means* (for groups or variables) for statistical significance. For this project, ANOVA test is

performed to verify that the original and the three segmented sets (i.e Training, Validation and Test set) are from the same population. This is accomplished by analyzing the variance, by partitioning the total variance into the component that is due to true random error (i.e., within- group *SS*) and the components that are due to differences between means. These latter variance components are then tested for statistical significance. The comparison between the actual variation of the group averages and that expected is expressed in terms of the *F* ratio:

$$F = (\text{found variation of the group averages}) / (\text{expected variation of the group averages})$$

The null hypothesis is correct whenever *F* to be about 1 whilst "large" *F* indicates a location effect. The P-value (i.e probability) reports the significance level of the data such that:

- If P-value > 0.05 accept Null hypothesis.
- If P-value < 0.05 reject Null hypothesis.

#### 2.4.2 Root Means Square Error (RMSE)

RMSE is used to determine the error between the predicted and calculated values by using the following formula: [3]

$$RMSE = \sqrt{\frac{\sum_1^N [\tilde{y}_i(t) - y_i(t)]^2}{N}} \quad (2)$$

Where  $y_i(t)$  is the actual value for the variable *i* at time, *t*

$\tilde{y}_i(t)$  is the forecast value

*N* is the total number of measurement value for variable *i*

The percentage error of RMSE of less than 5 % is considered good for the modeling. The RMSE and the percentage error were calculated using the Microsoft Excel® Spreadsheet. The following is the formula used for percentage error calculation:

$$\text{Percentage error}(\%) = \frac{\text{RMSE}}{\text{Mean Actual Temperature}} \times 100\% \quad (3)$$

### 2.4.3 Correct Directional Change (CDC)

CDC is the number of times the prediction observation followed the up and down movement of the known target variable. It is another important measurement to ensure the predicted results behave in correspond manner to the actual trend. The CDC formula is as follow with same nomenclature as RMSE calculation: [3]

$$\text{CDC} = \frac{100\%}{N-1} \sum_{i=2}^N D_i \quad (4)$$

Where  $D_i = 1, \text{if } [y_i(t) - y_i(t-1)] \times [\tilde{y}_i(t) - \tilde{y}_i(t-1)] > 0$

$D_i = 0, \text{if } [y_i(t) - y_i(t-1)] \times [\tilde{y}_i(t) - \tilde{y}_i(t-1)] < 0$

## **CHAPTER 3**

### **METHODOLOGY OF PROJECT WORK**

#### **3.1 PROJECT OVERVIEW**

The project methodology for the post modeling of the heat exchanger sensitivity analysis predictive model will be similar to the previous model developed by Do Thanh Van. In general, the modeling and simulation work will utilize MATLAB Version 6.1. The NN model training, validation and testing phase will be conducted in the MATLAB Neural Network Toolbox's Network Data Manager with the integration of calculation spreadsheet created using Microsoft Excel®.

The relevant data of the preheat train used for this project is on daily average basis taken from 2/06/2002 to 16/02/2005 for Data Set A with 933 observations and the extension of new data for Data Set B taken from 17/02/2005 to 9/06/2005 with 111 observations. A new approach is applied by normalizing the Tube Integral Flow (IVt) using the minimum and maximum value of the whole period for both Data Set A and Data Set B. The original 'Reset' method in IVt calculation used in the previous model has been dropped for better accuracy of the results. For this project, the variables used have been reduced from original 25 predictors to 24 predictors by dropping the Flash Point. Prior to minimize error in the predicted results, *Feedback mode* has been applied for both Data Set A and Data Set B with time lagged by *two days* hence making a total of 28 predictors.

#### **3.2 PROJECT METHODOLOGY**

This project is carried out in series of stages as follows:

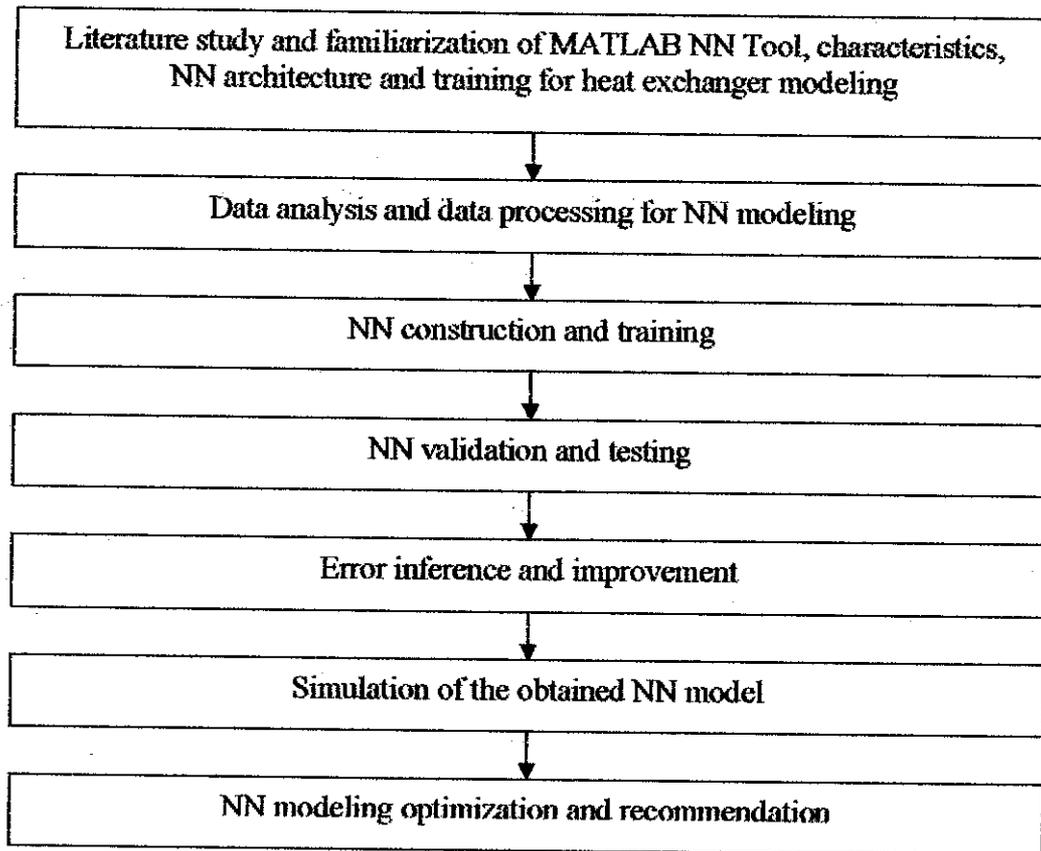


Figure 5. Project methodology for NN post modeling of heat exchanger

### 3.2.1 Literature Study and Familiarization of MATLAB NN Tool

Familiarization of MATLAB NN Tool is done by study the features, characteristics and proper chronological of NN architecture and training to be applied in the heat exchanger modeling. The MATLAB NN Tool is built with the integration of Microsoft Excel® calculation spreadsheets. All relevant data for the CPT modeling were organized in proper spreadsheets manner for ease of data analysis. The variables included process data (tube and shell side flow rates and temperature), lab data (different crude properties) and planning data (crude type and blend compositions).

### 3.2.2 Data Analysis and Processing for Neural Network Modeling

The original 'Reset' normalization technique in the previous model has been removed and the new NN-based model is constructed by normalizing the Tube Integral Flow (IVt) using the minimum and maximum value of temperature for the whole range of Data Set A and Data Set B. Initial 25 variables were reduced to 24 by dropping the flash point, which served as the new predictors to the NN model as shown in Table 2.

Table 2. The finalized 24 predictors for new NN model

Peak Efficiency Value	-
LSWR- Tube side inlet temperature (11TI031)	°C
Tube side Volumetric Flow rate (11FC053)	m <sup>3</sup> /hr
Tube Integral flow	m <sup>3</sup>
Crude – Shell side inlet temperature (11TI205)	°C
Shell side total Volumetric Flow rate	m <sup>3</sup> /hr
Shell Integral flow	m <sup>3</sup>
Basic Sediment and Water	vol. %
Salt Content	lb/1000bbbls
Wax Content	wt %
Pour point	°C
Asphaltenes	wt %
Total Acid Number	mgKOH/g
Nitrogen Content	ppm
Ash Content	wt %
Kinematic Viscosity @ 70°C	cSt
Characterization Factor	-
Sodium (Na)	ppm
Density @ 15°C	kg/L
Crude feed component for CDU - Tapis	vol. %
Crude feed component for CDU - Miri	vol. %
Crude feed component for CDU - Terengganu	vol. %
Crude feed component for CDU - Bintulu	vol. %
Crude feed component for CDU - Masa	vol. %

Data Set A was taken from 2/06/2002 till 16/02/2005 with total 933 observations for process modeling whilst Data Set B covered data from 17/02/2005 till 9/06/2005 with 111 observations. For NN construction, Data Set A is randomized and re-arranged in

ascending order according to *random number* and followed by partition into three main parts:

- (a) 50 % of observation data equivalent to 466 sets for *training* data.
- (b) 40 % of observation data equivalent to 373 sets for *validation* data.
- (c) 10 % of observation data equivalent to 94 sets for *testing* data.

Normalization of the data was performed using the following general equation:

$$x_n = \frac{(x - x_{\min})}{(x_{\max} - x_{\min})} \quad (5)$$

Where,

$x$  = true value

$x_n$  = normalized value

$x_{\min}$  = minimum value

$x_{\max}$  = maximum value

### 3.2.3 Neural Network Construction, Training, Validation and Testing

#### Neural Network Construction

Numerous trial and errors are needed prior to find the optimum number of hidden layers, number of neurons per layers, transfer function configurations and the learning function. As for this project, there are 3 main transfer functions namely PURELIN (P), LOGSIG (L) and TANSIG (T).

PURELIN is a linear transfer function. If linear output neurons are used, the network outputs can take any values. The function LOGSIG generates outputs from 0 to 1 as the neuron's net input goes from negative to positive infinity. Meanwhile, TANSIG function is non-linear transfer function which is bounded between -1 to 1 and analytic everywhere. According to the journal referred to S.S.P. Rattan and W.W. Hsieh (2004), it has to be a constant function for a complex transfer function to be bounded and analytic everywhere. Using a complex transfer function like TANSIG without any

constraint will lead to non-convergent solutions (Nitta, 1997). Thus, early researchers did not consider such functions as suitable complex transfer functions since it mainly focused on overcoming the unbounded nature of the analytic functions in the complex domain but preserved the arguments or phases (Georgiou & Koutsouseras, 1992; Hirose, 1992) [7].

Here, 6 best combinations of NN transfer functions that have been considered for process modeling were; PLP, TLT, LLL, LPL, TTL and TLP. The best configuration for the NN model was selected from the model that gave the lowest RMSE,  $R^2$  and CDC values. The number of neurons is equal to the number of inputs/outputs for the respective first and last layers.

#### Training and Validation

Validation set is needed to evaluate the performance of the trained model. Validation set can avoid over training of the NN model by providing early stopping. Normally validation set error value is compared with the trained set error value to determine the optimum model parameters, such as the number of epochs, transfer functions options and how many layers are necessary.

#### Testing

Test data was fed into the successfully trained model for simulation. The model is used to predict the tube and shell outlet temperatures based on the input data. A graph is plotted to compare the actual denormalized values and predicted values generated from the optimum NN configuration.

### **3.2.4 Error Inference and Improvement**

The purpose of NN model improvement is to further minimize the error in prediction value. The improvement strategies are:

- By trial and error method, create different NN models using different training functions, increasing epoch number, changing number of layers and changing number of neurons in each layer.
- Addition of *Feedback variables* with time lagged as new predictors to the model for training and validation.
- Calculate RMSE, CDC and correlation coefficient,  $R^2$  for test data at different criterions. The value of  $R^2$  for both tube and shell side can be directly obtained by plotting actual versus predicted values in x-y graph using Microsoft Excel.

The statistical Analysis above can be summarized in tabulated form for ease of comparison and analysis of the model performance.

### **3.2.5 Simulation of the obtained NN model**

The simulation results (i.e predicates) generated by the optimum NN model for both test set of Data set A and Data set B will be presented in scatter x-y graph using Microsoft Excel. The graph consists of the actual and predicted values for both the tube and shell outlet temperature.

### **3.2.6 NN modeling optimization**

*Feedback mode with time lagged* by two days is applied for both the tube and shell outlet temperature. The lagged variables were fed back into the models as the new inputs making total of 28 predictors and the model has been re-trained to generate more accurate predicted results. Details on the Feedback mode will be further discussed in the Result and Discussion section.

ANOVA test was carried out to compare the means and standard deviations of the new NN model. This was done to ensure the sets of data in Data Set B are from the same population. The overall optimization strategy flow diagram of this NN modeling is shown in Figure 6 below.

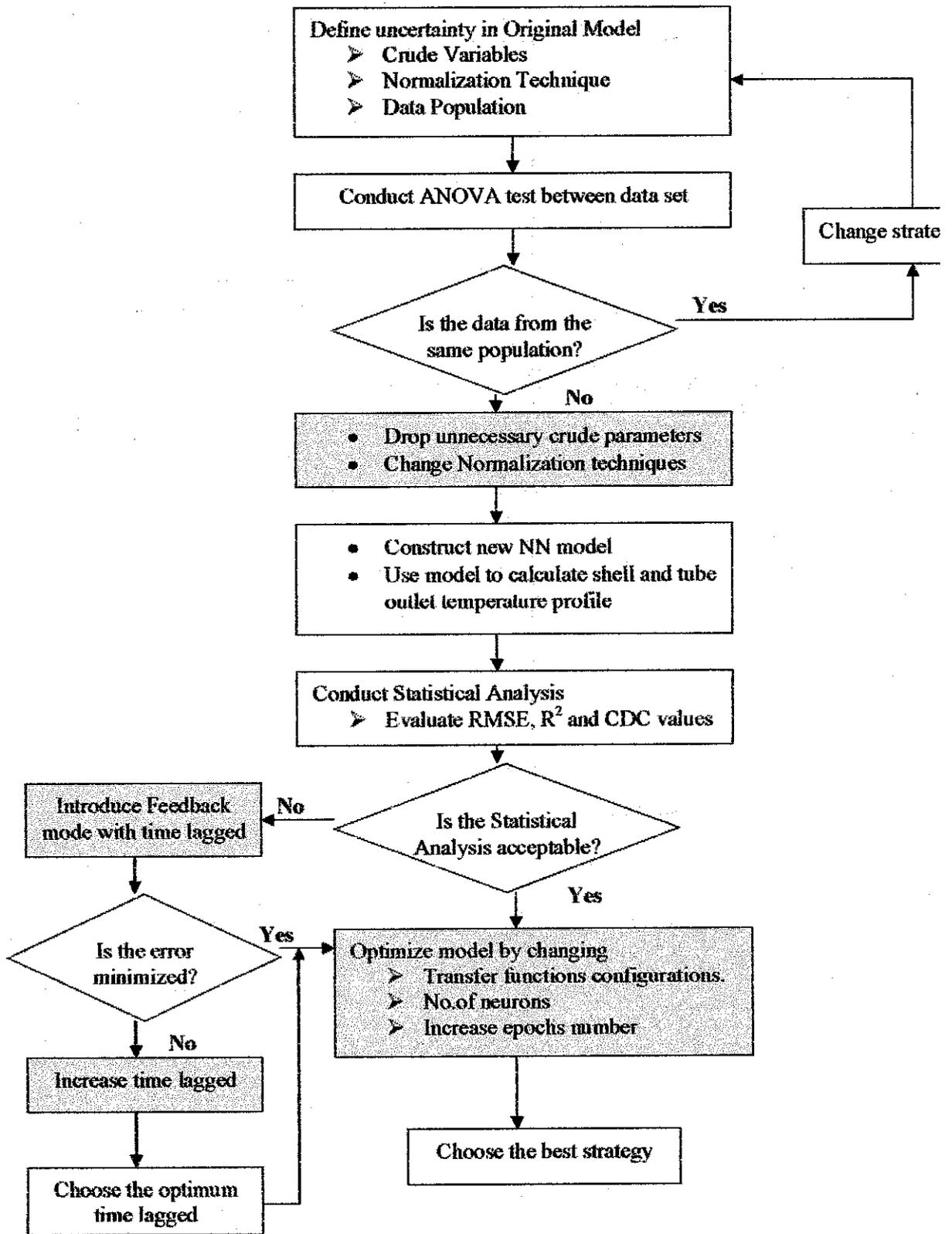


Figure 6. NN Modeling of Overall Optimization Strategy Flow Diagram

## CHAPTER 4

### RESULTS AND DISCUSSION

#### 4.1 INITIAL FINDINGS

Due to lack of robustness of the previous NN predictive model, it can only capture the trend of tube and shell outlet temperature within the range of historical Data Set A Reset Tube Integral Flow (IVt) but not for the new Data Set B Reset. The ANOVA test conducted shown 11 variables are statistically the same while 14 variables are statistically different between the old data set and the new data set. The summary of the ANOVA test is shown in Table 3 below:

Table 3. Summary of ANOVA test between Data Set A Reset IVt and Data Set B Reset

Variables	P-value	Remarks
Ind: Index for cleaning time	1.91E-41	reject
Tin: Crude Shell side inlet temperature	4.71E-05	reject
Ivc: Shell Integral flow	0.406177	accept
Vs: Shell side vol flow rate	0.800268	accept
ti: LSWR tube side inlet temp	0.710897	accept
IVt: Tube Integral flow	0.127711	accept
Vprod: tube side vol flow rate	0.000133	reject
TA: crude feed component for CDU (Tapis)	0.108277	accept
MR: crude feed component for CDU (Miri)	4.12E-09	reject
TC: Terengganu Condensate	1.92E-05	reject
BC: Bintulu Condensate	5.46E-21	reject
MA: Masa Crude	0.040933	reject
Density at 15 C	1.28E-14	reject
Flash points	0.619303	accept
Sed: Basic Sediment & water	0.075065	accept
TAN: total acid number	0.495126	accept
Pp: pour point	4.18E-50	reject
Sl: salt content	0.251915	accept
N2: Nitrogen content	3.05E-16	reject
Ash: Ash content	3.27E-09	reject
Wax: wax content	0.000234	reject
u: Kinematic viscosity at 70 C	2.36E-24	reject
CF: Characterization Factor	0.165629	accept
Asp: Asphaltenes	0.000839	reject
Na: Sodium	3.29E-06	reject
to(t): LSWR tube side outlet temp	5.55E-62	reject
Tout(t): Crude shell side outlet temp	0.184326	accept

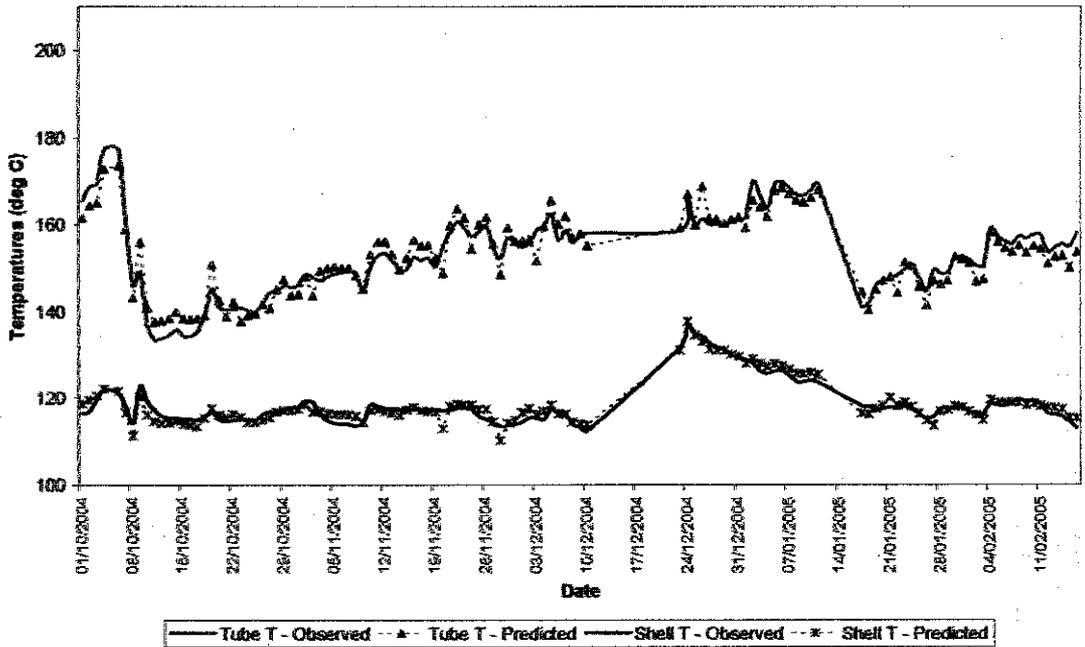
The statistical different in means and standard deviations between Data Set A and Data Set B indicate those data set are not from the same population and cannot be physically mean. Here, the prediction using the old trained model for the new Data Set B resulted in significance error that might incorporates some sort of gradual change which has been masked in the huge old data set.

