

# FYP II Final Oral Presentation

Application of corrosion prediction models to optimize material selection in offshore facilities

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# Project Background

Corrosion study - Exploration & Production (E&P) business.

Different **philosophies** of CO<sub>2</sub> corrosion prediction models (ECE4 & MULTICORP).

**Parameters:** partial pressure of CO<sub>2</sub>, H<sub>2</sub>S content, high temperature, pH, iron content and flow velocity.

**Predicted corrosion** (design & operation)– assessed (what parameters are crucial).

Influence on **material selection** and total project **cost**.

# Problem Statement

PETRONAS employs ECE4 and MULTICORP.

Design of project's facilities - integrity and costs.

Proper corrosion prediction is important.

Material selection and project life cycle.

Economic feasibility.

..a multinational O&G company once experienced a **failure** by not taking into consideration one of the parameters.

Paper 05551, CO2 Corrosion Prediction Model-Basic Principles

# Objectives

Study the corrosion **predictions** from both ECE4 and MULTICORP.  
(design & operation phase)

Discuss important **parameters** to come out with the best possible **accuracy** of predicted corrosion.

Proper **material selection** process - **economical** aspect maximized for profit optimization.

## ECE 4

### Alloy Selection

...from input data pH is calculated...consider the **suitability** of 8 corrosion resistant alloys (CRAs)

..identify materials which are **safe or unsafe** in stated conditions.

### Life-Cycle Cost Analysis

Used to give rough indication of relative cost between CRA and carbon steel.

## Corrosion Control in O&G Pipelines.

Report by Rolf Nyborg, Institute for Energy Technology (IFE), Norway

Important aspect in corrosion evaluation...obtain a realistic estimate of the **actual pH** value in the water phase.

..if formation water is produced, it is important to obtain **good water analysis data...bicarbonate and organic acids.**

The actual pH value must be calculated from the **CO<sub>2</sub>** and **H<sub>2</sub>S** partial pressure, temperature, bicarbonate content in the water.

## CO<sub>2</sub> Corrosion Prediction Model – Basic Principles.

Paper No. 05551, NACE International 2005.

### Norsok

Model the effects of **fluid flow** rate since it proved that flow rate influences CO<sub>2</sub> corrosion.

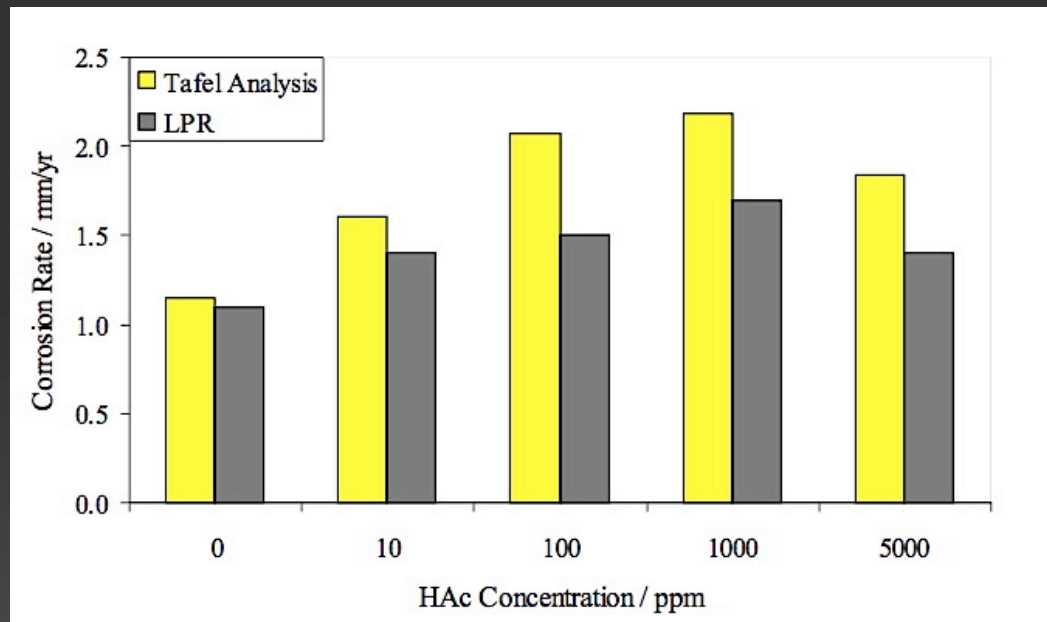
More severe in conditions with high content of **organic acids**. Not suitable for used in produced water environment.

Uncertainties.

## The Effect of Cl<sup>-</sup> and Acetic Acid on Localized CO<sub>2</sub> Corrosion in Wet Gas Flow.

Paper No. Paper 03327, Corrosion in Multiphase Systems Center Institute for Corrosion and Multiphase Technology Ohio University

Localized attack in CO<sub>2</sub> corrosion of mild steel is always associated with the formation and breakdown of **protective iron carbonate** film.