From the trend between the tail of the old Data Set A Reset IVt (i.e taken from 1/10/2004 to 16/2/2005 with 121 observations) and Data Set B Reset as shown in Figure 7 and Figure 8 respectively, the predicted de-normalized values for both shell and tube outlet temperatures of tail Data Set A was good whilst for Data Set B the values suddenly deteriorated. Thus, a new NN-based model using different approach in normalization technique is required to minimize the error in the predicted values. The followings are the statistical analysis done for the tail Data Set A and Data Set B:

Table 4. Statistical Analysis on Tail Data Set A Reset IVt and Data Set B Reset

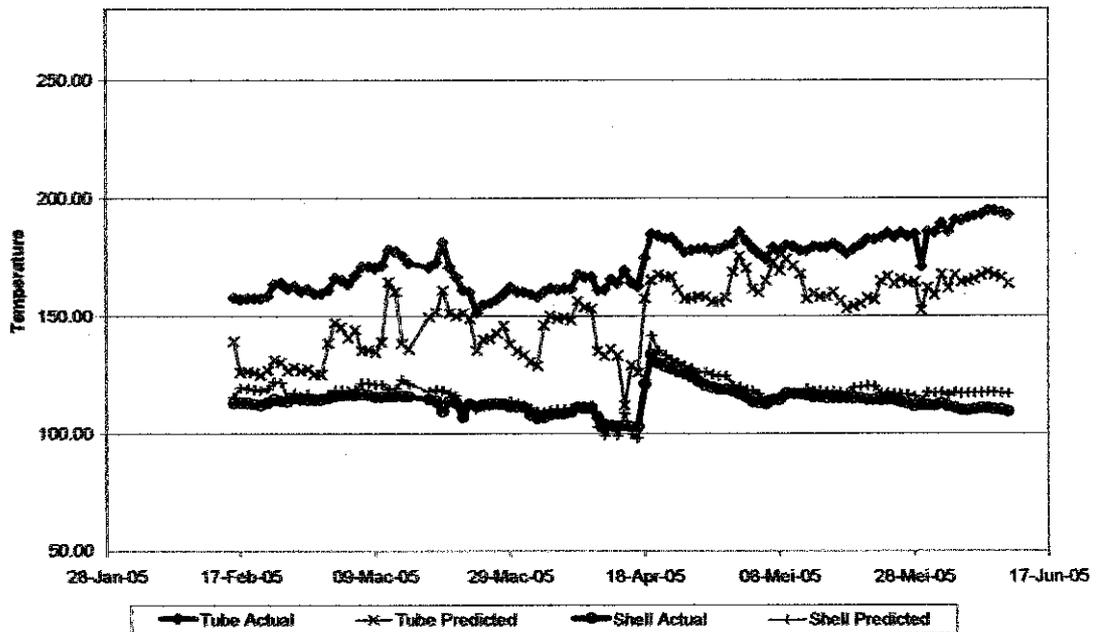
Stat Analysis	Tube outlet (to)		Shell outlet (Tout)	
	Set B Reset	Set A tail	Set B Reset	Set A tail
RMSE	24.0785	2.7989 (1.8293%)	4.2224	1.3850 (1.166%)
CDC	89.3805	86.6667	74.3363	80
R2	0.682	0.9195	0.8397	0.9336

**Outlet Temperatures: Actual vs Predicted for Test Data Set**



**Figure 7. Graph of predicted and actual de-normalized outlet temperatures for tail of Data Set A Reset IVt.**

**Outlet Temperatures:Actual vs Predicted for Test Data Set**



**Figure 8. Graph of predicted and actual de-normalized outlet temperatures for Data Set B Reset**

## 4.2 OPTIMIZATION STRATEGIES

This post modeling of heat exchanger sensitivity analysis utilizes neural network (NN) based model that covered a *step by step optimization approaches* done on the previous model which is developed by Do Than Van using original 25 predictors trained at 300 epochs number. The main objectives of this study are to minimize the error in the predicted values and enhance the robustness of this model to predict in future rather than memorizing the pattern of training data behavior. Basically this study is carried out in series of stages as follows:

### 4.2.1 Different Approach in Normalization Technique

In response to the matter in Section 4.1, a new NN model was constructed by normalizing the Tube Integral Flow (IVt) using the minimum and maximum value of the whole period for both Data Set A and Data Set B. The original 'Reset' normalization technique in the previous model has been removed. Original 25 variables used in the previous model were reduced to 24 variables by dropping the flash point, which served as the new predictors to the NN model.

The new NN model utilized the same NN configuration as previous model by using PLP transfer function at 300 epochs number. However, the predicted results were still not satisfied even though the results for Data Set B gave slight improvement to the tube and shell side RMSE values. The optimum configurations for the NN model are tabulated in Table 5 whilst the statistical analysis done for this new model is shown in Table 6.

Table 5. The optimum settings for new NN model construction

Parameters	Values
Network	Feed-forward back propagation
Training function	TRAINRP
Adaptation learning function	LEARNGDM
Performance function	MSE
Epochs	300
Number of layer	3

Layer 1: number of neurons	24
Transfer function	PURELIN
Layer 2: number of neurons	15
Transfer function	LOGSIG
Layer 3: number of neurons	2
Transfer function	PURELIN
Min grad	1E-006
Max fail	5
delt_inc	1.2
delt_dec	0.5
delta0	0.07

Table 6. Comparison of Statistical Analysis between the new and original NN model

**SET A**

Stat Analysis	Tube outlet (to)		Shell outlet (Tout)	
	Original	New	Original	New
RMSE	2.1875	3.034	0.9523	1.5606
CDC	93.5484	93.5484	92.4731	93.5484
R2	0.9765	0.9547	0.9789	0.9395

**SET B**

Stat Analysis	Tube outlet (to)		Shell outlet (Tout)	
	Original	New	Original	New
RMSE	24.0785	22.9702	4.2224	2.9529
CDC	89.3805	90	74.3363	71.8182
R2	0.682	0.6271	0.8397	0.7333

Basically, the NN model is used to predict the tube and shell outlet temperatures based on the input data. Here, the predicted results for Data Set B would be of interest throughout the discussion to show the accuracy and robustness of the optimized model in predicting future trend. Figure 9 shown the graph of the actual de-normalized and predicted values generated from the new NN model with 24 predictors. The plots for the tube and shell side temperature coefficient of correlation are shown in Appendix B-1 and B-2 respectively.

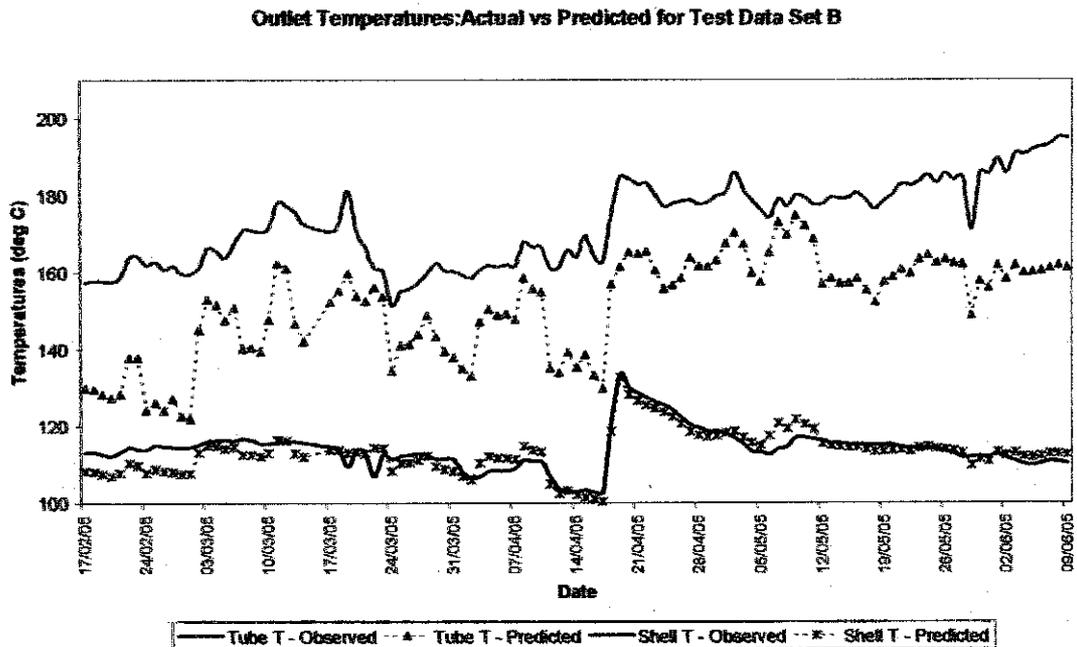


Figure 9. Graph of predicted and actual de-normalized outlet temperatures for new NN model with 24 predictors.

#### 4.2.2 Introduction of Feedback Mode with Time Lagged

Prior to minimize error in the predicted values for Data Set B especially the tube side outlet temperature, the new NN model is further optimized by introducing the *feedback variables* with time lagged by *two days* in the Training, Validation and Testing data (Please refer to Appendix C-1 for raw data). The predicates (i.e output) of the NN model which refer to the tube side outlet temperature ( $t_o$ ) and shell side outlet temperature ( $T_o$ ) were lagged by 2 days and fed back into the model as the predictors (i.e input) at  $(t-1)$ ,  $(t-2)$ ,  $(T-1)$  and  $(T-2)$  as shown in Appendix C-2.

The feedback mode has been applied for both Data Set A and Data Set B with total of 28 *predictors* (i.e original 24 predictors + 4 feedback variables) at 400 epochs number. From the comparison done between the three best combinations of NN transfer functions namely *PLP*, *TIT* and *III*, the combination of *PLP* transfer functions configuration appeared to give the **best overall performance** in term of RMSE and CDC for both the tube and shell side as compared to others.

Introduction of feedback variables into the new NN model resulted in *significant improvement* in the tube side outlet temperature (to) for Data Set B provided the RMSE values has been *reduced by half*. This is because the feedback variables comprise of lagged predicates values will be further used to compare with the desired output and back propagated to the previous layer causing the system to adjust the weights to be processed many times as the connection weights are continually refined. Thus, this improves the accuracy and reduces the sudden ‘jump’ of the predicted values. However, the RMSE value of the predicted shell side outlet temperature were slightly increased but within compromise values.

Besides, the epochs numbers that have been increased to 400 enable the data to be fully trained before the validation error started to increase. For this model, the epoch stopped at 233, the desired error was 0 and the performance was 0.000687244 as shown in Appendix C-3. The optimum configurations for the NN model are tabulated in Table 7 whilst the statistical analysis done for this feedback model is shown in Table 8.

Table 7. The optimum settings for feedback NN model construction

<b>Parameters</b>	<b>Values</b>
Network	Feed-forward back propagation
Training function	TRAINRP
Adaptation learning function	LEARNGDM
Performance function	MSE
Epochs	400
Number of layer	3
Layer 1: number of neurons Transfer function	28 PURELIN
Layer 2: number of neurons Transfer function	15 LOGSIG
Layer 3: number of neurons Transfer function	2 PURELIN
Min grad	1E-006
Max fail	5
delt inc	1.2
delt dec	0.5
delta0	0.07

Table 8. Statistical Analysis between TLT, PLP and LLL transfer functions configuration

**SET A**

Stat Analysis	Tube outlet (to)			Shell outlet (Tout)		
	TLT	LLL	PLP	TLT	LLL	PLP
RMSE	3.6653	3.0799	<b>3.671</b>	1.3740	1.6153	<b>1.9765</b>
CDC	91.3043	91.3043	<b>93.4783</b>	89.1304	91.3043	<b>90.2174</b>
R2	0.9418	0.9527	<b>0.9339</b>	0.9545	0.9372	<b>0.9046</b>

**SET B**

Stat Analysis	Tube outlet (to)			Shell outlet (Tout)		
	TLT	LLL	PLP	TLT	LLL	PLP
RMSE	9.1282	12.9041	<b>10.0755</b>	7.0602	3.3233	<b>3.5194</b>
CDC	81.4815	76.8519	<b>84.2593</b>	62.037	65.7407	<b>69.4444</b>
R2	0.6326	0.2347	<b>0.4861</b>	0.3066	0.7738	<b>0.7468</b>

Figure 10 shown the graph of the actual de-normalized and predicted values generated from the NN feedback model with 28 predictors using PLP transfer functions whilst Figure 11 and 12 shown the graphs for both TLT and LLL configurations respectively. The plots for the tube and shell side temperature coefficient of correlation for PLP feedback NN model are shown in Appendix D.

Outlet Temperatures: Actual vs Predicted for Test Data Set B feedback mode

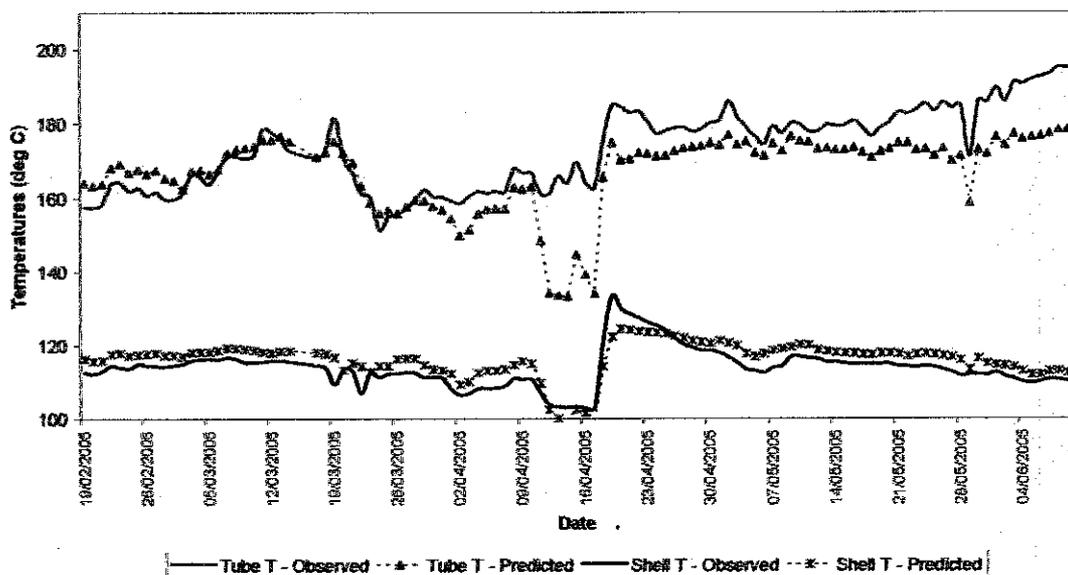


Figure 10. Graph of predicted and actual de-normalized outlet temperatures for new NN feedback model with 28 predictors using PLP

Outlet Temperatures: Actual vs Predicted for Test Data Set B feedback mode

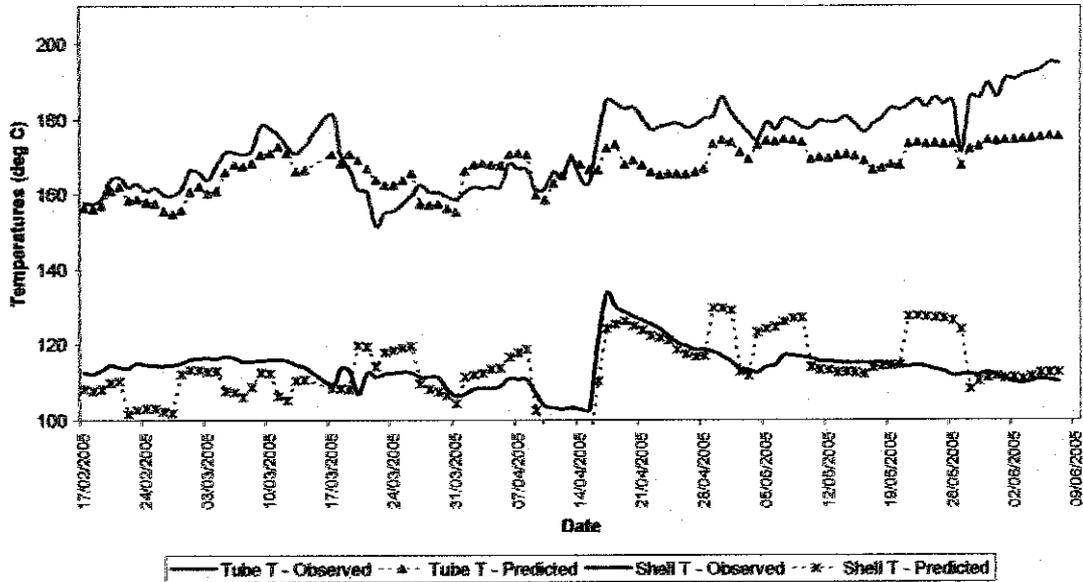


Figure 11. Graph of predicted and actual de-normalized outlet temperatures for new NN feedback model with 28 predictors using TLT

Outlet Temperatures: Actual vs Predicted for Test Data Set B feedback mode

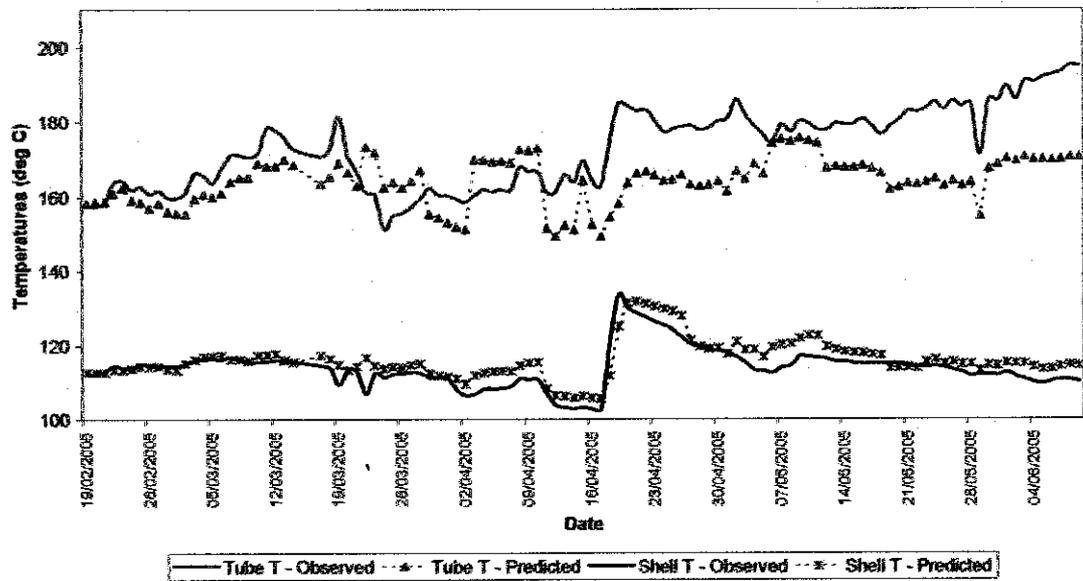


Figure 12. Graph of predicted and actual de-normalized outlet temperatures for new NN feedback model with 28 predictors using LLL

### 4.2.3 Increase Time Lagged in NN Feedback Mode

In response to the optimization strategy in Section 4.2.2, introduction of feedback mode with time lagged by 2 days able to reduce the RMSE values of the predicted tube side outlet temperature for Data Set B by half. Here, it is expected that by increasing the time lagged, the RMSE values will be further minimized.

The time lagged has been increased by 4 days for both the tube side outlet temperature ( $t_o$ ) and shell side outlet temperature ( $T_o$ ) at time ( $t-1$ ), ( $t-2$ ), ( $t-3$ ), ( $t-4$ ), and ( $T-1$ ), ( $T-2$ ), ( $T-3$ ), ( $T-4$ ) thus making a total of 32 predictors (i.e original 24 predictors +8 feedback variables). The new predictors had been trained at 400 epochs number using the optimum model with PLP transfer functions configuration.

From the statistical analysis done for Data Set B, increasing time lagged to 4 days resulted in *more deteriorated predicted values* in term of RMSE and  $R^2$  as compared to feedback mode with time lagged by 2 days. However, the CDC values shown slight improvement. This phenomenon occurred because of the model might be "over-trained" and the model tends to memorize the patterns rather than generalizing the data hence making the NN model useless on the new data sets. As a conclusion, the optimum NN model settings for this post modeling study is *feedback NN model with time lagged by 2 days*.

The results on the statistical analysis is shown in Table 9 whilst Figure 13 shown the graph of the actual de-normalized and predicted values generated from the NN feedback model with time lagged by 4 days.

Table 9. Statistical Analysis between time lagged by 2 days and 4 days

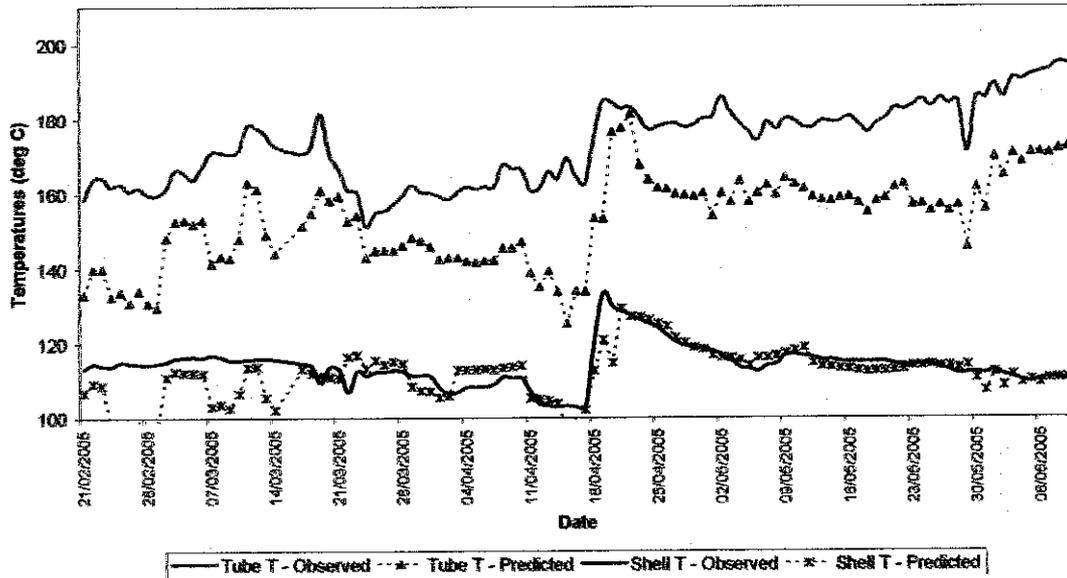
#### SET A

Stat Analysis	Tube outlet ( $t_o$ )		Shell outlet ( $T_{out}$ )	
	lag 2	lag 4	lag 2	lag 4
RMSE	3.6710	3.2117	1.9765	2.2672
CDC	93.4783	88.3333	90.2174	70.8333
R2	0.9339	0.9471	0.9046	0.8793

**SET B**

Stat Analysis	Tube outlet (to)		Shell outlet (Tout)	
	lag 2	lag 4	lag 2	lag 4
RMSE	10.0755	<b>21.4678</b>	3.5194	<b>6.1395</b>
CDC	84.2593	88.3333	69.4444	70.8333
R2	0.4861	0.6692	0.7468	0.3282

**Outlet Temperatures: Actual vs Predicted for Test Data Set B feedback mode**



**Figure 13. Graph of predicted and actual de-normalized outlet temperatures for NN feedback model with time lagged by 4 days.**

**4.2.4 Changing Number of Neurons in First/Middle Layer**

At this stage, the optimization strategy is to give final polishing to the optimum NN model settings by changing the number of neurons in the first or the middle layer. By philosophy, as the complexity in the relationship between the input data and the desired output increases, the number of the processing elements in the hidden layer should also increase.

Via a lot of trials and errors, statistical analysis comparing three best NN transfer function configurations with different optimum number of neurons in different layers

has been done respectively. The followings are the three best NN configurations with number of neurons at each layer inside the bracket for feedback NN model with time lagged by 2 days:

- i. PLP [ 28,15,2 ]
- ii. LLL [ 40,35,2 ]
- iii. TLT [ 40,30,2 ]

Table 10 shown results on the statistical analysis of all the three configurations whilst Figure 14 and Figure 15 shown the trend on predicted temperature profile of Data Set B over time for both the LLL and TLT configurations respectively. For PLP configuration, the trend on the predicted temperature profile over time is given in Figure 10.

Table 10. Comparison of Statistical Analysis between TLT, LLL and PLP configurations

**SET A**

Stat Analysis	Tube outlet (to)			Shell outlet (Tout)		
	TLT [40,30,2]	LLL [40,35,2]	PLP [28,15,2]	TLT [40,30,2]	LLL [40,35,2]	PLP [28,15,2]
RMSE	3.2185	3.1359	3.671	2.0541	1.1922	1.9765
CDC	90.2174	91.3043	93.4783	85.8696	92.3913	90.2174
R2	0.9502	0.9525	0.9339	0.8991	0.9651	0.9046

**SET B**

Stat Analysis	Tube outlet (to)			Shell outlet (Tout)		
	TLT [40,30,2]	LLL [40,35,2]	PLP [28,15,2]	TLT [40,30,2]	LLL [40,35,2]	PLP [28,15,2]
RMSE	8.5287	9.9224	10.0755	4.6419	3.5250	3.5194
CDC	66.6667	72.2222	84.2593	60.1852	66.6667	69.4444
R2	0.4135	0.6204	0.4861	0.7632	0.7325	0.7468

Outlet Temperatures: Actual vs Predicted for Test Data Set B feedback mode

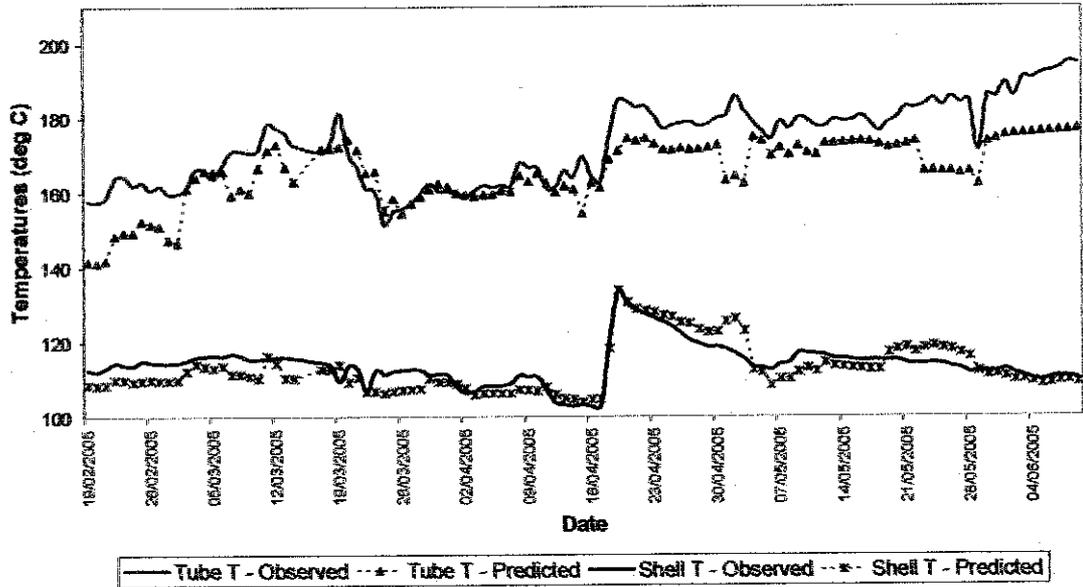


Figure 14. Graph of predicted and actual de-normalized outlet temperatures for NN feedback model for LLL [ 40,35,2 ] configurations.

Outlet Temperatures: Actual vs Predicted for Test Data Set B feedback mode

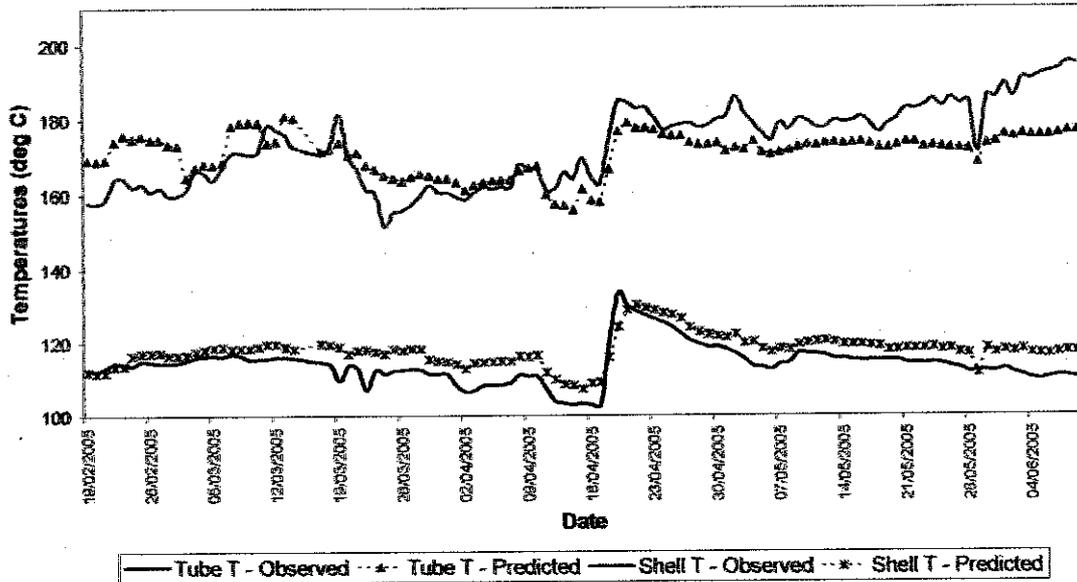


Figure 15. Graph of predicted and actual de-normalized outlet temperatures for NN feedback model for TLT [ 40,30,2 ] configurations.

From the comparison done on the statistical analysis results and trend of temperature profile between all the three NN transfer functions configurations, **PLP [ 28,15,2 ]** gives the **overall best performance** in term of RMSE,  $R^2$  and CDC values.

Focusing on the results of the statistical analysis for Data Set B, even though the RMSE value of PLP configuration slightly higher than TLT and LLL configurations for the tube side, the CDC value of PLP is higher than the others. The higher the CDC values, the better the model can capture the direction change of the output during training process and can predict the change well. Based on Figure 10, the temperature profile plotted using PLP configuration follow the actual temperature trend and almost lies on the actual trend at the starting phase. These results indicate the model is good.

As for LLL configuration, the RMSE values is better than PLP but the starting and end phase of the predicted tube side outlet temperature profile shown fluctuation and deviated from the actual trend. Meanwhile, the TLT configuration gives the lowest RMSE value for the tube side but the temperature profile almost constant everywhere which is not good (i.e not following the actual trend) and indicating low CDC value.

#### **4.2.5 Conduct ANOVA Test on Feedback mode PLP configuration (2 days lag)**

From the optimum NN model settings, the trend of the temperature profile for both tube and shell side shown *drifting in data* between the first and the second half of the time range. Data Set B which covered data from 17/02/2005 till 9/06/2005 with 111 observations thus was segregated into 2 main parts to test on the population between data namely:

- i. Part 1 - covered data from 19/02/2005 until 9/04/2005
- ii. Part 2 – covered data from 10/04/2005 until 9/06/2005

ANOVA test has been conducted on the NN feedback model with time lagged by 2 days to ensure the sets of data in Data Set B are from the same population. Based on the

results obtained, only 6 variables between the 2 main parts are statistically the same while remaining 22 variables are statistically different. The statistical different in data indicates the Data Set B are not from the same population and this explains why the error in Data Set B cannot be further optimized. According to the respective technologist in PP(M)SB, there were changes in the actual operating condition whereby the feed of the Crude Distillation Unit (CDU) has been reduced due to mechanical cleaning in heat exchanger E-1103 from 10/04/2005 until 18/04/2005 and the bypass stream of heat exchanger E-1104 was not opened during that time hence causing sudden drop in the actual tube and shell side outlet temperatures. The followings are the summary of the ANOVA test results:

Table 11. ANOVA test results

Variables	P-value	Remarks
Ind: Index for cleaning time	1.8E-124	reject
Tin: Crude Shell side inlet temperature	2.34E-06	reject
Ivc : Shell Integral flow	5.22E-33	reject
Vs: Shell side vol flow rate	0.315317	accepted
ti: LSWR tube side inlet temp	5.89E-16	reject
IV t: Tube Integral flow	2.11E-33	reject
Vprod: tube side vol flow rate	0.038708	reject
TA: crude feed component for CDU (Tapis)	0.001548	reject
MR: crude feed component for CDU (Miri)	4.22E-06	reject
TC: Terengganu Condensate	0.003403	reject
BC: Bintulu Condensate	0.001583	reject
MA: Masa Crude	0.986997	accepted
Density at 15 C	2.07E-06	reject
Sed: Basic Sediment & water	0.00074	reject
TAN: total acid number	0.462966	accepted
Pp: pour point	0.396702	accepted
SI: salt content	0.019643	reject
N2: Nitrogen content	4.19E-06	reject
Ash: Ash content	0.01255	reject
Wax wax content	4.08E-06	reject
$\nu$ : Kinematic viscosity at 70 C	0.290139	accepted
CF: Characterization Factor	2.87E-08	reject
Asp: Asphaltenes	0.952891	accepted
Na: Sodium	4.87E-05	reject
to (t-1)	1.15E-24	reject
to(t-2)	7.1E-24	reject
Tout (t-1)	0.001947	reject
Tout(t-2)	0.005533	reject
to(t): LSWR tube side outlet temp	6.49E-26	reject
Tout(t): Crude shell side outlet temp	0.000601	reject

In response to above matter, the statistical analysis done for the 2 main parts as shown in Table 12 proved that there is **drifting in Data Set B**. Due to changes in actual operating condition in CDU at PP(M)SB from 10/04/2005 until 18/04/2005, the statistical analysis shows that results for Part 1 is better than Part 2 in term of overall RMSE,  $R^2$  and CDC values for both the tube and shell side outlet temperature.

Table 12. Statistical Analysis to test drifting in Data Set B

**SET B ~part 1 (19/02/05 - 9/04/05)**

Stat Analysis	Tube outlet (to)	Shell outlet (Tout)
	PLP [28,15,2]	PLP [28,15,2]
RMSE	4.0927	3.4934
CDC	85.1064	59.5745
R2	0.6733	0.7773

**SET B ~ part 2 (10/04/05 - 9/06/05)**

Stat Analysis	Tube outlet (to)	Shell outlet (Tout)
	PLP [28,15,2]	PLP [28,15,2]
RMSE	10.9752	3.4267
CDC	85	76.6667
R2	0.5422	0.7309

#### 4.2.6 Adaptive Training of NN model

Since the Data Set B are in different populations due to process changes, the optimum NN feedback model used for this study can only predicts future trend up to maximum 2 months. Therefore, the NN model needs to be re-trained by implication of *Adaptive Training*. Here, Part 2 of Data Set B from 10/04/2005 until 9/06/2005 will be re-trained using new training data set to improve the accuracy of the predicted results. Linear networks that are adjusted at each time step based on the new input and target vectors can find the weight and bias that minimizes the network's sum-squared error for recent input and target vectors.

For Adaptive Training, the Part 2 of Data Set B has been segregated into 3 main partitions namely:

- i. *Training Data* taken from 26/03/2005 until 13/05/2005 for 49 days observations
- ii. *Validation Data* taken from 14/05/2005 until 28/05/2005 for 15 days observations
- iii. *Testing Data* taken from 29/05/2005 until 9/06/2005 for 12 days observations

Table 13 shows the statistical analysis of the adaptive training whilst Figure 16 shows the graph of the actual de-normalized and predicted values generated from the new model. From the results obtained, the statistical analysis of the adaptive model is acceptable for both tube and shell side outlet temperature. A slight increment of RMSE value in tube side outlet temperature might due to the network not contain enough training data as the input to the feedback model to enable complete learning. Therefore, more new sets of actual operating data need to be obtained from PP(M)SB for the network's results of Adaptive Training to converge towards the targeted values.

Table 13. Statistical Measures of Part 2 Data Set B Adaptive Training

Stat Analysis	Tube outlet (to)	Shell outlet (Tout)
	Set B Adaptive	Set B Adaptive
RMSE	11.1462	2.1668
CDC	72.7273	54.5455
R2	0.4378	0.4562

For this study, only *single crude blend ratio* is considered. The ratio of crude blend is taken as 50% Tapis, 38.9% Miri and 11.1% Bintulu Condensate. This is the ratio of crude blend at which fouling rate is suspected to accelerate faster.

All of the data created were tested against the optimum NN model using PLP transfer function configuration with feedback mode at 400 epochs number. The optimum number of neurons used is 28, 15 and 2 for the first, middle and last layer respectively.

As an overall performance depicted in Figure 17, it is recommended that preventive maintenance; either mechanical cleaning or hotmelting will be carried out for Heat Exchanger after 150 operating days when the efficiency drops below 30 %. The minimum efficiency of 30 % is adopted from the technical practice in PP(M)SB. Please refer to Appendix E-1 for the efficiency calculation spreadsheet.

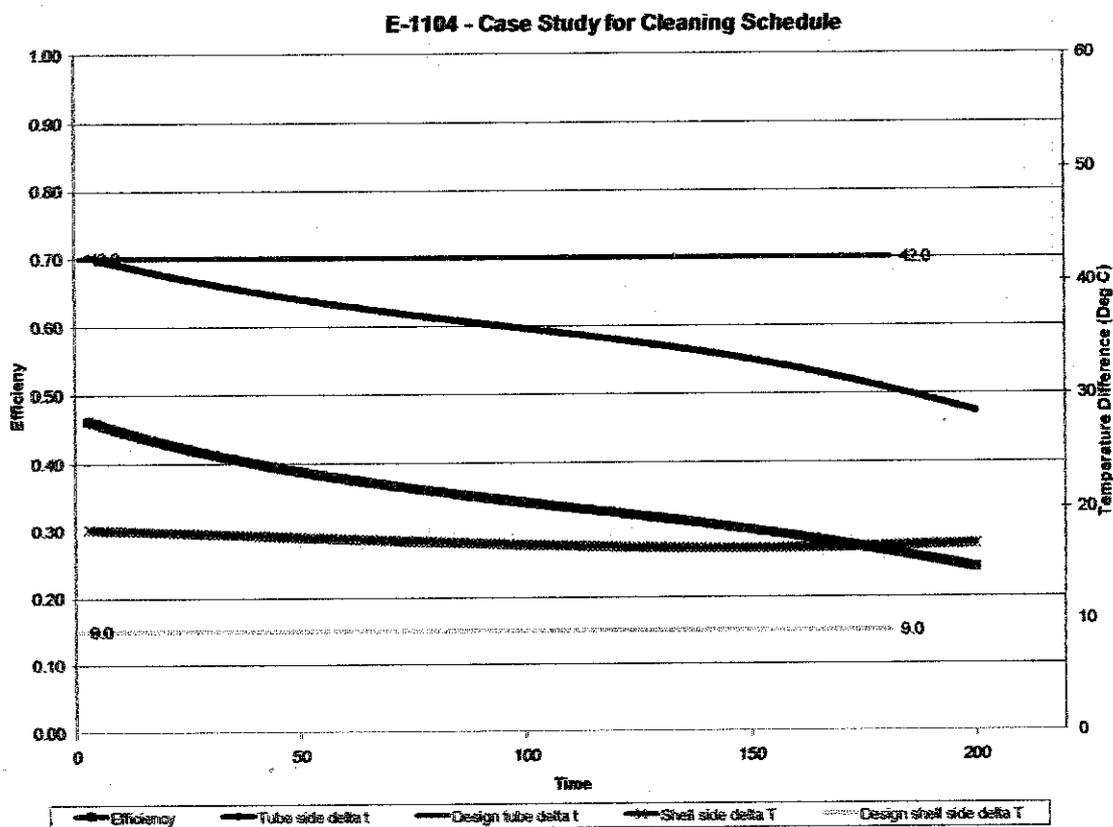


Figure 17. Predicted performance for heat exchanger maintenance scheduling for single crude blend

#### 4.3.2 Case Study 2 ~ Various Crude Blend Ratios

A new set of data has been created based on the actual operation information in PP(M)SB. Most of the predictors (i.e inlet temperatures, average flow rate, crude blend ratio and properties) were kept constant throughout the 200 days. Since the current Neural Network model deals with feedback mode with time lagged by 2 days, the outlet temperatures of both tube and shell side need to be created as the feedback predictors to the model. For this case study, the predictors specifically the tube and shell side integral flow are the accumulative amount of fluid flowing through the equipment and change accordingly with time.