CR is not significantly affected by HAc at room temperature but at high temperature environment.



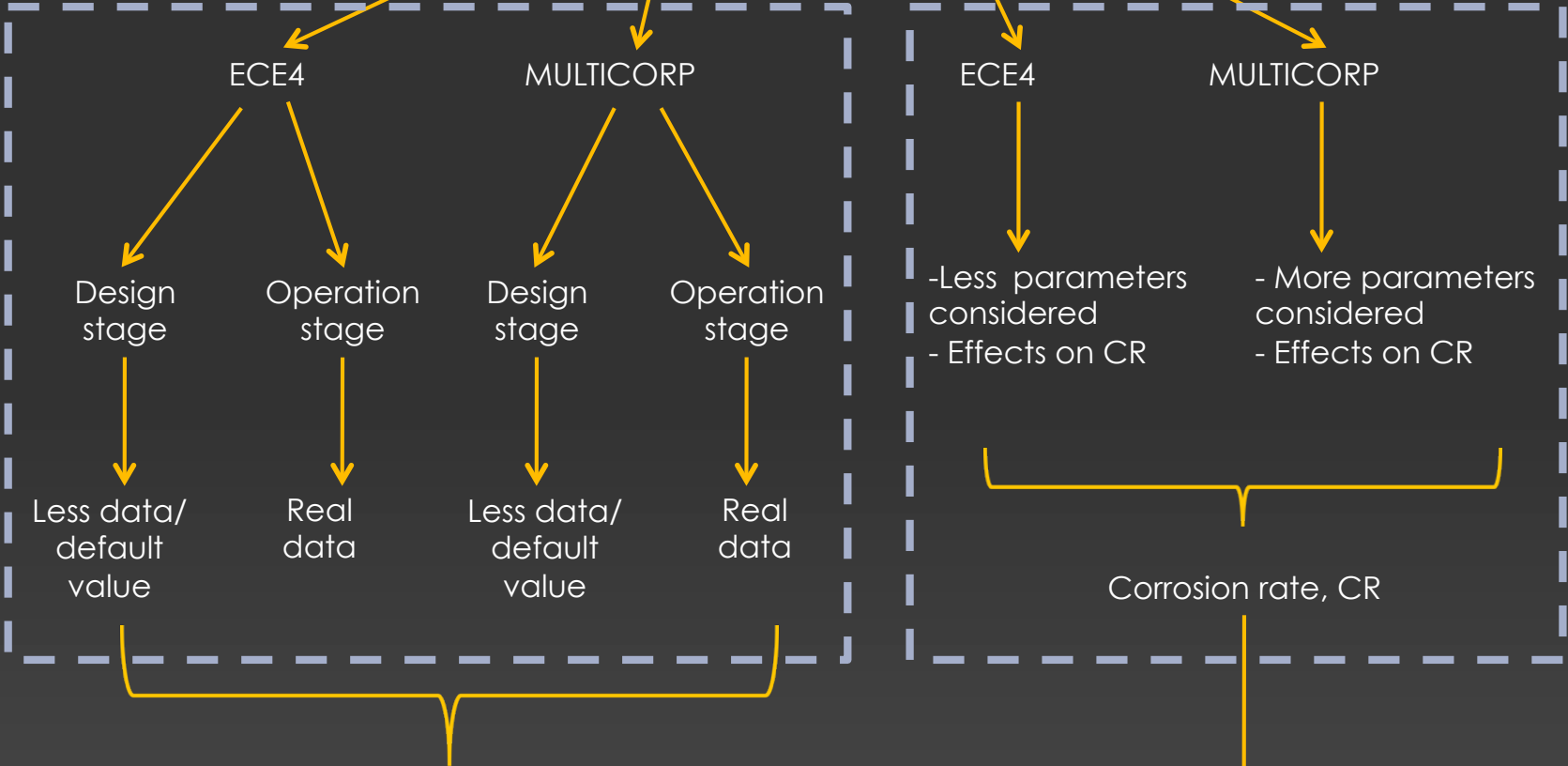
# Methodology

Gather field data.

Two outputs that are desired to be found:

- To compare corrosion predicted from two different models (ECE4 & MULTICORP) by using same well data.
- To compare corrosion predicted in design and operational stage using field data.