For more realistic operating condition, various crude blend ratios have been used considering 5 main types of crude which are Tapis, Miri, Terengganu Condensate, Bintulu Condensate and Masa crude. For this study, typical ratio of crude blend at which fouling is suspected to accelerate faster has been considered wisely. By philosophy, typical crude blend ratios which accelerate the fouling rate are crude blend containing Tapis crude and Terengganu Condensate. Miri and Masa crude are the light crudes which give the least foul to the heat exchanger

All of the data created were tested against the optimum NN model using PLP transfer function configuration with feedback mode at 400 epochs number. The optimum number of neurons used is 28, 15 and 2 for the first, middle and last layer respectively.

As an overall performance depicted in Figure 18, it is recommended that preventive maintenance; either mechanical cleaning or hotmelting will be carried out for Heat Exchanger after **84 operating days** when the efficiency drops below 30 %. The minimum efficiency of 30 % is adopted from the technical practice in PP(M)SB. Please refer to Appendix E-2 for the efficiency calculation spreadsheet.

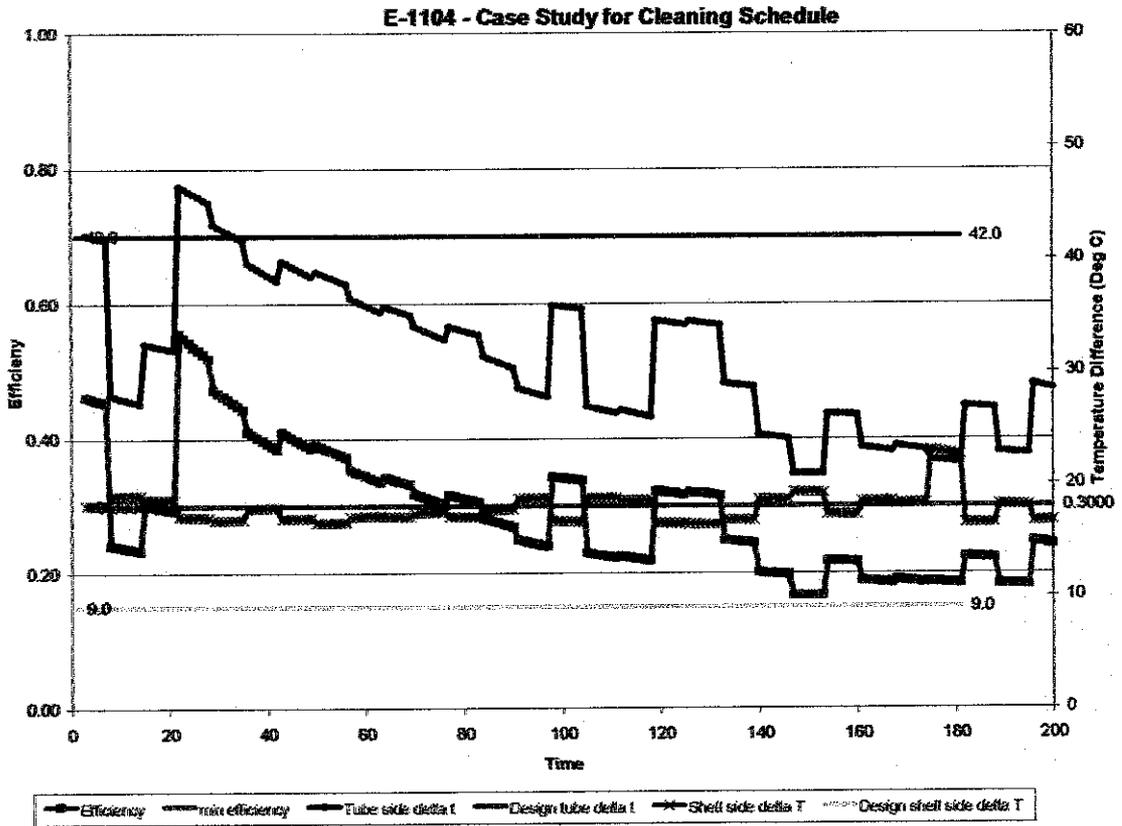


Figure 18. Predicted performance for E-1104 maintenance scheduling for various crude blend

## CHAPTER 5

### CONCLUSION AND RECOMMENDATION

#### 5.1 CONCLUSION

The final draft dissertation of the Final Year Research Project entitled 'Heat Exchanger Modeling by Neural Network Optimization for PETRONAS Penapisan Melaka Sdn. Bhd (PPMSB) Crude Preheat Train' has successfully completed and the objectives set up earlier have been achieved within the given time frame. Systematic step by step optimization strategies have been conducted and a new optimized NN predictive model has been successfully constructed that consist of the following features:

- i. New NN predictive model with current 28 variables, using PLP transfer function configurations and epochs number of 400.
- ii. Introduction of feedback variables for both tube side and shell side outlet temperature with time lagged by two days able to reduce error in the predicted values significantly.
- iii. Significant improvement in tube side outlet temperature ( $t_o$ ) for Data Set B provided RMSE value is reduced by half.
- iv. Slight increment in the RMSE value of the shell side predicted outlet temperature ( $T_o$ ) but within acceptable values.

The optimization strategies conducted has enhanced the robustness of the NN model in predicting in future. Two case studies on heat exchanger maintenance scenario have been developed using the optimized model considering single crude blend and various crude blend ratio.

All in all, it can be concluded that the optimized model has performed well and this study can be used as reference for future development of NN application in the Heat Exchanger maintenance scheduling and as well for interconnection of heat exchanger in the Crude Preheat Train network model.

## **5.2 RECOMMENDATION ON PATH FORWARDS**

Due to the limited time frame and knowledge constraints, there are few plans set earlier that the author has not been able to incorporate into this Final Year Research Project. As for any projects, there are still some rooms for improvement hence the followings are few recommendations to be considered for the future betterment of the Neural Network performance:

- i. Back to the first principles and performs thorough study on the fouling of heat exchanger and fouling mitigation technique for better heat recovery system in the Crude Preheat Train.
- ii. Develop and construct the Neural Network predictive model for all eleven heat exchangers in the Crude Preheat Train.
- iii. Develop framework for interconnection of all eleven heat exchangers in the Crude Preheat Train for preventive maintenance scheduling in the real industrial applications.
- iv. Further optimization of the existing feedback model by changing the transfer function configurations and number of neurons in the hidden layer. Best combinations of transfer function will be hidden layers of sigmoid function followed by output layers of linear neurons for feedforward back propagation Neural Network Architecture.

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## **APPENDICES**

### **Appendix A: NFIT monitoring approach in the Ebert and Panchal Model**

**A-1 Preheat exchanger network scheme**

**A-2 Trend on heat exchanger fouling rates**

### **Appendix B: Plots of temperature coefficient of correlation, $R^2$ for new NN model with 24 predictors (Data Set B)**

**B-1 Tube side temperature coefficient of correlation**

**B-2 Shell side temperature coefficient of correlation**

### **Appendix C: NN Feedback Model with Time Lagged**

**C-1 Training, Validation and Testing Data sets of Feedback mode**

**C-2 Simplified diagram of NN Feedback Model mechanism**

**C-3 Performance Curve of NN Feedback Model**

**C-4 Optimum Neural Network Configuration**

### **Appendix D: Graphs of simulated results generated from NN Feedback Model with Time Lagged by 2 days (Data Set B)**

**D-1 Plots of tube side temperature coefficient of correlation for PLP**

**D-2 Plots of shell side temperature coefficient of correlation for PLP**

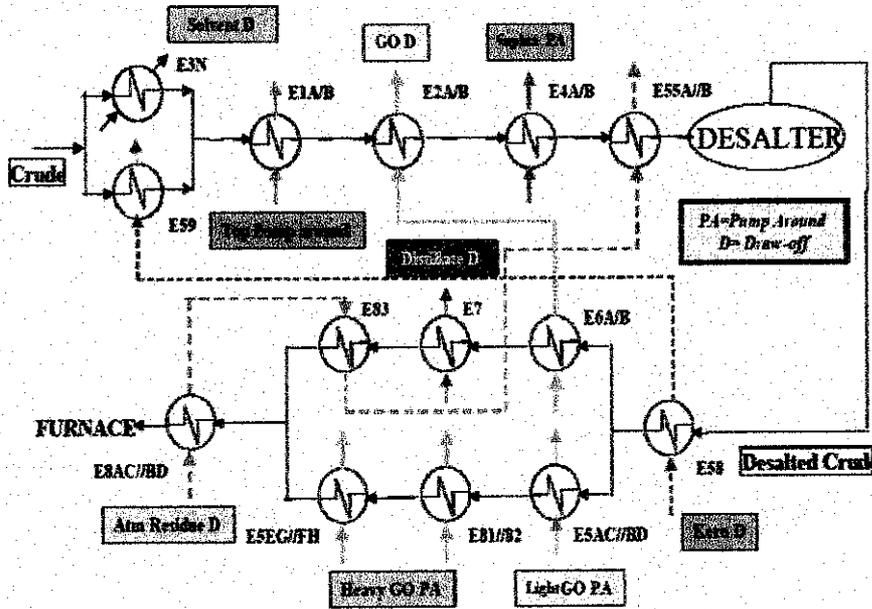
### **Appendix E: Case Study Heat Exchanger Efficiency Calculation Spreadsheets**

**E-1 Heat Exchanger Efficiency for Case Study 1**

**E-2 Heat Exchanger Efficiency for Case Study 2**

## Appendix A: NFFT monitoring approach in the Ebert and Panchal Model

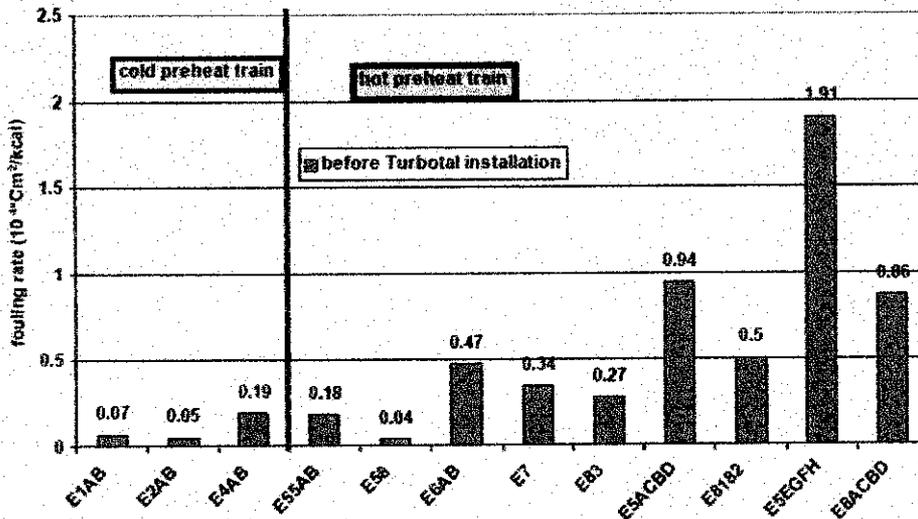
### A-1 Preheat exchanger network scheme



Legend of the diagram:

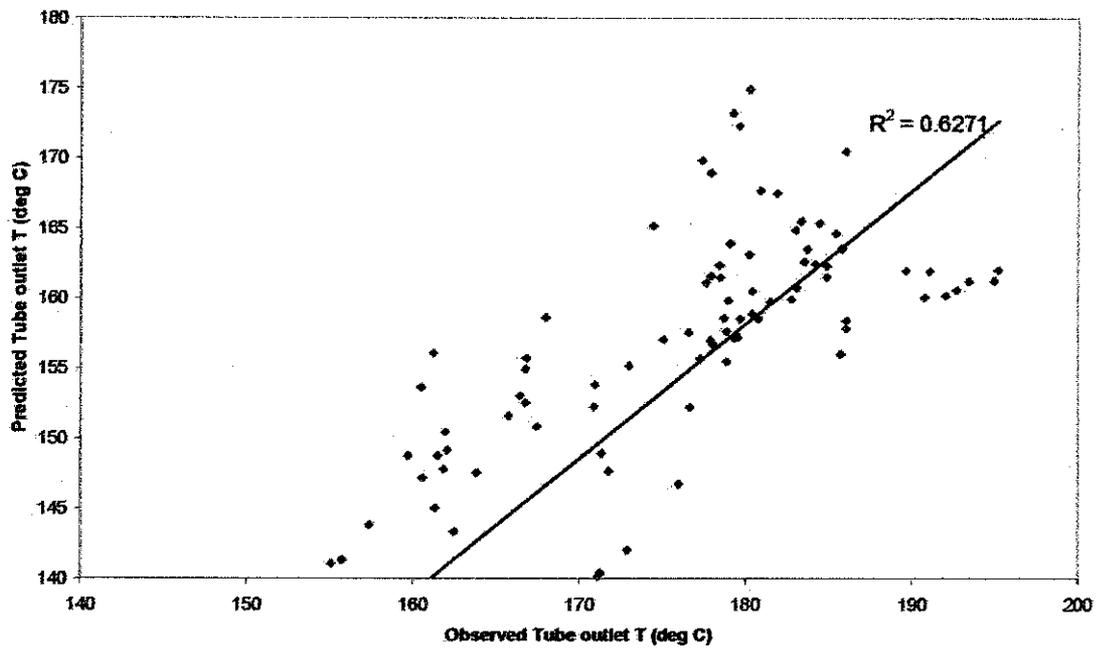
- i. The Pre Desalter E55A/B is the Cold Atmospheric Residue D heat exchanger.
- ii. The E8AC//BD (near the furnace) is the Hot Atmospheric Residue D heat exchanger.

### A-2 Trend on heat exchanger fouling rates

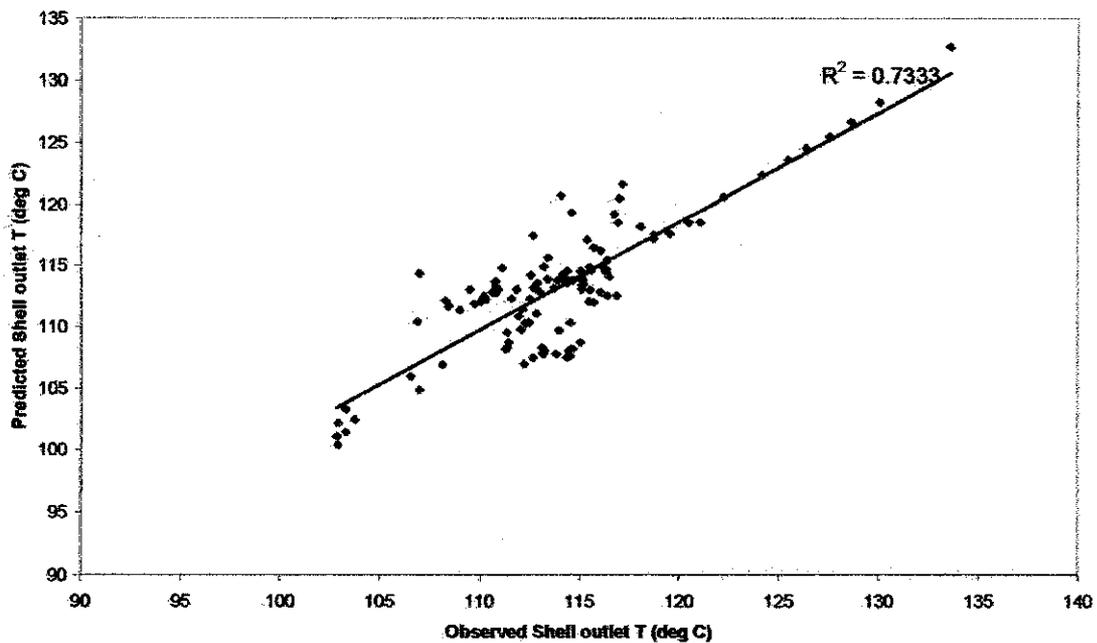


**Appendix B: Plots of temperature coefficient of correlation,  $R^2$  for new NN model with 24 predictors (Data Set B)**

**B-1 Tube side temperature coefficient of correlation**



**B-2 Shell side temperature coefficient of correlation**





0.4640	0.4641	0.4642	0.4643	0.4644	0.4645	0.4646	0.4647	0.4648	0.4649	0.4650	0.4651	0.4652	0.4653	0.4654	0.4655	0.4656	0.4657	0.4658	0.4659	0.4660	0.4661	0.4662	0.4663	0.4664	0.4665	0.4666	0.4667	0.4668	0.4669	0.4670	0.4671	0.4672	0.4673	0.4674	0.4675	0.4676	0.4677	0.4678	0.4679	0.4680	0.4681	0.4682	0.4683	0.4684	0.4685	0.4686	0.4687	0.4688	0.4689	0.4690	0.4691	0.4692	0.4693	0.4694	0.4695	0.4696	0.4697	0.4698	0.4699	0.4700	0.4701	0.4702	0.4703	0.4704	0.4705	0.4706	0.4707	0.4708	0.4709	0.4710	0.4711	0.4712	0.4713	0.4714	0.4715	0.4716	0.4717	0.4718	0.4719	0.4720	0.4721	0.4722	0.4723	0.4724	0.4725	0.4726	0.4727	0.4728	0.4729	0.4730	0.4731	0.4732	0.4733	0.4734	0.4735	0.4736	0.4737	0.4738	0.4739	0.4740	0.4741	0.4742	0.4743	0.4744	0.4745	0.4746	0.4747	0.4748	0.4749	0.4750	0.4751	0.4752	0.4753	0.4754	0.4755	0.4756	0.4757	0.4758	0.4759	0.4760	0.4761	0.4762	0.4763	0.4764	0.4765	0.4766	0.4767	0.4768	0.4769	0.4770	0.4771	0.4772	0.4773	0.4774	0.4775	0.4776	0.4777	0.4778	0.4779	0.4780	0.4781	0.4782	0.4783	0.4784	0.4785	0.4786	0.4787	0.4788	0.4789	0.4790	0.4791	0.4792	0.4793	0.4794	0.4795	0.4796	0.4797	0.4798	0.4799	0.4800	0.4801	0.4802	0.4803	0.4804	0.4805	0.4806	0.4807	0.4808	0.4809	0.4810	0.4811	0.4812	0.4813	0.4814	0.4815	0.4816	0.4817	0.4818	0.4819	0.4820	0.4821	0.4822	0.4823	0.4824	0.4825	0.4826	0.4827	0.4828	0.4829	0.4830	0.4831	0.4832	0.4833	0.4834	0.4835	0.4836	0.4837	0.4838	0.4839	0.4840	0.4841	0.4842	0.4843	0.4844	0.4845	0.4846	0.4847	0.4848	0.4849	0.4850	0.4851	0.4852	0.4853	0.4854	0.4855	0.4856	0.4857	0.4858	0.4859	0.4860	0.4861	0.4862	0.4863	0.4864	0.4865	0.4866	0.4867	0.4868	0.4869	0.4870	0.4871	0.4872	0.4873	0.4874	0.4875	0.4876	0.4877	0.4878	0.4879	0.4880	0.4881	0.4882	0.4883	0.4884	0.4885	0.4886	0.4887	0.4888	0.4889	0.4890	0.4891	0.4892	0.4893	0.4894	0.4895	0.4896	0.4897	0.4898	0.4899	0.4900	0.4901	0.4902	0.4903	0.4904	0.4905	0.4906	0.4907	0.4908	0.4909	0.4910	0.4911	0.4912	0.4913	0.4914	0.4915	0.4916	0.4917	0.4918	0.4919	0.4920	0.4921	0.4922	0.4923	0.4924	0.4925	0.4926	0.4927	0.4928	0.4929	0.4930	0.4931	0.4932	0.4933	0.4934	0.4935	0.4936	0.4937	0.4938	0.4939	0.4940	0.4941	0.4942	0.4943	0.4944	0.4945	0.4946	0.4947	0.4948	0.4949	0.4950	0.4951	0.4952	0.4953	0.4954	0.4955	0.4956	0.4957	0.4958	0.4959	0.4960	0.4961	0.4962	0.4963	0.4964	0.4965	0.4966	0.4967	0.4968	0.4969	0.4970	0.4971	0.4972	0.4973	0.4974	0.4975	0.4976	0.4977	0.4978	0.4979	0.4980	0.4981	0.4982	0.4983	0.4984	0.4985	0.4986	0.4987	0.4988	0.4989	0.4990	0.4991	0.4992	0.4993	0.4994	0.4995	0.4996	0.4997	0.4998	0.4999	0.5000
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0.3761	0.448	0.5248	0.6016	0.6784	0.7552	0.8320	0.9088	0.9856	1.0624	1.1392	1.2160	1.2928	1.3696	1.4464	1.5232	1.6000	1.6768	1.7536	1.8304	1.9072	1.9840	2.0608	2.1376	2.2144	2.2912	2.3680	2.4448	2.5216	2.5984	2.6752	2.7520	2.8288	2.9056	2.9824	3.0592	3.1360	3.2128	3.2896	3.3664	3.4432	3.5200	3.5968	3.6736	3.7504	3.8272	3.9040	3.9808	4.0576	4.1344	4.2112	4.2880	4.3648	4.4416	4.5184	4.5952	4.6720	4.7488	4.8256	4.9024	4.9792	5.0560	5.1328	5.2096	5.2864	5.3632	5.4400	5.5168	5.5936	5.6704	5.7472	5.8240	5.9008	5.9776	6.0544	6.1312	6.2080	6.2848	6.3616	6.4384	6.5152	6.5920	6.6688	6.7456	6.8224	6.8992	6.9760	7.0528	7.1296	7.2064	7.2832	7.3600	7.4368	7.5136	7.5904	7.6672	7.7440	7.8208	7.8976	7.9744	8.0512	8.1280	8.2048	8.2816	8.3584	8.4352	8.5120	8.5888	8.6656	8.7424	8.8192	8.8960	8.9728	9.0496	9.1264	9.2032	9.2800	9.3568	9.4336	9.5104	9.5872	9.6640	9.7408	9.8176	9.8944	9.9712	10.0480	10.1248	10.2016	10.2784	10.3552	10.4320	10.5088	10.5856	10.6624	10.7392	10.8160	10.8928	10.9696	11.0464	11.1232	11.2000	11.2768	11.3536	11.4304	11.5072	11.5840	11.6608	11.7376	11.8144	11.8912	11.9680	12.0448	12.1216	12.1984	12.2752	12.3520	12.4288	12.5056	12.5824	12.6592	12.7360	12.8128	12.8896	12.9664	13.0432	13.1200	13.1968	13.2736	13.3504	13.4272	13.5040	13.5808	13.6576	13.7344	13.8112	13.8880	13.9648	14.0416	14.1184	14.1952	14.2720	14.3488	14.4256	14.5024	14.5792	14.6560	14.7328	14.8096	14.8864	14.9632	15.0400	15.1168	15.1936	15.2704	15.3472	15.4240	15.5008	15.5776	15.6544	15.7312	15.8080	15.8848	15.9616	16.0384	16.1152	16.1920	16.2688	16.3456	16.4224	16.4992	16.5760	16.6528	16.7296	16.8064	16.8832	16.9600	17.0368	17.1136	17.1904	17.2672	17.3440	17.4208	17.4976	17.5744	17.6512	17.7280	17.8048	17.8816	17.9584	18.0352	18.1120	18.1888	18.2656	18.3424	18.4192	18.4960	18.5728	18.6496	18.7264	18.8032	18.8800	18.9568	19.0336	19.1104	19.1872	19.2640	19.3408	19.4176	19.4944	19.5712	19.6480	19.7248	19.8016	19.8784	19.9552	20.0320	20.1088	20.1856	20.2624	20.3392	20.4160	20.4928	20.5696	20.6464	20.7232	20.8000	20.8768	20.9536	21.0304	21.1072	21.1840	21.2608	21.3376	21.4144	21.4912	21.5680	21.6448	21.7216	21.7984	21.8752	21.9520	22.0288	22.1056	22.1824	22.2592	22.3360	22.4128	22.4896	22.5664	22.6432	22.7200	22.7968	22.8736	22.9504	23.0272	23.1040	23.1808	23.2576	23.3344	23.4112	23.4880	23.5648	23.6416	23.7184	23.7952	23.8720	23.9488	24.0256	24.1024	24.1792	24.2560	24.3328	24.4096	24.4864	24.5632	24.6400	24.7168	24.7936	24.8704	24.9472	25.0240	25.1008	25.1776	25.2544	25.3312	25.4080	25.4848	25.5616	25.6384	25.7152	25.7920	25.8688	25.9456	26.0224	26.0992	26.1760	26.2528	26.3296	26.4064	26.4832	26.5600	26.6368	26.7136	26.7904	26.8672	26.9440	27.0208	27.0976	27.1744	27.2512	27.3280	27.4048	27.4816	27.5584	27.6352	27.7120	27.7888	27.8656	27.9424	28.0192	28.0960	28.1728	28.2496	28.3264	28.4032	28.4800	28.5568	28.6336	28.7104	28.7872	28.8640	28.9408	29.0176	29.0944	29.1712	29.2480	29.3248	29.4016	29.4784	29.5552	29.6320	29.7088	29.7856	29.8624	29.9392	30.0160	30.0928	30.1696	30.2464	30.3232	30.4000	30.4768	30.5536	30.6304	30.7072	30.7840	30.8608	30.9376	31.0144	31.0912	31.1680	31.2448	31.3216	31.3984	31.4752	31.5520	31.6288	31.7056	31.7824	31.8592	31.9360	32.0128	32.0896	32.1664	32.2432	32.3200	32.3968	32.4736	32.5504	32.6272	32.7040	32.7808	32.8576	32.9344	33.0112	33.0880	33.1648	33.2416	33.3184	33.3952	33.4720	33.5488	33.6256	33.7024	33.7792	33.8560	33.9328	34.0096	34.0864	34.1632	34.2400	34.3168	34.3936	34.4704	34.5472	34.6240	34.7008	34.7776	34.8544	34.9312	35.0080	35.0848	35.1616	35.2384	35.3152	35.3920	35.4688	35.5456	35.6224	35.6992	35.7760	35.8528	35.9296	36.0064	36.0832	36.1600	36.2368	36.3136	36.3904	36.4672	36.5440	36.6208	36.6976	36.7744	36.8512	36.9280	37.0048	37.0816	37.1584	37.2352	37.3120	37.3888	37.4656	37.5424	37.6192	37.6960	37.7728	37.8496	37.9264	38.0032	38.0800	38.1568	38.2336	38.3104	38.3872	38.4640	38.5408	38.6176	38.6944	38.7712	38.8480	38.9248	39.0016	39.0784	39.1552	39.2320	39.3088	39.3856	39.4624	39.5392	39.6160	39.6928	39.7696	39.8464	39.9232	40.0000
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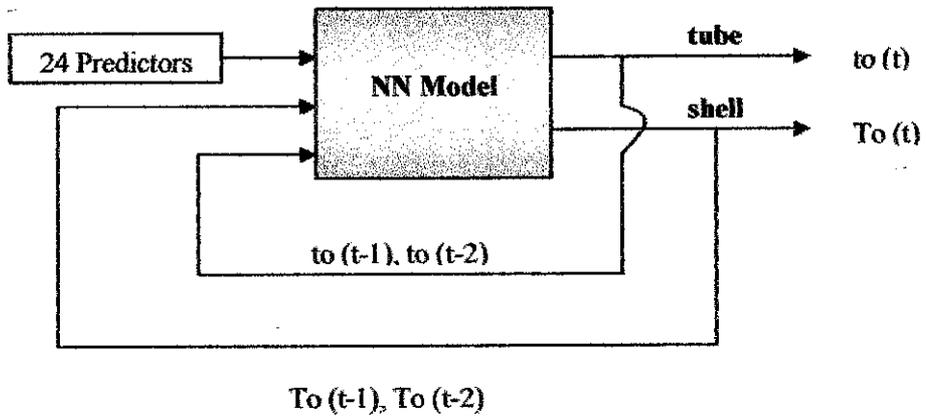




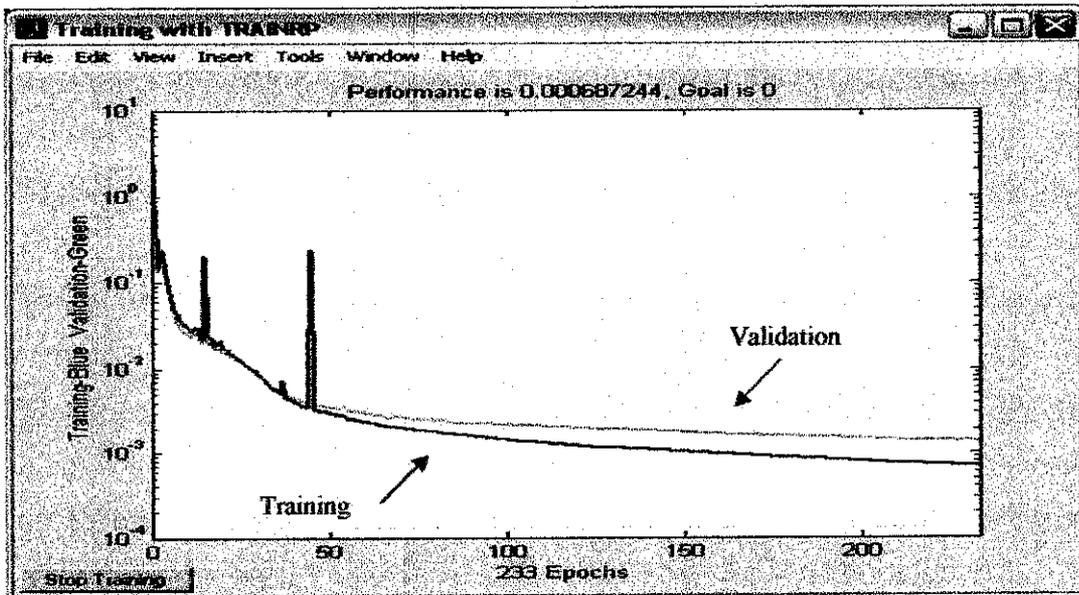


### Appendix C: NN Feedback Model with Time Lagged

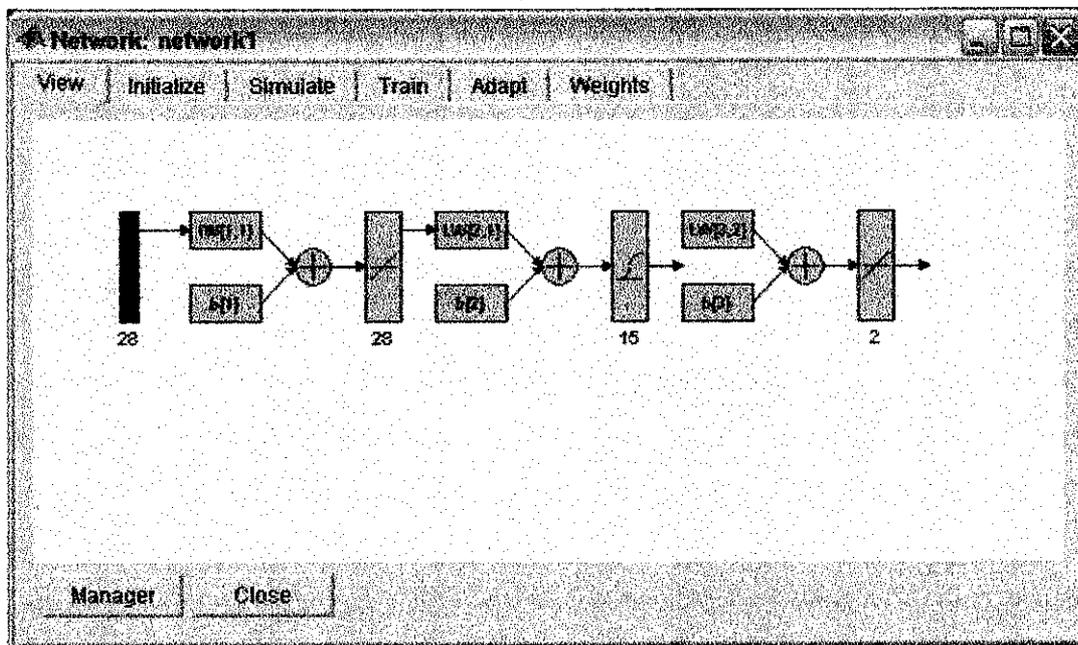
#### C-2 Simplified diagram of NN Feedback Model mechanism