Offshore field data



Corrosion rate, CR



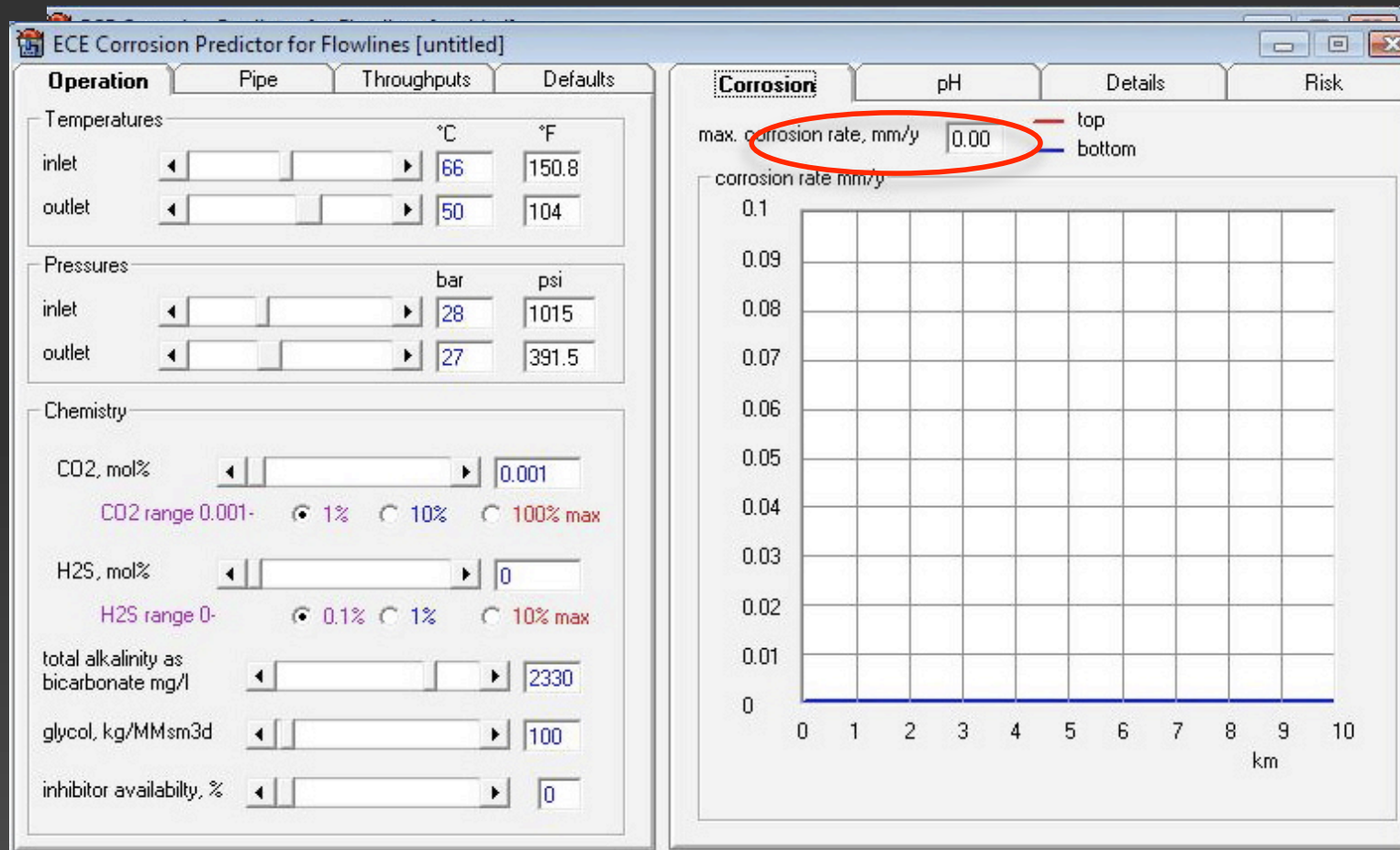
Reality check & Simulation check



Data interpretation



Design and operational stage comparison output.