#### C-3 Performance Curve of NN Feedback Model

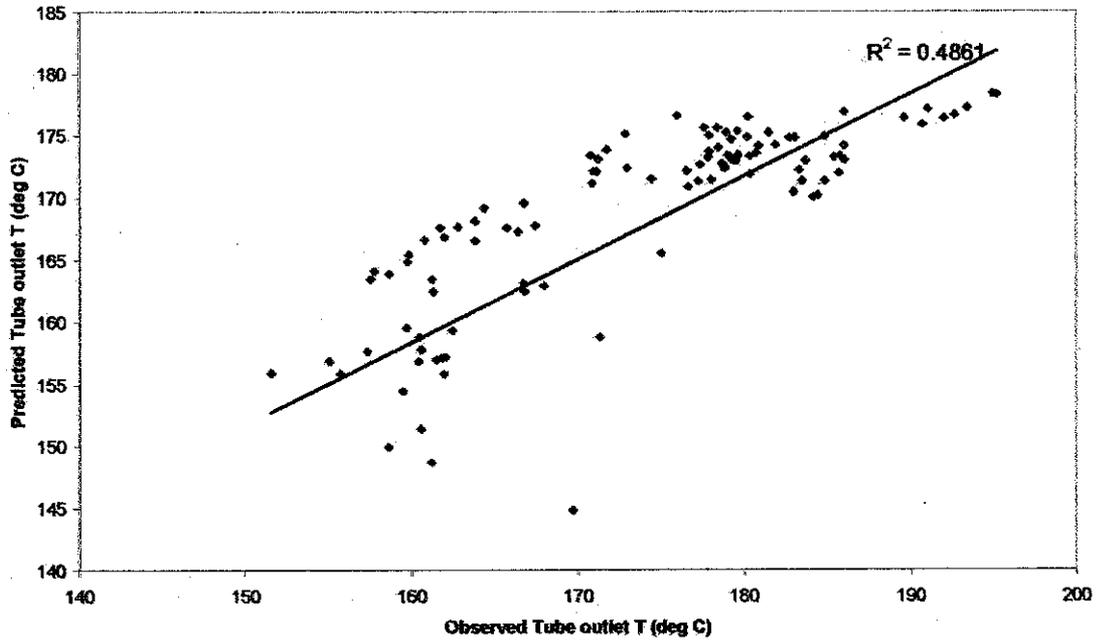


### C-4 Optimum Neural Network Configuration

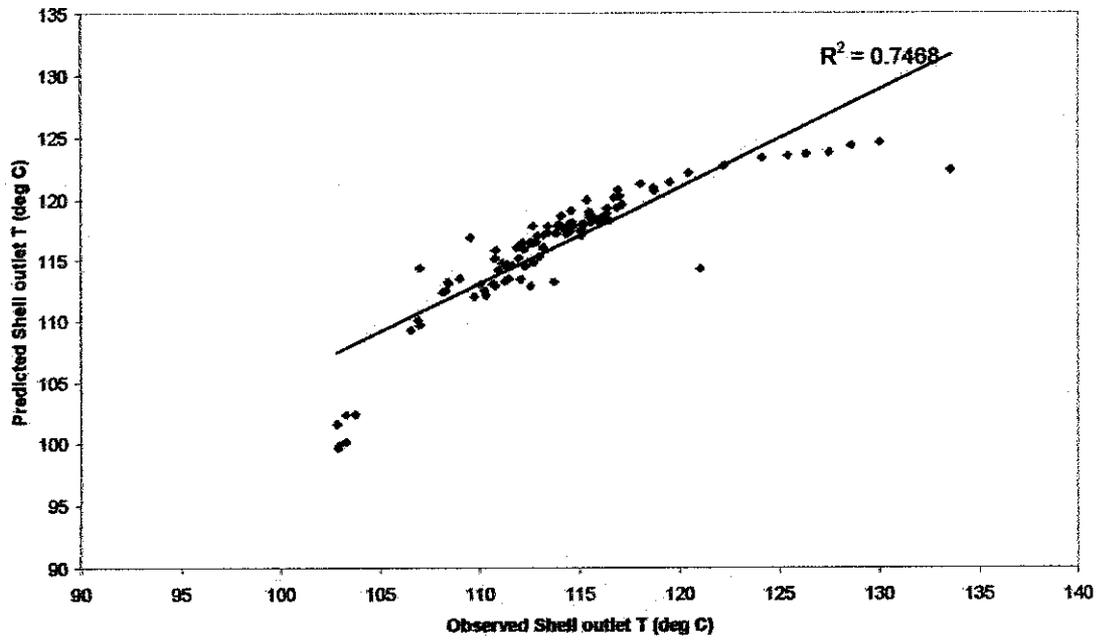


**Appendix D: Graphs of simulated results generated from NN Feedback Model with Time Lagged by 2 days (Data Set B)**

**D-1 Plots of tube side temperature coefficient of correlation for PLP**



**D-2 Plots of shell side temperature coefficient of correlation for PLP**





46	175.00	136.33	38.67	110.00	127.45	17.45	35.90	0.5950	0.4513	0.878	2.6957	640	115.00	106052.98	922.20	0.6572	85562.23	115.00	0.3925
47	175.00	136.39	38.61	110.00	127.44	17.44	35.94	0.5940	0.4516	0.878	2.6912	640	115.00	106052.98	922.20	0.6572	85900.71	114.65	0.3913
48	175.00	136.45	38.55	110.00	127.42	17.42	35.99	0.5930	0.4520	0.878	2.6868	640	115.00	106052.98	922.20	0.6572	86244.02	114.31	0.3901
49	175.00	136.52	38.48	110.00	127.41	17.41	36.03	0.5921	0.4523	0.878	2.6824	640	115.00	106052.98	922.20	0.6572	86584.15	113.96	0.3889
50	175.00	136.58	38.42	110.00	127.39	17.39	36.08	0.5911	0.4527	0.878	2.6780	640	115.00	106052.98	922.20	0.6572	86929.06	113.61	0.3878
51	175.00	136.64	38.36	110.00	127.38	17.38	36.12	0.5901	0.4530	0.878	2.6736	640	115.00	106052.98	922.20	0.6572	87270.82	113.27	0.3866
52	175.00	136.70	38.30	110.00	127.36	17.36	36.16	0.5893	0.4533	0.878	2.6692	640	115.00	106052.98	922.20	0.6572	87609.00	112.92	0.3856
53	175.00	136.76	38.24	110.00	127.34	17.34	36.21	0.5883	0.4536	0.878	2.6653	640	115.00	106052.98	922.20	0.6572	87950.27	112.62	0.3844
54	175.00	136.83	38.17	110.00	127.33	17.33	36.25	0.5873	0.4540	0.879	2.6609	640	115.00	106052.98	922.20	0.6572	88318.26	112.28	0.3832
55	175.00	136.88	38.12	110.00	127.32	17.32	36.29	0.5866	0.4544	0.879	2.6570	640	115.00	106052.98	922.20	0.6572	88681.64	111.98	0.3822
56	175.00	136.94	38.06	110.00	127.30	17.30	36.34	0.5855	0.4546	0.879	2.6528	640	115.00	106052.98	922.20	0.6572	89061.99	111.64	0.3810
57	175.00	137.00	38.00	110.00	127.29	17.29	36.38	0.5846	0.4549	0.879	2.6487	640	115.00	106052.98	922.20	0.6572	89441.45	111.35	0.3800
58	175.00	137.05	37.95	110.00	127.27	17.27	36.42	0.5836	0.4551	0.879	2.6448	640	115.00	106052.98	922.20	0.6572	89817.67	111.05	0.3790
59	175.00	137.12	37.89	110.00	127.25	17.25	36.46	0.5828	0.4555	0.879	2.6404	640	115.00	106052.98	922.20	0.6572	90190.23	110.71	0.3779
60	175.00	137.17	37.83	110.00	127.24	17.24	36.50	0.5819	0.4558	0.879	2.6365	640	115.00	106052.98	922.20	0.6572	90559.36	110.42	0.3769
61	175.00	137.23	37.77	110.00	127.22	17.22	36.55	0.5811	0.4560	0.879	2.6327	640	115.00	106052.98	922.20	0.6572	90928.68	110.12	0.3758
62	175.00	137.28	37.72	110.00	127.21	17.21	36.59	0.5802	0.4563	0.879	2.6288	640	115.00	106052.98	922.20	0.6572	91291.19	109.83	0.3748
63	175.00	137.34	37.66	110.00	127.19	17.19	36.63	0.5794	0.4565	0.879	2.6249	640	115.00	106052.98	922.20	0.6572	91649.51	109.53	0.3738
64	175.00	137.40	37.60	110.00	127.18	17.18	36.67	0.5785	0.4568	0.880	2.6211	640	115.00	106052.98	922.20	0.6572	92014.19	109.24	0.3728
65	175.00	137.45	37.55	110.00	127.16	17.16	36.71	0.5777	0.4571	0.880	2.6172	640	115.00	106052.98	922.20	0.6572	92376.77	107.95	0.3669
66	175.00	137.51	37.49	110.00	127.15	17.15	36.75	0.5768	0.4573	0.880	2.6133	640	115.00	106052.98	922.20	0.6572	92739.81	107.66	0.3661
67	175.00	137.56	37.44	110.00	127.13	17.13	36.79	0.5760	0.4576	0.880	2.6095	640	115.00	106052.98	922.20	0.6572	93103.55	108.66	0.3708
68	175.00	137.62	37.38	110.00	127.12	17.12	36.82	0.5751	0.4579	0.880	2.6056	640	115.00	106052.98	922.20	0.6572	93462.95	108.37	0.3699
69	175.00	137.67	37.33	110.00	127.10	17.10	36.87	0.5743	0.4582	0.880	2.6017	640	115.00	106052.98	922.20	0.6572	93819.78	107.79	0.3679
70	175.00	137.73	37.27	110.00	127.09	17.09	36.91	0.5734	0.4585	0.880	2.5979	640	115.00	106052.98	922.20	0.6572	94179.89	107.50	0.3669
71	175.00	137.78	37.22	110.00	127.07	17.07	36.94	0.5726	0.4588	0.880	2.5946	640	115.00	106052.98	922.20	0.6572	94541.77	107.25	0.3661
72	175.00	137.83	37.17	110.00	127.06	17.06	36.98	0.5718	0.4589	0.880	2.5907	640	115.00	106052.98	922.20	0.6572	94901.28	106.96	0.3651
73	175.00	137.89	37.11	110.00	127.04	17.04	37.02	0.5710	0.4592	0.880	2.5868	640	115.00	106052.98	922.20	0.6572	95268.99	106.68	0.3641
74	175.00	137.93	37.07	110.00	127.03	17.03	37.05	0.5702	0.4594	0.880	2.5835	640	115.00	106052.98	922.20	0.6572	95639.26	106.43	0.3633
75	175.00	137.99	37.01	110.00	127.01	17.01	37.10	0.5694	0.4597	0.881	2.5796	640	115.00	106052.98	922.20	0.6572	96011.40	106.15	0.3623
76	175.00	138.04	36.96	110.00	127.00	17.00	37.13	0.5686	0.4599	0.881	2.5763	640	115.00	106052.98	922.20	0.6572	96383.35	105.62	0.3615
77	175.00	138.09	36.91	110.00	126.98	16.98	37.17	0.5678	0.4602	0.881	2.5725	640	115.00	106052.98	922.20	0.6572	96759.19	105.38	0.3597
78	175.00	138.14	36.86	110.00	126.97	16.97	37.20	0.5670	0.4604	0.881	2.5693	640	115.00	106052.98	922.20	0.6572	97140.10	105.38	0.3587
79	175.00	138.20	36.80	110.00	126.96	16.96	37.24	0.5662	0.4607	0.881	2.5653	640	115.00	106052.98	922.20	0.6572	97526.00	104.85	0.3579
80	175.00	138.24	36.76	110.00	126.94	16.94	37.28	0.5655	0.4608	0.881	2.5620	640	115.00	106052.98	922.20	0.6572	97918.32	104.61	0.3570
81	175.00	138.29	36.71	110.00	126.93	16.93	37.31	0.5647	0.4611	0.881	2.5586	640	115.00	106052.98	922.20	0.6572	98317.18	104.33	0.3563
82	175.00	138.35	36.65	110.00	126.91	16.91	37.35	0.5639	0.4614	0.881	2.5548	640	115.00	106052.98	922.20	0.6572	98722.49	104.09	0.3553
83	175.00	138.39	36.61	110.00	126.90	16.90	37.39	0.5632	0.4616	0.881	2.5515	640	115.00	106052.98	922.20	0.6572	99134.39	103.85	0.3544
84	175.00	138.44	36.56	110.00	126.88	16.88	37.42	0.5624	0.4618	0.881	2.5482	640	115.00	106052.98	922.20	0.6572	99552.01	103.61	0.3536
85	175.00	138.49	36.51	110.00	126.87	16.87	37.46	0.5617	0.4621	0.881	2.5448	640	115.00	106052.98	922.20	0.6572	99976.16	103.34	0.3527
86	175.00	138.55	36.45	110.00	126.86	16.86	37.49	0.5608	0.4624	0.881	2.5410	640	115.00	106052.98	922.20	0.6572	100416.52	103.10	0.3519
87	175.00	138.61	36.41	110.00	126.84	16.84	37.53	0.5601	0.4626	0.882	2.5377	640	115.00	106052.98	922.20	0.6572	100873.27	102.86	0.3511
88	175.00	138.64	36.36	110.00	126.83	16.83	37.56	0.5594	0.4628	0.882	2.5343	640	115.00	106052.98	922.20	0.6572	101346.91	102.62	0.3503
89	175.00	138.69	36.31	110.00	126.81	16.81	37.60	0.5586	0.4630	0.882	2.5310	640	115.00	106052.98	922.20	0.6572	101828.36	102.38	0.3494
90	175.00	138.74	36.26	110.00	126.80	16.80	37.63	0.5579	0.4633	0.882	2.5277	640	115.00	106052.98	922.20	0.6572	102317.54	102.15	0.3486
91	175.00	138.79	36.22	110.00	126.79	16.79	37.67	0.5572	0.4635	0.882	2.5244	640	115.00	106052.98	922.20	0.6572	102814.27	101.91	0.3477
92	175.00	138.84	36.16	110.00	126.77	16.77	37.71	0.5565	0.4638	0.882	2.5215	640	115.00	106052.98	922.20	0.6572	103318.52	101.65	0.3469
93	175.00	138.89	36.11	110.00	126.76	16.76	37.74	0.5556	0.4641	0.882	2.5172	640	115.00	106052.98	922.20	0.6572	103830.15	101.41	0.3461
94	175.00	138.93	36.07	110.00	126.75	16.75	37.77	0.5549	0.4644	0.882	2.5139	640	115.00	106052.98	922.20	0.6572	104349.16	101.18	0.3453
95	175.00	138.98	36.02	110.00	126.73	16.73	37.81	0.5541	0.4645	0.882	2.5106	640	115.00	106052.98	922.20	0.6572	104876.16	100.94	0.3445
96	175.00	139.03	35.97	110.00	126.72	16.72	37.84	0.5534	0.4647	0.882	2.5073	640	115.00	106052.98	922.20	0.6572	105412.33	100.71	0.3437
97	175.00	139.08	35.92	110.00	126.70	16.70	37.88	0.5526	0.4650	0.882	2.5040	640	115.00	106052.98	922.20	0.6572	105958.81	100.48	0.3429
98	175.00	139.12	35.88	110.00	126.69	16.69	37.91	0.5519	0.4653	0.882	2.5006	640	115.00	106052.98	922.20	0.6572	106515.98	100.25	0.3422
99	175.00	139.17	35.83	110.00	126.68	16.68	37.94	0.5512	0.4655	0.882	2.4973	640	115.00	106052.98	922.20	0.6572	107084.33	100.25	0.3422

100	175.00	139.22	35.78	110.00	126.67	16.67	37.98	0.5505	0.4658	0.882	2.4940	640	115.00	106052.98	922.20	0.6572	74415.22	100.02	0.3414
101	175.00	139.27	35.73	110.00	126.66	16.66	38.01	0.5497	0.4661	0.883	2.4937	640	115.00	106052.98	922.20	0.6572	74246.78	99.79	0.3406
102	175.00	139.31	35.69	110.00	126.64	16.64	38.05	0.5490	0.4663	0.883	2.4934	640	115.00	106052.98	922.20	0.6572	74075.41	99.56	0.3398
103	175.00	139.36	35.64	110.00	126.63	16.63	38.08	0.5483	0.4667	0.883	2.4931	640	115.00	106052.98	922.20	0.6572	73907.66	99.34	0.3390
104	175.00	139.42	35.58	110.00	126.62	16.62	38.12	0.5474	0.4670	0.883	2.4928	640	115.00	106052.98	922.20	0.6572	73740.83	99.07	0.3381
105	175.00	139.46	35.54	110.00	126.61	16.61	38.15	0.5467	0.4673	0.883	2.4925	640	115.00	106052.98	922.20	0.6572	73574.94	98.85	0.3374
106	175.00	139.51	35.49	110.00	126.59	16.59	38.18	0.5460	0.4676	0.883	2.4923	640	115.00	106052.98	922.20	0.6572	73409.97	98.62	0.3366
107	175.00	139.56	35.44	110.00	126.58	16.58	38.22	0.5452	0.4679	0.883	2.4920	640	115.00	106052.98	922.20	0.6572	73245.00	98.40	0.3358
108	175.00	139.61	35.39	110.00	126.57	16.57	38.25	0.5445	0.4681	0.883	2.4918	640	115.00	106052.98	922.20	0.6572	73080.55	98.17	0.3351
109	175.00	139.65	35.35	110.00	126.56	16.56	38.28	0.5438	0.4685	0.883	2.4916	640	115.00	106052.98	922.20	0.6572	72916.08	97.95	0.3343
110	175.00	139.70	35.30	110.00	126.55	16.55	38.32	0.5430	0.4688	0.883	2.4913	640	115.00	106052.98	922.20	0.6572	72751.74	97.73	0.3335
111	175.00	139.75	35.24	110.00	126.54	16.54	38.35	0.5422	0.4693	0.883	2.4911	640	115.00	106052.98	922.20	0.6572	72587.51	97.47	0.3327
112	175.00	139.81	35.19	110.00	126.53	16.53	38.39	0.5415	0.4696	0.883	2.4908	640	115.00	106052.98	922.20	0.6572	72423.49	97.25	0.3319
113	175.00	139.85	35.15	110.00	126.51	16.51	38.42	0.5407	0.4699	0.883	2.4906	640	115.00	106052.98	922.20	0.6572	72259.54	97.02	0.3311
114	175.00	139.90	35.10	110.00	126.50	16.50	38.45	0.5400	0.4702	0.883	2.4903	640	115.00	106052.98	922.20	0.6572	72095.71	96.80	0.3303
115	175.00	139.96	35.04	110.00	126.49	16.49	38.49	0.5391	0.4705	0.884	2.4901	640	115.00	106052.98	922.20	0.6572	71932.19	96.55	0.3295
116	175.00	140.00	35.00	110.00	126.49	16.49	38.52	0.5384	0.4711	0.884	2.4898	640	115.00	106052.98	922.20	0.6572	71768.99	96.33	0.3288
117	175.00	140.06	34.94	110.00	126.48	16.48	38.56	0.5376	0.4715	0.884	2.4895	640	115.00	106052.98	922.20	0.6572	71606.11	96.08	0.3279
118	175.00	140.11	34.89	110.00	126.46	16.46	38.59	0.5368	0.4719	0.884	2.4892	640	115.00	106052.98	922.20	0.6572	71443.56	95.86	0.3272
119	175.00	140.15	34.85	110.00	126.45	16.45	38.62	0.5361	0.4722	0.884	2.4889	640	115.00	106052.98	922.20	0.6572	71281.34	95.64	0.3264
120	175.00	140.21	34.79	110.00	126.44	16.44	38.66	0.5352	0.4727	0.884	2.4887	640	115.00	106052.98	922.20	0.6572	71119.42	95.39	0.3256
121	175.00	140.27	34.73	110.00	126.44	16.44	38.70	0.5344	0.4732	0.884	2.4884	640	115.00	106052.98	922.20	0.6572	70957.81	95.15	0.3247
122	175.00	140.31	34.69	110.00	126.43	16.43	38.73	0.5337	0.4736	0.884	2.4881	640	115.00	106052.98	922.20	0.6572	70796.59	94.93	0.3240
123	175.00	140.37	34.63	110.00	126.42	16.42	38.76	0.5328	0.4741	0.884	2.4878	640	115.00	106052.98	922.20	0.6572	70635.76	94.68	0.3232
124	175.00	140.42	34.58	110.00	126.41	16.41	38.80	0.5319	0.4746	0.884	2.4875	640	115.00	106052.98	922.20	0.6572	70475.36	94.43	0.3223
125	175.00	140.47	34.53	110.00	126.40	16.40	38.83	0.5312	0.4750	0.884	2.4872	640	115.00	106052.98	922.20	0.6572	70315.42	94.22	0.3216
126	175.00	140.53	34.47	110.00	126.40	16.40	38.87	0.5304	0.4756	0.884	2.4869	640	115.00	106052.98	922.20	0.6572	70155.94	93.98	0.3207
127	175.00	140.58	34.42	110.00	126.39	16.39	38.90	0.5295	0.4762	0.884	2.4866	640	115.00	106052.98	922.20	0.6572	69997.00	93.74	0.3199
128	175.00	140.64	34.36	110.00	126.38	16.38	38.94	0.5287	0.4767	0.884	2.4863	640	115.00	106052.98	922.20	0.6572	69838.68	93.49	0.3191
129	175.00	140.69	34.31	110.00	126.37	16.37	38.97	0.5278	0.4773	0.884	2.4860	640	115.00	106052.98	922.20	0.6572	69680.82	93.25	0.3183
130	175.00	140.75	34.25	110.00	126.36	16.36	39.01	0.5269	0.4779	0.884	2.4857	640	115.00	106052.98	922.20	0.6572	69523.48	93.01	0.3174
131	175.00	140.80	34.20	110.00	126.36	16.36	39.05	0.5261	0.4784	0.884	2.4854	640	115.00	106052.98	922.20	0.6572	69366.74	92.77	0.3166
132	175.00	140.86	34.14	110.00	126.35	16.35	39.08	0.5252	0.4790	0.885	2.4851	640	115.00	106052.98	922.20	0.6572	69210.56	92.53	0.3158
133	175.00	140.92	34.08	110.00	126.35	16.35	39.12	0.5243	0.4797	0.885	2.4848	640	115.00	106052.98	922.20	0.6572	69054.94	92.25	0.3149
134	175.00	140.98	34.02	110.00	126.34	16.34	39.15	0.5234	0.4804	0.885	2.4845	640	115.00	106052.98	922.20	0.6572	68899.88	92.02	0.3140
135	175.00	141.03	33.97	110.00	126.34	16.34	39.19	0.5226	0.4810	0.885	2.4842	640	115.00	106052.98	922.20	0.6572	68745.38	91.78	0.3132
136	175.00	141.10	33.90	110.00	126.33	16.33	39.23	0.5216	0.4818	0.885	2.4839	640	115.00	106052.98	922.20	0.6572	68591.48	91.51	0.3123
137	175.00	141.15	33.85	110.00	126.33	16.33	39.26	0.5207	0.4825	0.885	2.4836	640	115.00	106052.98	922.20	0.6572	68438.18	91.27	0.3115
138	175.00	141.22	33.78	110.00	126.32	16.32	39.30	0.5197	0.4832	0.885	2.4833	640	115.00	106052.98	922.20	0.6572	68285.48	91.00	0.3106
139	175.00	141.28	33.72	110.00	126.32	16.32	39.34	0.5188	0.4840	0.885	2.4830	640	115.00	106052.98	922.20	0.6572	68133.34	90.74	0.3097
140	175.00	141.34	33.66	110.00	126.32	16.32	39.38	0.5178	0.4848	0.885	2.4827	640	115.00	106052.98	922.20	0.6572	67981.74	90.47	0.3088
141	175.00	141.41	33.59	110.00	126.31	16.31	39.42	0.5168	0.4856	0.885	2.4824	640	115.00	106052.98	922.20	0.6572	67830.74	90.21	0.3079
142	175.00	141.47	33.53	110.00	126.31	16.31	39.45	0.5158	0.4865	0.885	2.4821	640	115.00	106052.98	922.20	0.6572	67680.36	89.95	0.3070
143	175.00	141.53	33.47	110.00	126.31	16.31	39.49	0.5149	0.4873	0.885	2.4818	640	115.00	106052.98	922.20	0.6572	67530.64	89.68	0.3061
144	175.00	141.60	33.40	110.00	126.31	16.31	39.53	0.5139	0.4881	0.885	2.4815	640	115.00	106052.98	922.20	0.6572	67381.58	89.42	0.3052
145	175.00	141.66	33.34	110.00	126.31	16.31	39.57	0.5129	0.4890	0.885	2.4812	640	115.00	106052.98	922.20	0.6572	67233.14	89.16	0.3043
146	175.00	141.73	33.27	110.00	126.30	16.30	39.61	0.5118	0.4898	0.885	2.4809	640	115.00	106052.98	922.20	0.6572	67085.34	88.87	0.3033
147	175.00	141.79	33.21	110.00	126.30	16.30	39.65	0.5108	0.4907	0.885	2.4806	640	115.00	106052.98	922.20	0.6572	66938.14	88.61	0.3024
148	175.00	141.87	33.13	110.00	126.30	16.30	39.69	0.5097	0.4916	0.886	2.4803	640	115.00	106052.98	922.20	0.6572	66791.54	88.32	0.3014
149	175.00	141.94	33.06	110.00	126.30	16.30	39.73	0.5087	0.4924	0.886	2.4800	640	115.00	106052.98	922.20	0.6572	66645.54	88.04	0.3005
150	175.00	142.01	32.99	110.00	126.30	16.30	39.77	0.5076	0.4931	0.886	2.4797	640	115.00	106052.98	922.20	0.6572	66499.94	87.75	0.2996
151	175.00	142.07	32.93	110.00	126.30	16.30	39.81	0.5066	0.4939	0.886	2.4794	640	115.00	106052.98	922.20	0.6572	66354.74	87.49	0.2986
152	175.00	142.15	32.85	110.00	126.30	16.30	39.85	0.5054	0.4948	0.886	2.4791	640	115.00	106052.98	922.20	0.6572	66209.94	87.18	0.2975
153	175.00	142.22	32.78	110.00	126.31	16.31	39.89	0.5043	0.4955	0.886	2.4788	640	115.00	106052.98	922.20	0.6572	66065.54	86.89	0.2966

184	175.00	142.29	32.71	110.00	126.31	16.31	39.93	0.5032	0.4966	0.886	2.2796	640	115.00	106052.98	922.20	0.6572	64438.22	86.61	0.2856
185	175.00	142.31	32.63	110.00	126.31	16.31	39.97	0.5021	0.4997	0.886	2.2747	640	115.00	106052.98	922.20	0.6572	64429.92	86.33	0.2846
186	175.00	142.44	32.56	110.00	126.31	16.31	40.02	0.5008	0.5010	0.886	2.2691	640	115.00	106052.98	922.20	0.6572	63996.05	86.02	0.2936
187	175.00	142.52	32.48	110.00	126.31	16.31	40.06	0.4996	0.5023	0.886	2.2636	640	115.00	106052.98	922.20	0.6572	63765.92	85.71	0.2925
188	175.00	142.60	32.40	110.00	126.32	16.32	40.10	0.4985	0.5035	0.886	2.2587	640	115.00	106052.98	922.20	0.6572	63558.84	85.43	0.2916
189	175.00	142.67	32.33	110.00	126.32	16.32	40.15	0.4973	0.5048	0.886	2.2531	640	115.00	106052.98	922.20	0.6572	63329.48	85.12	0.2905
190	175.00	142.75	32.25	110.00	126.32	16.32	40.19	0.4961	0.5062	0.886	2.2476	640	115.00	106052.98	922.20	0.6572	63100.72	84.81	0.2895
191	175.00	142.83	32.17	110.00	126.33	16.33	40.23	0.4949	0.5077	0.886	2.2421	640	115.00	106052.98	922.20	0.6572	62875.24	84.51	0.2884
192	175.00	142.91	32.09	110.00	126.33	16.33	40.28	0.4937	0.5090	0.886	2.2366	640	115.00	106052.98	922.20	0.6572	62647.68	84.20	0.2874
193	175.00	143.00	32.00	110.00	126.34	16.34	40.33	0.4925	0.5105	0.886	2.2310	640	115.00	106052.98	922.20	0.6572	62397.79	83.87	0.2862
194	175.00	143.08	31.92	110.00	126.34	16.34	40.37	0.4911	0.5120	0.886	2.2250	640	115.00	106052.98	922.20	0.6572	62174.11	83.57	0.2852
195	175.00	143.17	31.83	110.00	126.35	16.35	40.41	0.4898	0.5136	0.887	2.2189	640	115.00	106052.98	922.20	0.6572	61928.20	83.24	0.2841
196	175.00	143.25	31.75	110.00	126.35	16.35	40.46	0.4885	0.5151	0.887	2.2133	640	115.00	106052.98	922.20	0.6572	61705.72	82.94	0.2831
197	175.00	143.33	31.67	110.00	126.36	16.36	40.50	0.4872	0.5166	0.887	2.2073	640	115.00	106052.98	922.20	0.6572	61458.53	82.61	0.2819
198	175.00	143.42	31.58	110.00	126.37	16.37	40.55	0.4858	0.5183	0.887	2.2012	640	115.00	106052.98	922.20	0.6572	61214.63	82.28	0.2808
199	175.00	143.51	31.49	110.00	126.38	16.38	40.60	0.4845	0.5201	0.887	2.1951	640	115.00	106052.98	922.20	0.6572	60973.97	81.95	0.2797
200	175.00	143.59	31.41	110.00	126.39	16.39	40.64	0.4832	0.5217	0.887	2.1890	640	115.00	106052.98	922.20	0.6572	60731.41	81.63	0.2786
171	175.00	143.69	31.31	110.00	126.39	16.39	40.69	0.4817	0.5235	0.887	2.1824	640	115.00	106052.98	922.20	0.6572	60467.10	81.27	0.2774
172	175.00	143.78	31.22	110.00	126.40	16.40	40.74	0.4804	0.5253	0.887	2.1763	640	115.00	106052.98	922.20	0.6572	60228.47	80.95	0.2763
173	175.00	143.86	31.14	110.00	126.41	16.41	40.78	0.4790	0.5270	0.887	2.1703	640	115.00	106052.98	922.20	0.6572	59987.97	80.63	0.2752
174	175.00	143.94	31.04	110.00	126.42	16.42	40.83	0.4776	0.5290	0.887	2.1636	640	115.00	106052.98	922.20	0.6572	59728.40	80.28	0.2740
175	175.00	144.05	30.95	110.00	126.43	16.43	40.88	0.4761	0.5308	0.887	2.1570	640	115.00	106052.98	922.20	0.6572	59467.09	79.93	0.2728
176	175.00	144.14	30.86	110.00	126.44	16.44	40.93	0.4748	0.5327	0.887	2.1509	640	115.00	106052.98	922.20	0.6572	59231.14	79.61	0.2717
177	175.00	144.24	30.76	110.00	126.45	16.45	40.98	0.4733	0.5346	0.887	2.1443	640	115.00	106052.98	922.20	0.6572	58973.78	79.27	0.2705
178	175.00	144.33	30.67	110.00	126.46	16.46	41.03	0.4718	0.5366	0.887	2.1377	640	115.00	106052.98	922.20	0.6572	58717.17	78.92	0.2694
179	175.00	144.43	30.57	110.00	126.47	16.47	41.08	0.4704	0.5386	0.887	2.1310	640	115.00	106052.98	922.20	0.6572	58461.29	78.58	0.2682
180	175.00	144.53	30.47	110.00	126.48	16.48	41.13	0.4689	0.5406	0.887	2.1238	640	115.00	106052.98	922.20	0.6572	58184.32	78.20	0.2669
181	175.00	144.62	30.38	110.00	126.49	16.49	41.18	0.4673	0.5428	0.888	2.1172	640	115.00	106052.98	922.20	0.6572	57929.98	77.86	0.2657
182	175.00	144.72	30.28	110.00	126.50	16.50	41.23	0.4659	0.5449	0.888	2.1106	640	115.00	106052.98	922.20	0.6572	57676.37	77.52	0.2646
183	175.00	144.81	30.19	110.00	126.51	16.51	41.27	0.4644	0.5471	0.888	2.1040	640	115.00	106052.98	922.20	0.6572	57425.88	77.19	0.2634
184	175.00	144.92	30.08	110.00	126.52	16.52	41.33	0.4628	0.5493	0.888	2.0968	640	115.00	106052.98	922.20	0.6572	57152.12	76.82	0.2622
185	175.00	145.01	29.99	110.00	126.53	16.53	41.38	0.4613	0.5514	0.888	2.0901	640	115.00	106052.98	922.20	0.6572	56900.72	76.48	0.2610
186	175.00	145.12	29.88	110.00	126.55	16.55	41.43	0.4598	0.5537	0.888	2.0830	640	115.00	106052.98	922.20	0.6572	56659.61	76.12	0.2598
187	175.00	145.22	29.78	110.00	126.58	16.56	41.48	0.4582	0.5560	0.888	2.0758	640	115.00	106052.98	922.20	0.6572	56399.61	75.75	0.2585
188	175.00	145.32	29.68	110.00	126.57	16.57	41.53	0.4566	0.5583	0.888	2.0686	640	115.00	106052.98	922.20	0.6572	56089.13	75.39	0.2573
189	175.00	145.42	29.58	110.00	126.58	16.58	41.58	0.4551	0.5605	0.888	2.0620	640	115.00	106052.98	922.20	0.6572	55843.03	75.06	0.2562
190	175.00	145.52	29.48	110.00	126.59	16.59	41.63	0.4535	0.5629	0.888	2.0548	640	115.00	106052.98	922.20	0.6572	55574.11	74.70	0.2549
191	175.00	145.62	29.38	110.00	126.61	16.61	41.68	0.4519	0.5653	0.888	2.0476	640	115.00	106052.98	922.20	0.6572	55308.29	74.34	0.2537
192	175.00	145.73	29.27	110.00	126.63	16.62	41.74	0.4504	0.5676	0.888	2.0404	640	115.00	106052.98	922.20	0.6572	55040.98	73.98	0.2525
193	175.00	145.83	29.17	110.00	126.63	16.63	41.79	0.4488	0.5701	0.888	2.0332	640	115.00	106052.98	922.20	0.6572	54776.74	73.62	0.2513
194	175.00	145.93	29.07	110.00	126.64	16.64	41.84	0.4472	0.5725	0.888	2.0261	640	115.00	106052.98	922.20	0.6572	54511.03	73.27	0.2501
195	175.00	146.04	28.96	110.00	126.66	16.66	41.89	0.4456	0.5750	0.888	2.0189	640	115.00	106052.98	922.20	0.6572	54248.34	72.91	0.2489
196	175.00	146.14	28.86	110.00	126.67	16.67	41.94	0.4440	0.5774	0.888	2.0117	640	115.00	106052.98	922.20	0.6572	53984.20	72.56	0.2476
197	175.00	146.24	28.76	110.00	126.68	16.68	41.99	0.4424	0.5800	0.889	2.0045	640	115.00	106052.98	922.20	0.6572	53723.05	72.21	0.2464
198	175.00	146.34	28.66	110.00	126.69	16.69	42.04	0.4409	0.5824	0.889	1.9973	640	115.00	106052.98	922.20	0.6572	53460.47	71.86	0.2452
199	175.00	146.46	28.54	110.00	126.70	16.70	42.10	0.4393	0.5852	0.889	1.9896	640	115.00	106052.98	922.20	0.6572	53180.23	71.48	0.2440
200	175.00	146.56	28.44	110.00	126.71	16.71	42.15	0.4376	0.5877	0.889	1.9824	640	115.00	106052.98	922.20	0.6572	52919.23	71.13	0.2428



44	175.00	135.44	39.56	110.00	126.90	16.90	35.57	0.6086	0.4273	0.877	2.7575	640	115.00	106052.98	922.20	0.6572	88345.47	118.74	0.4053
45	175.00	135.67	39.33	110.00	126.92	16.92	35.71	0.6051	0.4301	0.878	2.7415	640	115.00	106052.98	922.20	0.6572	87463.77	117.56	0.4012
46	175.00	135.89	39.11	110.00	126.93	16.93	35.84	0.6017	0.4329	0.878	2.7261	640	115.00	106052.98	922.20	0.6572	86621.40	116.43	0.3974
47	175.00	136.12	38.88	110.00	126.95	16.95	35.98	0.5982	0.4358	0.878	2.7100	640	115.00	106052.98	922.20	0.6572	85766.84	115.26	0.3934
48	175.00	136.34	38.66	110.00	126.96	16.96	36.11	0.5947	0.4387	0.879	2.6946	640	115.00	106052.98	922.20	0.6572	84900.67	114.15	0.3896
49	175.00	136.55	38.44	110.00	126.97	16.97	36.24	0.5913	0.4416	0.879	2.6791	640	115.00	106052.98	922.20	0.6572	84112.25	113.05	0.3908
50	175.00	136.76	38.22	110.00	126.98	16.98	36.37	0.5878	0.4445	0.879	2.6637	640	115.00	106052.98	922.20	0.6572	83395.40	111.94	0.3876
51	175.00	136.97	38.00	110.00	126.99	16.99	36.50	0.5843	0.4474	0.879	2.6483	640	115.00	106052.98	922.20	0.6572	82700.00	110.83	0.3845
52	175.00	137.18	37.78	110.00	127.00	17.00	36.63	0.5808	0.4503	0.880	2.6329	640	115.00	106052.98	922.20	0.6572	82026.00	109.72	0.3814
53	175.00	137.39	37.56	110.00	127.01	17.01	36.76	0.5773	0.4532	0.880	2.6175	640	115.00	106052.98	922.20	0.6572	81373.50	108.61	0.3783
54	175.00	137.60	37.34	110.00	127.02	17.02	36.89	0.5738	0.4561	0.880	2.6021	640	115.00	106052.98	922.20	0.6572	80741.50	107.50	0.3752
55	175.00	137.81	37.12	110.00	127.03	17.03	37.02	0.5703	0.4590	0.881	2.5867	640	115.00	106052.98	922.20	0.6572	80129.50	106.39	0.3721
56	175.00	138.02	36.90	110.00	127.04	17.04	37.15	0.5668	0.4619	0.881	2.5713	640	115.00	106052.98	922.20	0.6572	79537.50	105.28	0.3690
57	175.00	138.23	36.68	110.00	127.05	17.05	37.28	0.5633	0.4648	0.881	2.5559	640	115.00	106052.98	922.20	0.6572	78965.50	104.17	0.3659
58	175.00	138.44	36.46	110.00	127.06	17.06	37.41	0.5598	0.4677	0.882	2.5405	640	115.00	106052.98	922.20	0.6572	78413.50	103.06	0.3628
59	175.00	138.65	36.24	110.00	127.07	17.07	37.54	0.5563	0.4706	0.882	2.5251	640	115.00	106052.98	922.20	0.6572	77881.50	101.95	0.3597
60	175.00	138.86	36.02	110.00	127.08	17.08	37.67	0.5528	0.4735	0.882	2.5097	640	115.00	106052.98	922.20	0.6572	77369.50	100.84	0.3566
61	175.00	139.07	35.80	110.00	127.09	17.09	37.80	0.5493	0.4764	0.882	2.4943	640	115.00	106052.98	922.20	0.6572	76877.50	99.73	0.3535
62	175.00	139.28	35.58	110.00	127.10	17.10	37.93	0.5458	0.4793	0.882	2.4789	640	115.00	106052.98	922.20	0.6572	76405.50	98.62	0.3504
63	175.00	139.49	35.36	110.00	127.11	17.11	38.06	0.5423	0.4822	0.882	2.4635	640	115.00	106052.98	922.20	0.6572	75953.50	97.51	0.3473
64	175.00	139.70	35.14	110.00	127.12	17.12	38.19	0.5388	0.4851	0.882	2.4481	640	115.00	106052.98	922.20	0.6572	75521.50	96.40	0.3442
65	175.00	139.91	34.92	110.00	127.13	17.13	38.32	0.5353	0.4880	0.882	2.4327	640	115.00	106052.98	922.20	0.6572	75109.50	95.29	0.3411
66	175.00	140.12	34.70	110.00	127.14	17.14	38.45	0.5318	0.4909	0.882	2.4173	640	115.00	106052.98	922.20	0.6572	74717.50	94.18	0.3380
67	175.00	140.33	34.48	110.00	127.15	17.15	38.58	0.5283	0.4938	0.882	2.4019	640	115.00	106052.98	922.20	0.6572	74345.50	93.07	0.3349
68	175.00	140.54	34.26	110.00	127.16	17.16	38.71	0.5248	0.4967	0.882	2.3865	640	115.00	106052.98	922.20	0.6572	73993.50	91.96	0.3318
69	175.00	140.75	34.04	110.00	127.17	17.17	38.84	0.5213	0.4996	0.882	2.3711	640	115.00	106052.98	922.20	0.6572	73661.50	90.85	0.3287
70	175.00	140.96	33.82	110.00	127.18	17.18	38.97	0.5178	0.5025	0.882	2.3557	640	115.00	106052.98	922.20	0.6572	73349.50	89.74	0.3256
71	175.00	141.17	33.60	110.00	127.19	17.19	39.10	0.5143	0.5054	0.882	2.3403	640	115.00	106052.98	922.20	0.6572	73057.50	88.63	0.3225
72	175.00	141.38	33.38	110.00	127.20	17.20	39.23	0.5108	0.5083	0.882	2.3249	640	115.00	106052.98	922.20	0.6572	72785.50	87.52	0.3194
73	175.00	141.59	33.16	110.00	127.21	17.21	39.36	0.5073	0.5112	0.882	2.3095	640	115.00	106052.98	922.20	0.6572	72533.50	86.41	0.3163
74	175.00	141.80	32.94	110.00	127.22	17.22	39.49	0.5038	0.5141	0.882	2.2941	640	115.00	106052.98	922.20	0.6572	72291.50	85.30	0.3132
75	175.00	142.01	32.72	110.00	127.23	17.23	39.62	0.5003	0.5170	0.882	2.2787	640	115.00	106052.98	922.20	0.6572	72059.50	84.19	0.3101
76	175.00	142.22	32.50	110.00	127.24	17.24	39.75	0.4968	0.5199	0.882	2.2633	640	115.00	106052.98	922.20	0.6572	71837.50	83.08	0.3070
77	175.00	142.43	32.28	110.00	127.25	17.25	39.88	0.4933	0.5228	0.882	2.2479	640	115.00	106052.98	922.20	0.6572	71625.50	81.97	0.3039
78	175.00	142.64	32.06	110.00	127.26	17.26	40.01	0.4898	0.5257	0.882	2.2325	640	115.00	106052.98	922.20	0.6572	71423.50	80.86	0.3008
79	175.00	142.85	31.84	110.00	127.27	17.27	40.14	0.4863	0.5286	0.882	2.2171	640	115.00	106052.98	922.20	0.6572	71231.50	79.75	0.2977
80	175.00	143.06	31.62	110.00	127.28	17.28	40.27	0.4828	0.5315	0.882	2.2017	640	115.00	106052.98	922.20	0.6572	71049.50	78.64	0.2946
81	175.00	143.27	31.40	110.00	127.29	17.29	40.40	0.4793	0.5344	0.882	2.1863	640	115.00	106052.98	922.20	0.6572	70877.50	77.53	0.2915
82	175.00	143.48	31.18	110.00	127.30	17.30	40.53	0.4758	0.5373	0.882	2.1709	640	115.00	106052.98	922.20	0.6572	70715.50	76.42	0.2884
83	175.00	143.69	30.96	110.00	127.31	17.31	40.66	0.4723	0.5402	0.882	2.1555	640	115.00	106052.98	922.20	0.6572	70563.50	75.31	0.2853
84	175.00	143.90	30.74	110.00	127.32	17.32	40.79	0.4688	0.5431	0.882	2.1401	640	115.00	106052.98	922.20	0.6572	70421.50	74.20	0.2822
85	175.00	144.11	30.52	110.00	127.33	17.33	40.92	0.4653	0.5460	0.882	2.1247	640	115.00	106052.98	922.20	0.6572	70289.50	73.09	0.2791
86	175.00	144.32	30.30	110.00	127.34	17.34	41.05	0.4618	0.5489	0.882	2.1093	640	115.00	106052.98	922.20	0.6572	70167.50	71.98	0.2760
87	175.00	144.53	30.08	110.00	127.35	17.35	41.18	0.4583	0.5518	0.882	2.0939	640	115.00	106052.98	922.20	0.6572	70055.50	70.87	0.2729
88	175.00	144.74	29.86	110.00	127.36	17.36	41.31	0.4548	0.5547	0.882	2.0785	640	115.00	106052.98	922.20	0.6572	69953.50	69.76	0.2698
89	175.00	144.95	29.64	110.00	127.37	17.37	41.44	0.4513	0.5576	0.882	2.0631	640	115.00	106052.98	922.20	0.6572	69861.50	68.65	0.2667
90	175.00	145.16	29.42	110.00	127.38	17.38	41.57	0.4478	0.5605	0.882	2.0477	640	115.00	106052.98	922.20	0.6572	69779.50	67.54	0.2636
91	175.00	145.37	29.20	110.00	127.39	17.39	41.70	0.4443	0.5634	0.882	2.0323	640	115.00	106052.98	922.20	0.6572	69707.50	66.43	0.2605
92	175.00	145.58	28.98	110.00	127.40	17.40	41.83	0.4408	0.5663	0.882	2.0169	640	115.00	106052.98	922.20	0.6572	69645.50	65.32	0.2574
93	175.00	145.79	28.76	110.00	127.41	17.41	41.96	0.4373	0.5692	0.882	2.0015	640	115.00	106052.98	922.20	0.6572	69593.50	64.21	0.2543
94	175.00	146.00	28.54	110.00	127.42	17.42	42.09	0.4338	0.5721	0.882	1.9861	640	115.00	106052.98	922.20	0.6572	69551.50	63.10	0.2512
95	175.00	146.21	28.32	110.00	127.43	17.43	42.22	0.4303	0.5750	0.882	1.9707	640	115.00	106052.98	922.20	0.6572	69519.50	61.99	0.2481
96	175.00	146.42	28.10	110.00	127.44	17.44	42.35	0.4268	0.5779	0.882	1.9553	640	115.00	106052.98	922.20	0.6572	69497.50	60.88	0.2450
97	175.00	146.63	27.88	110.00	127.45	17.45	42.48	0.4233	0.5808	0.882	1.9400	640	115.00	106052.98	922.20	0.6572	69485.50	59.77	0.2419