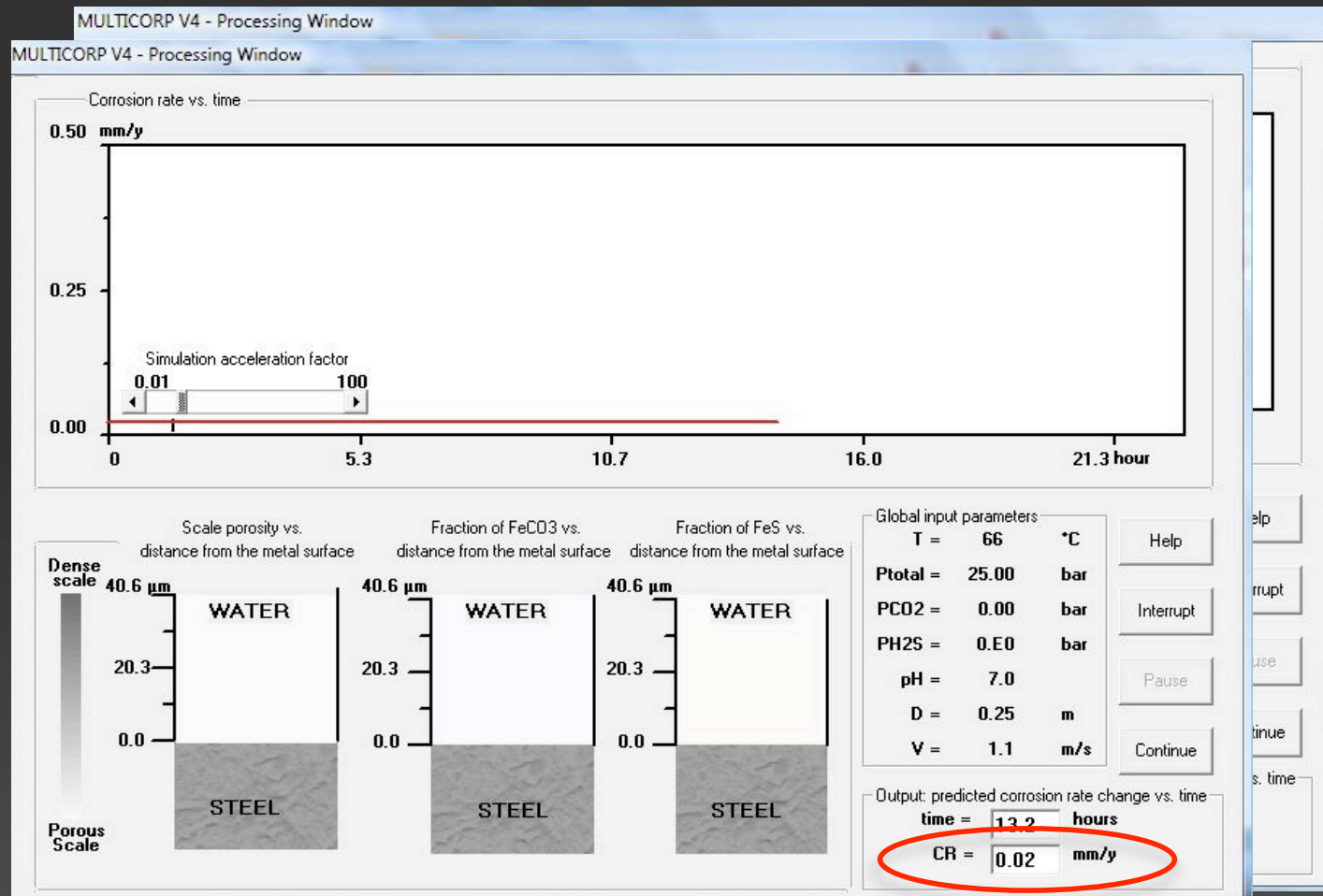


Design = 0 mm/yr

Operational = 0 mm/yr

# MULTICORP

Design and operational stage comparison output.



Design = 0.13 mm/yr  
Operational = 0.02 mm/yr

# Discussions

Design and operation stage predictions. (ECE4)

<b>Field</b>	<b>Corrosion rate, mm/year (ECE4)</b>	
	<b>Design</b>	<b>Operation</b>
Field B	0	0
Field J	0.250	0.160

Design and operation stage predictions. (MULTICORP)

<b>Field</b>	<b>Corrosion rate, mm/year (MULTICORP)</b>	
	<b>Design</b>	<b>Operation</b>
Field B	0.130	0.020
Field J	0.080	0.018

<b>ECE4 - B Field</b>		
Parameters	Value	
	Design	Operation
Temperature (deg C)		
Inlet	70	66
Outlet	30	50
Pressure (bar)		
Inlet	20	28
Outlet	7	27
CO <sub>2</sub> mol %	0.04	0.001
H <sub>2</sub> S mol %	-	0
Production flow rates		
Crude (m <sup>3</sup> /day)	435	1000
Gas (MMscfd)	0.2	0
Water (m <sup>3</sup> /day)	2390	2660
API gravity	30	39
Alkalinity as bicarbonate (ppm)	-	2330
Water cut (%)	85	68
Corrosion rate (mm/y)	0	0

MULTICORP – B Field		
Parameters	Value	
	Design	Operation
Temperature (deg C)		
Inlet	70	66
Outlet	30	50
Pressure (bar)		
Inlet	20	28
Outlet	7	27
CO <sub>2</sub> mol %	0.04	0.001
H <sub>2</sub> S mol %	-	0
Production flow rates		
Crude (m <sup>3</sup> /day)	435	2186.3
Gas (MMscfd)	0.2	0
Water (m <sup>3</sup> /day)	2390	512
API gravity	30	39
Alkalinity as bicarbonate (ppm)	0	3600
Sulphates (ppm)	0	98
Chlorides (ppm)	0	13000
Water cut (%)	85	68
Oil density (kg/m <sup>3</sup> )	780	793.7
Oil viscosity (N.s/m <sup>2</sup> )	-	0.0013
Velocity (m/s)	-	1.158
Corrosion rate (mm/y)	0.13	0.02



For field J, data from offshore ultrasonic test shows 0.1 mm thickness loss (after 7 years of service). Initial thickness =12 mm.