98	175.00	139.14	35.86	110.00	126.69	16.69	37.92	0.5517	0.4655	0.882	2.4995	640	115.00	106052.98	922.20	0.6572	74706.72	100.41	0.3427
99	175.00	139.19	35.81	110.00	126.68	16.68	37.95	0.5510	0.4657	0.882	2.4962	640	115.00	106052.98	922.20	0.6572	74594.34	100.18	0.3419
100	175.00	139.23	35.77	110.00	126.67	16.67	37.99	0.5502	0.4660	0.882	2.4929	640	115.00	106052.98	922.20	0.6572	74362.34	99.95	0.3411
101	175.00	139.28	35.72	110.00	126.66	16.66	38.02	0.5495	0.4663	0.883	2.4896	640	115.00	106052.98	922.20	0.6572	74194.02	99.72	0.3404
102	175.00	139.33	35.67	110.00	126.64	16.64	38.05	0.5488	0.4665	0.883	2.4863	640	115.00	106052.98	922.20	0.6572	74022.75	99.49	0.3396
103	175.00	139.38	35.62	110.00	126.63	16.63	38.09	0.5480	0.4668	0.883	2.4830	640	115.00	106052.98	922.20	0.6572	73851.85	99.26	0.3388
104	175.00	139.42	35.58	110.00	126.62	16.62	38.12	0.5473	0.4671	0.883	2.4796	640	115.00	106052.98	922.20	0.6572	73684.99	99.04	0.3380
105	175.00	148.14	26.86	110.00	128.73	18.73	42.07	0.4133	0.6972	0.888	1.8725	640	115.00	106052.98	922.20	0.6572	50116.58	67.36	0.2299
106	175.00	148.24	26.76	110.00	128.73	18.73	42.13	0.4117	0.7000	0.888	1.8653	640	115.00	106052.98	922.20	0.6572	49856.92	67.01	0.2287
107	175.00	148.33	26.67	110.00	128.73	18.73	42.18	0.4102	0.7025	0.888	1.8587	640	115.00	106052.98	922.20	0.6572	49615.99	66.69	0.2276
108	175.00	148.42	26.57	110.00	128.73	18.73	42.23	0.4088	0.7050	0.888	1.8520	640	115.00	106052.98	922.20	0.6572	49375.75	66.37	0.2265
109	175.00	148.52	26.48	110.00	128.73	18.73	42.28	0.4073	0.7075	0.888	1.8454	640	115.00	106052.98	922.20	0.6572	49136.15	66.04	0.2254
110	175.00	148.61	26.38	110.00	128.73	18.73	42.33	0.4059	0.7101	0.888	1.8388	640	115.00	106052.98	922.20	0.6572	48897.24	65.72	0.2243
111	175.00	148.71	26.29	110.00	128.73	18.73	42.38	0.4044	0.7126	0.888	1.8321	640	115.00	106052.98	922.20	0.6572	48659.00	65.40	0.2232
112	175.00	148.81	26.19	110.00	128.73	18.73	42.43	0.4029	0.7151	0.888	1.8255	640	115.00	106052.98	922.20	0.6572	48420.58	65.08	0.2221
113	175.00	148.91	26.10	110.00	128.73	18.73	42.48	0.4014	0.7176	0.888	1.8189	640	115.00	106052.98	922.20	0.6572	48182.00	64.76	0.2210
114	175.00	149.01	26.00	110.00	128.73	18.73	42.53	0.4000	0.7201	0.888	1.8122	640	115.00	106052.98	922.20	0.6572	47943.51	64.44	0.2199
115	175.00	149.11	25.91	110.00	128.73	18.73	42.58	0.3985	0.7226	0.888	1.8056	640	115.00	106052.98	922.20	0.6572	47705.00	64.12	0.2188
116	175.00	149.21	25.81	110.00	128.73	18.73	42.63	0.3970	0.7251	0.888	1.7990	640	115.00	106052.98	922.20	0.6572	47466.50	63.80	0.2177
117	175.00	149.31	25.72	110.00	128.73	18.73	42.68	0.3955	0.7276	0.888	1.7924	640	115.00	106052.98	922.20	0.6572	47228.00	63.48	0.2166
118	175.00	149.41	25.62	110.00	128.73	18.73	42.73	0.3940	0.7301	0.888	1.7858	640	115.00	106052.98	922.20	0.6572	46989.50	63.16	0.2155
119	175.00	149.51	25.53	110.00	128.73	18.73	42.78	0.3925	0.7326	0.888	1.7792	640	115.00	106052.98	922.20	0.6572	46751.00	62.84	0.2144
120	175.00	149.61	25.43	110.00	128.73	18.73	42.83	0.3910	0.7351	0.888	1.7726	640	115.00	106052.98	922.20	0.6572	46512.50	62.52	0.2133
121	175.00	149.71	25.34	110.00	128.73	18.73	42.88	0.3895	0.7376	0.888	1.7660	640	115.00	106052.98	922.20	0.6572	46274.00	62.20	0.2122
122	175.00	149.81	25.24	110.00	128.73	18.73	42.93	0.3880	0.7401	0.888	1.7594	640	115.00	106052.98	922.20	0.6572	46035.50	61.88	0.2111
123	175.00	149.91	25.15	110.00	128.73	18.73	42.98	0.3865	0.7426	0.888	1.7528	640	115.00	106052.98	922.20	0.6572	45797.00	61.56	0.2100
124	175.00	150.01	25.05	110.00	128.73	18.73	43.03	0.3850	0.7451	0.888	1.7462	640	115.00	106052.98	922.20	0.6572	45558.50	61.24	0.2089
125	175.00	150.11	24.96	110.00	128.73	18.73	43.08	0.3835	0.7476	0.888	1.7396	640	115.00	106052.98	922.20	0.6572	45320.00	60.92	0.2078
126	175.00	150.21	24.86	110.00	128.73	18.73	43.13	0.3820	0.7501	0.888	1.7330	640	115.00	106052.98	922.20	0.6572	45081.50	60.60	0.2067
127	175.00	150.31	24.77	110.00	128.73	18.73	43.18	0.3805	0.7526	0.888	1.7264	640	115.00	106052.98	922.20	0.6572	44843.00	60.28	0.2056
128	175.00	150.41	24.67	110.00	128.73	18.73	43.23	0.3790	0.7551	0.888	1.7198	640	115.00	106052.98	922.20	0.6572	44604.50	59.96	0.2045
129	175.00	150.51	24.58	110.00	128.73	18.73	43.28	0.3775	0.7576	0.888	1.7132	640	115.00	106052.98	922.20	0.6572	44366.00	59.64	0.2034
130	175.00	150.61	24.48	110.00	128.73	18.73	43.33	0.3760	0.7601	0.888	1.7066	640	115.00	106052.98	922.20	0.6572	44127.50	59.32	0.2023
131	175.00	150.71	24.39	110.00	128.73	18.73	43.38	0.3745	0.7626	0.888	1.7000	640	115.00	106052.98	922.20	0.6572	43889.00	59.00	0.2012
132	175.00	150.81	24.29	110.00	128.73	18.73	43.43	0.3730	0.7651	0.888	1.6934	640	115.00	106052.98	922.20	0.6572	43650.50	58.68	0.2001
133	175.00	150.91	24.20	110.00	128.73	18.73	43.48	0.3715	0.7676	0.888	1.6868	640	115.00	106052.98	922.20	0.6572	43412.00	58.36	0.1990
134	175.00	151.01	24.10	110.00	128.73	18.73	43.53	0.3700	0.7701	0.888	1.6802	640	115.00	106052.98	922.20	0.6572	43173.50	58.04	0.1979
135	175.00	151.11	24.01	110.00	128.73	18.73	43.58	0.3685	0.7726	0.888	1.6736	640	115.00	106052.98	922.20	0.6572	42935.00	57.72	0.1968
136	175.00	151.21	23.91	110.00	128.73	18.73	43.63	0.3670	0.7751	0.888	1.6670	640	115.00	106052.98	922.20	0.6572	42696.50	57.40	0.1957
137	175.00	151.31	23.82	110.00	128.73	18.73	43.68	0.3655	0.7776	0.888	1.6604	640	115.00	106052.98	922.20	0.6572	42458.00	57.08	0.1946
138	175.00	151.41	23.72	110.00	128.73	18.73	43.73	0.3640	0.7801	0.888	1.6538	640	115.00	106052.98	922.20	0.6572	42219.50	56.76	0.1935
139	175.00	151.51	23.63	110.00	128.73	18.73	43.78	0.3625	0.7826	0.888	1.6472	640	115.00	106052.98	922.20	0.6572	41981.00	56.44	0.1924
140	175.00	151.61	23.53	110.00	128.73	18.73	43.83	0.3610	0.7851	0.888	1.6406	640	115.00	106052.98	922.20	0.6572	41742.50	56.12	0.1913
141	175.00	151.71	23.44	110.00	128.73	18.73	43.88	0.3595	0.7876	0.888	1.6340	640	115.00	106052.98	922.20	0.6572	41504.00	55.80	0.1902
142	175.00	151.81	23.34	110.00	128.73	18.73	43.93	0.3580	0.7901	0.888	1.6274	640	115.00	106052.98	922.20	0.6572	41265.50	55.48	0.1891
143	175.00	151.91	23.25	110.00	128.73	18.73	43.98	0.3565	0.7926	0.888	1.6208	640	115.00	106052.98	922.20	0.6572	41027.00	55.16	0.1880
144	175.00	152.01	23.15	110.00	128.73	18.73	44.03	0.3550	0.7951	0.888	1.6142	640	115.00	106052.98	922.20	0.6572	40788.50	54.84	0.1869
145	175.00	152.11	23.06	110.00	128.73	18.73	44.08	0.3535	0.7976	0.888	1.6076	640	115.00	106052.98	922.20	0.6572	40550.00	54.52	0.1858
146	175.00	152.21	22.96	110.00	128.73	18.73	44.13	0.3520	0.8001	0.888	1.6010	640	115.00	106052.98	922.20	0.6572	40311.50	54.20	0.1847
147	175.00	152.31	22.87	110.00	128.73	18.73	44.18	0.3505	0.8026	0.888	1.5944	640	115.00	106052.98	922.20	0.6572	40073.00	53.88	0.1836
148	175.00	152.41	22.77	110.00	128.73	18.73	44.23	0.3490	0.8051	0.888	1.5878	640	115.00	106052.98	922.20	0.6572	39834.50	53.56	0.1825
149	175.00	152.51	22.68	110.00	128.73	18.73	44.28	0.3475	0.8076	0.888	1.5812	640	115.00	106052.98	922.20	0.6572	39596.00	53.24	0.1814
150	175.00	152.61	22.58	110.00	128.73	18.73	44.33	0.3460	0.8101	0.888	1.5746	640	115.00	106052.98	922.20	0.6572	39357.50	52.92	0.1803
151	175.00	152.71	22.49	110.00	128.73	18.73	44.38	0.3445	0.8126	0.888	1.5680	640	115.00	106052.98	922.20	0.6572	39119.00	52.60	0.1792

152	175.00	154.10	20.90	110.00	129.19	19.19	44.95	0.3215	0.9185	1.4564	640	115.00	106052.98	922.20	0.6572	36337.16	48.84	0.1667
153	175.00	154.10	20.90	110.00	129.18	19.18	44.95	0.3216	0.9175	1.4570	640	115.00	106052.98	922.20	0.6572	36348.51	48.86	0.1667
154	175.00	148.79	26.21	110.00	127.28	17.28	43.10	0.4033	0.8591	1.8272	640	115.00	106052.98	922.20	0.6572	47646.98	64.04	0.2186
155	175.00	148.80	26.20	110.00	127.27	17.27	43.11	0.4030	0.8593	1.8261	640	115.00	106052.98	922.20	0.6572	47604.35	63.98	0.2181
156	175.00	148.83	26.17	110.00	127.26	17.26	43.13	0.4027	0.8596	1.8244	640	115.00	106052.98	922.20	0.6572	47540.44	63.90	0.2179
157	175.00	148.84	26.16	110.00	127.25	17.25	43.14	0.4024	0.8596	1.8233	640	115.00	106052.98	922.20	0.6572	47497.87	63.84	0.2173
158	175.00	148.86	26.14	110.00	127.24	17.24	43.15	0.4022	0.8597	1.8222	640	115.00	106052.98	922.20	0.6572	47455.33	63.78	0.2177
159	175.00	148.87	26.13	110.00	127.23	17.23	43.17	0.4020	0.8597	1.8211	640	115.00	106052.98	922.20	0.6572	47410.88	63.72	0.2175
160	175.00	148.89	26.10	110.00	127.23	17.23	43.18	0.4016	0.8601	1.8194	640	115.00	106052.98	922.20	0.6572	47349.08	63.64	0.2172
161	175.00	151.62	23.24	110.00	128.44	18.44	44.12	0.3566	0.7934	1.6200	640	115.00	106052.98	922.20	0.6572	41225.44	55.41	0.1991
162	175.00	151.62	23.18	110.00	128.44	18.44	44.15	0.3566	0.7936	1.6156	640	115.00	106052.98	922.20	0.6572	41082.20	55.22	0.1985
163	175.00	151.60	23.12	110.00	128.45	18.45	44.17	0.3557	0.7980	1.6117	640	115.00	106052.98	922.20	0.6572	40958.93	55.05	0.1979
164	175.00	151.64	23.06	110.00	128.45	18.45	44.20	0.3548	0.8003	1.6073	640	115.00	106052.98	922.20	0.6572	40816.12	54.86	0.1972
165	175.00	152.00	23.00	110.00	128.46	18.46	44.23	0.3539	0.8024	1.6034	640	115.00	106052.98	922.20	0.6572	40691.55	54.69	0.1967
166	175.00	152.05	22.95	110.00	128.46	18.46	44.26	0.3531	0.8045	1.6000	640	115.00	106052.98	922.20	0.6572	40567.17	54.53	0.1961
167	175.00	152.11	22.89	110.00	128.47	18.47	44.28	0.3522	0.8066	1.5965	640	115.00	106052.98	922.20	0.6572	40442.96	54.36	0.1955
168	175.00	151.61	23.36	110.00	128.22	18.22	44.14	0.3599	0.7789	1.6305	640	115.00	106052.98	922.20	0.6572	41462.83	55.73	0.1902
169	175.00	151.68	23.32	110.00	128.23	18.23	44.19	0.3588	0.7817	1.6255	640	115.00	106052.98	922.20	0.6572	41304.66	55.52	0.1895
170	175.00	151.75	23.25	110.00	128.24	18.24	44.21	0.3577	0.7845	1.6205	640	115.00	106052.98	922.20	0.6572	41146.76	55.30	0.1888
171	175.00	151.81	23.19	110.00	128.25	18.25	44.24	0.3567	0.7871	1.6161	640	115.00	106052.98	922.20	0.6572	41007.19	55.12	0.1881
172	175.00	151.89	23.11	110.00	128.26	18.26	44.27	0.3556	0.7899	1.6111	640	115.00	106052.98	922.20	0.6572	40848.15	54.90	0.1874
173	175.00	151.95	23.05	110.00	128.27	18.27	44.30	0.3546	0.7925	1.6067	640	115.00	106052.98	922.20	0.6572	40709.02	54.72	0.1867
174	175.00	152.02	22.98	110.00	128.27	18.27	44.33	0.3535	0.7952	1.6018	640	115.00	106052.98	922.20	0.6572	40550.50	54.50	0.1860
175	175.00	152.02	22.98	110.00	128.27	18.27	44.37	0.3526	0.7980	1.5988	640	115.00	106052.98	922.20	0.6572	40789.41	54.82	0.1871
176	175.00	152.06	22.94	110.00	128.28	18.28	44.40	0.3516	0.8008	1.5965	640	115.00	106052.98	922.20	0.6572	40678.64	54.68	0.1866
177	175.00	152.09	22.91	110.00	128.28	18.28	44.43	0.3507	0.8037	1.5945	640	115.00	106052.98	922.20	0.6572	40566.39	54.52	0.1861
178	175.00	153.01	21.99	110.00	132.76	22.76	42.62	0.3383	1.0351	1.5327	640	115.00	106052.98	922.20	0.6572	40474.86	54.40	0.1857
179	175.00	153.04	21.96	110.00	132.69	22.69	42.68	0.3378	1.0333	1.5305	640	115.00	106052.98	922.20	0.6572	40363.20	54.25	0.1852
180	175.00	153.07	21.93	110.00	132.62	22.62	42.73	0.3373	1.0316	1.5283	640	115.00	106052.98	922.20	0.6572	40253.61	54.10	0.1847
181	175.00	153.10	21.90	110.00	132.55	22.55	42.78	0.3370	1.0294	1.5266	640	115.00	106052.98	922.20	0.6572	40161.09	53.98	0.1842
182	175.00	148.08	26.92	110.00	126.52	16.52	43.07	0.4141	0.8137	1.8763	640	115.00	106052.98	922.20	0.6572	48952.11	65.80	0.2246
183	175.00	148.10	26.90	110.00	126.51	16.51	43.09	0.4138	0.8140	1.8745	640	115.00	106052.98	922.20	0.6572	48889.45	65.71	0.2243
184	175.00	148.14	26.86	110.00	126.51	16.51	43.11	0.4133	0.8144	1.8725	640	115.00	106052.98	922.20	0.6572	48807.29	65.60	0.2239
185	175.00	148.17	26.83	110.00	126.50	16.50	43.13	0.4128	0.8149	1.8703	640	115.00	106052.98	922.20	0.6572	48735.21	65.49	0.2235
186	175.00	148.20	26.80	110.00	126.49	16.49	43.15	0.4123	0.8154	1.8680	640	115.00	106052.98	922.20	0.6572	48643.23	65.38	0.2231
187	175.00	148.23	26.77	110.00	126.49	16.49	43.17	0.4118	0.8158	1.8658	640	115.00	106052.98	922.20	0.6572	48561.33	65.27	0.2228
188	175.00	148.26	26.74	110.00	126.48	16.48	43.19	0.4113	0.8163	1.8636	640	115.00	106052.98	922.20	0.6572	48479.52	65.16	0.2224
189	175.00	152.19	22.61	110.00	128.13	18.13	44.49	0.3509	0.7951	1.5895	640	115.00	106052.98	922.20	0.6572	40090.02	53.88	0.1839
190	175.00	152.21	22.75	110.00	128.12	18.12	44.50	0.3506	0.7954	1.5885	640	115.00	106052.98	922.20	0.6572	40047.90	53.83	0.1837
191	175.00	152.23	22.77	110.00	128.11	18.11	44.52	0.3502	0.7954	1.5888	640	115.00	106052.98	922.20	0.6572	39989.59	53.75	0.1834
192	175.00	152.25	22.75	110.00	128.09	18.09	44.54	0.3500	0.7954	1.5885	640	115.00	106052.98	922.20	0.6572	39947.54	53.69	0.1831
193	175.00	152.27	22.73	110.00	128.08	18.08	44.55	0.3498	0.7955	1.5846	640	115.00	106052.98	922.20	0.6572	39907.13	53.64	0.1831
194	175.00	152.28	22.72	110.00	128.07	18.07	44.57	0.3495	0.7954	1.5835	640	115.00	106052.98	922.20	0.6572	39865.53	53.58	0.1829
195	175.00	152.30	22.70	110.00	128.06	18.06	44.58	0.3493	0.7954	1.5824	640	115.00	106052.98	922.20	0.6572	39824.77	53.53	0.1827
196	175.00	146.14	28.86	110.00	126.66	16.66	41.94	0.4440	0.5773	2.0117	640	115.00	106052.98	922.20	0.6572	53961.97	72.56	0.2476
197	175.00	146.14	28.76	110.00	126.63	16.63	41.99	0.4424	0.5795	2.0045	640	115.00	106052.98	922.20	0.6572	53720.84	72.21	0.2464
198	175.00	146.14	28.66	110.00	126.69	16.69	42.05	0.4409	0.5823	1.9973	640	115.00	106052.98	922.20	0.6572	53488.26	71.85	0.2452
199	175.00	146.46	28.54	110.00	126.70	16.70	42.10	0.4391	0.5851	1.9896	640	115.00	106052.98	922.20	0.6572	53178.04	71.48	0.2439
200	175.00	146.56	28.44	110.00	126.71	16.71	42.15	0.4376	0.5875	1.9824	640	115.00	106052.98	922.20	0.6572	52917.06	71.13	0.2427