CR estimated = 0.014 mm/y

Reliability of models with values from ultrasonic test.

<b>ECE4 = 0.16 mm/y</b>	<b>MULTICORP = 0.018 mm/y</b>
(>100 percent difference)	(+- 29 percent difference - operation)

MULTICORP produces more accurate result due to its consideration of few critical factors e.g. presence of carbonates, sulphates and velocity of fluids.

# comparisons:

Parameters	ECE4	MULTICORP
CO <sub>2</sub> mole %	✓	✓
H <sub>2</sub> S mole %	✓	✓
O <sub>2</sub> in water	-	-
Acetic acid in water	-	✓
Pressure	✓	✓
Temperature	✓	✓
Gas flow rate	✓	✓
Oil flow rate	✓	✓
Water flow rate	✓	✓
Internal diameter	✓	✓
Pipe length	✓	✓
Bicarbonates	-	✓
Sulphates	-	✓
Chlorides	-	✓
Dissolved iron in water	-	✓
API gravity	✓	✓
Oil density	-	✓
Oil viscosity	-	✓
Water density	-	✓
Water viscosity	-	✓
pH	✓	✓
CO <sub>2</sub> partial pressure	-	-
Oil velocity	-	✓
Water velocity	-	✓
Water cut	✓	✓

MULTICORP takes into consideration the effect of acetic acid in water.

Bicarbonates, sulphates, chlorides effects.

Oil & water density and viscosity.

Oil & water velocity.

## CO<sub>2</sub>/H<sub>2</sub>S

In CO<sub>2</sub>/H<sub>2</sub>S corrosion of mild steel, both iron carbonate and iron sulfide layers can form on the steel surface.

Only CO<sub>2</sub> presence – pH dependence is small. IF water is present, form H<sub>2</sub>CO<sub>3</sub> – corrosive to alloy and CS.

No H<sub>2</sub>S, at high temperature, high pH – form FeCO<sub>3</sub> (protective layer).

## Flow rate

Corrosion rate increases with velocity. Strips away protective films.

pH

Dissolved  $\text{CO}_2$  or  $\text{H}_2\text{S}$  that contribute significantly to a lower pH.

$\text{CO}_2$  corrosion mechanism - different to that of strong acids like HCl.

$\text{CO}_2$  corrosion direct reduce of  $\text{H}_2\text{CO}_3$  to  $\text{HCO}_3^-$  rather than reduction of  $\text{H}^+$  ions  
(carbonic acid corrosion much more corrosive).

Effect of acetic acid:

Corrosion rate increases gradually with the **concentration** of acetic acid.

Corrosion rate is higher at **higher temperature**.

Reaction is retarded by an increase in pH due to less hydrogen ions being available for reduction.

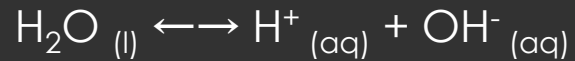
The undissociated **acetic acid** in the solution affects corrosion.

Under low condensation rate, presence of acetic acid (low concentrations) is enough to almost double the corrosion rate.

CO<sub>2</sub> corrosion of mild steel is always associated with the formation and **breakdown of protective iron carbonate films**.

The chemical and electrochemical equation involves in the CO<sub>2</sub> corrosion in the presence of acetic acid:

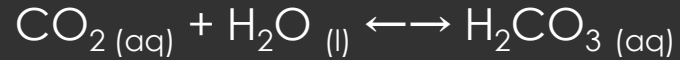
#### Water dissociation



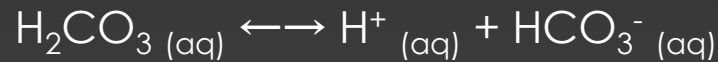
#### Carbon dioxide dissolution



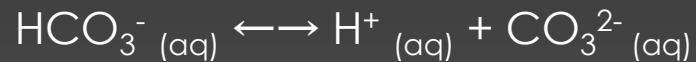
#### Carbon dioxide hydration



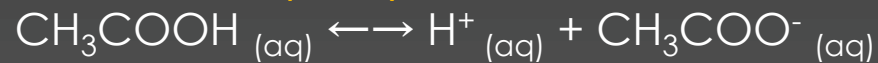
#### Carbonic acid dissociation



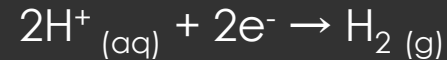
#### Bi-carbonate ion dissociation



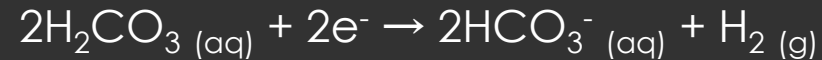
#### Acetic acid (HAc) dissociation



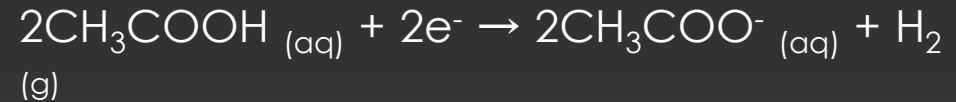
#### Proton reduction



#### Carbonic acid reduction



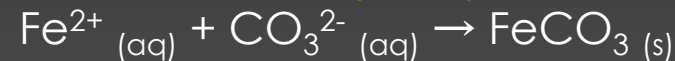
#### Undissociated acetic acid



#### Iron oxidation



#### Iron carbonate precipitation



Water corrosivity increased by dissolved gases, acids, salts, strong bases, entrained abrasives, high temperature, fluctuating pressure, cavitation, or impingement.

**Fast-moving** water carry dissolved metal ions away from corroding areas before the dissolved ions can be precipitated as protective layers.



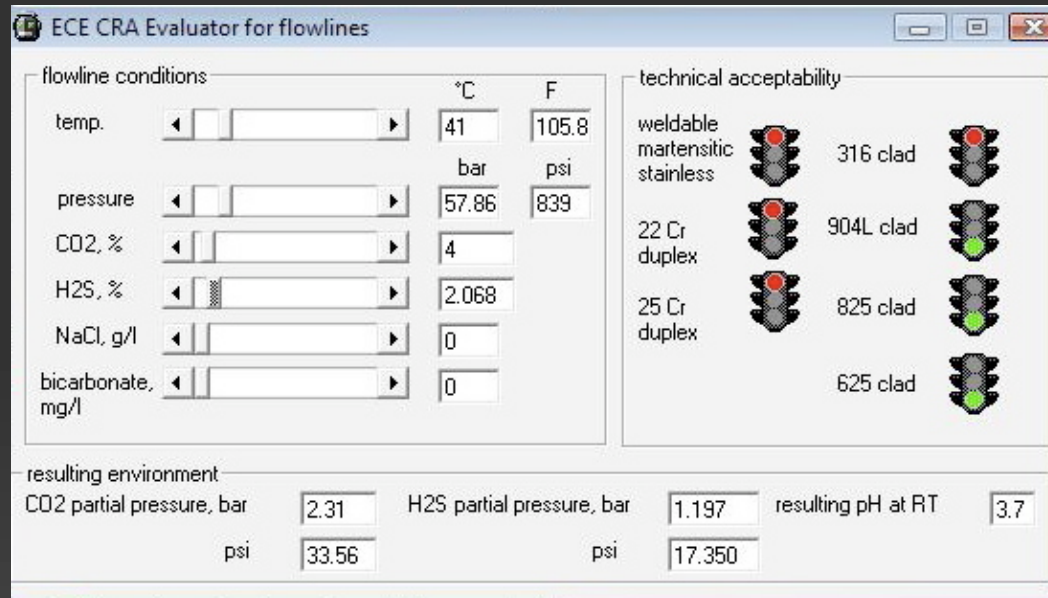
**Erosion-corrosion** - a combination of pitting and erosion.

Particles in a liquid or gas have effect on a metal surface - removal of protective surface films (protective oxide films).

**Temperature increases**, the protective films may become more soluble and/or less resistant to scouring.

**Turbulent** condition can cause an increase in corrosion rates or new forms and modes of corrosion.

## ECE4 CRA Evaluation Tool



Material	Acceptability
weldable martensitic stainless (316 clad)	Red (Fail)
22 Cr duplex (904L clad)	Yellow (Warning)
25 Cr duplex (825 clad)	Green (Pass)
625 clad	Green (Pass)

flowline conditions

temp. 41 °C 105.8 F

pressure 57.86 bar 839 psi

CO2, %

H2S, %

NaCl, g/l

bicarbonate, mg/l

technical acceptability

weldable martensitic stainless 316 clad

22 Cr duplex 904L clad

25 Cr duplex 825 clad

625 clad

resulting environment

CO2 partial pressure, bar 2.31 H2S partial pressure, bar 1.197 resulting pH at RT 3.7

psi 33.56 psi 17.350

Even at low temperature (around 40°C), one by one material starts to fail its technical acceptability in the case of H<sub>2</sub>S presence in CO<sub>2</sub> environment.

# Conclusions

Amount (required) data used during the design and operation stage were dissimilar. Influence predictions.

Presence of  $\text{CO}_2$ ,  $\text{H}_2\text{S}$ , free water, acetic acid and presence of carbonate content in the production highly affect the corrosion prediction.

Other factors; Inhibition type, flow velocity, flow type, pH, temperature etc.

ECE4 CRA evaluation tool make ease material selection process. Predicted CR.

MULTICORP considers critical parameters. Result more accurate.

Many more factors that can affect the corrosion prediction. Big impact to the material selection process and the overall life cycle of the project.

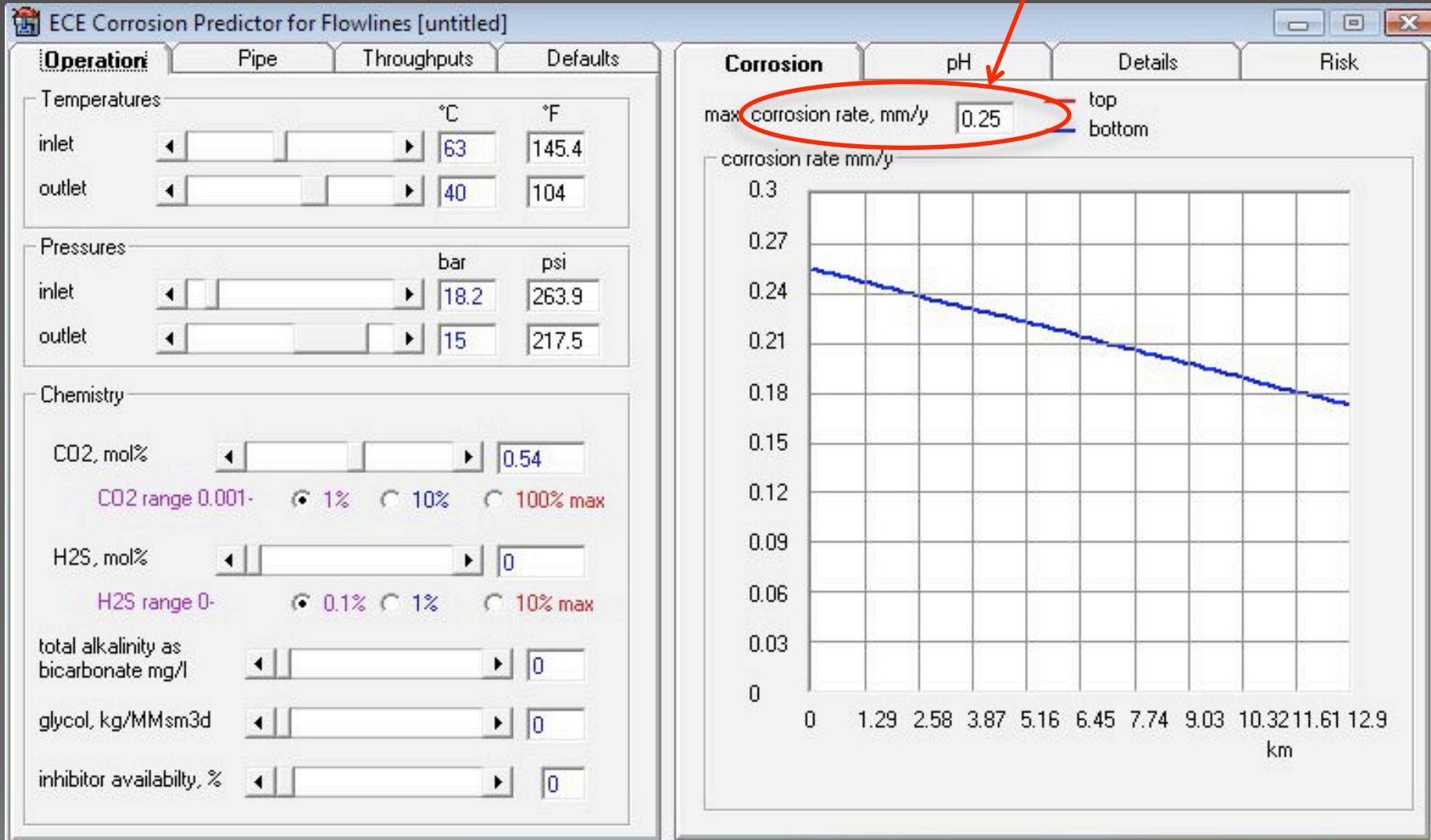
# Recommendations

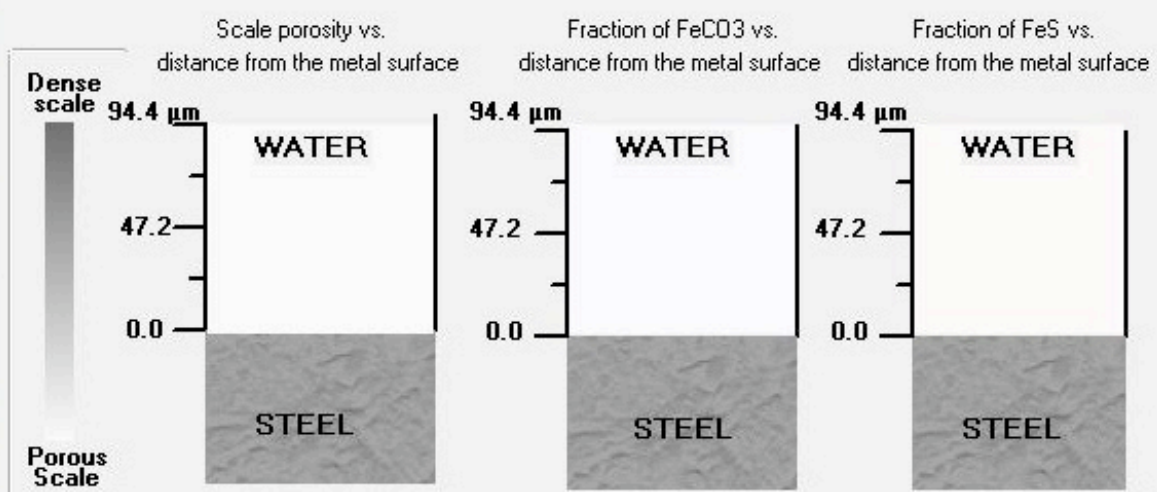
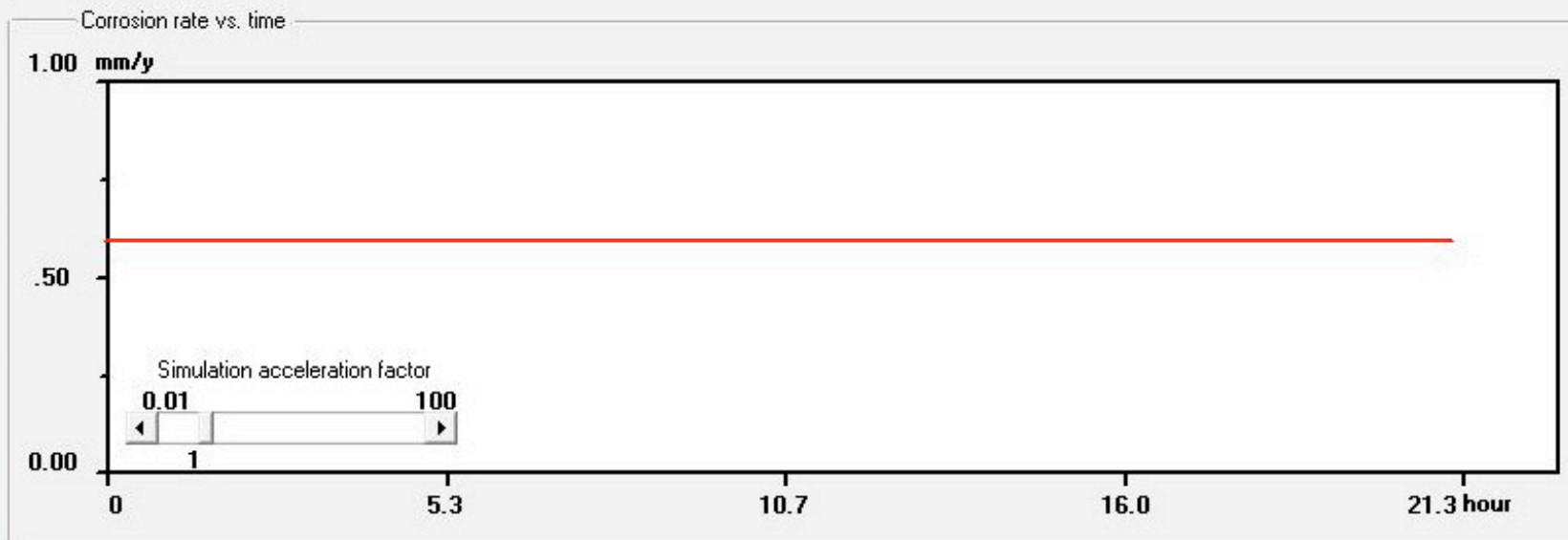
Study further other factors that can affect the corrosion prediction besides that were discussed above.

Model different field data using both ECE4 and MULTICORP considering more parameters.

Understanding the proper functions of the models and knowing the vital input data could help PETRONAS less rely on the consultant to perform the corrosion prediction and this could assist in producing outputs with a more accurate result in selecting materials.

ECE4 CR = 0.25 mm/yr





Global input parameters

T =	63	°C
Ptotal =	18.00	bar
PCO <sub>2</sub> =	0.10	bar
PH <sub>2</sub> S =	0.E0	bar
pH =	5.9	
D =	0.38	m
V =	0.4	m/s

Help

Interrupt

Pause

Continue

Output: predicted corrosion rate change vs. time

time = 19.7 hours

CR = 0.60 mm/y

MULTICORP

CR = 0.6 mm/yr